Thermodynamic and Thermophysical Properties of Organic Nitrogen Compounds. Part I. Methanamine, Ethanamine, 1- and 2- Propanamine, Benzenamine, 2-, 3-, and 4- Methylbenzenamine

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Thermodynamic and Thermophysical Properties of Organic Nitrogen Compounds. Part I. Methanamine, Ethanamine, 1- and 2-Propanamine, Benzenamine, 2-, 3-, and 4-Methylbenzenamine

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The thermodynamic and thermophysical properties of eight primary amines, methanamine, ethanamine, 1- and 2-propanamine, benzenamine, and 2-, 3-, and 4-methylbenzenamine have been evaluated. Recommended values are given for the following properties: normal boiling, freezing, and triple-point temperatures, critical constants, thermodynamic properties in the solid and liquid phases, vapor pressure, enthalpy of vaporization, density, second virial coefficients, and enthalpy of combustion. Ideal gas thermodynamic properties have been calculated by statistical mechanical methods.

Key words: critically evaluated data; methanamine; ethanamine; 1-propanamine; 2-propanamine; benzenamine; 2-methylbenzenamine; 3-methylbenzenamine; 4-methylbenzenamine; boiling temperature; freezing temperature; critical point; heat capacity; vapor pressure; enthalpy of vaporization; density; second virial coefficient; enthalpy of combustion; ideal gas thermodynamic properties; condensed phase thermodynamic properties; thermodynamics; thermochemistry; thermophysics.

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1. Introduction 1.1. Scope and Objectives

This report provides a compilation of a consistent set of evaluated physical and thermodynamic properties of a se-

lected group of amines. The critical evaluation of the thermodynamic and physical properties of chemical substances in the crystal, liquid and gas state, including the ideal gas state has been a principal research product at the Thermodynamics Research Center (TRC) for many years. The evaluations presented in this report constitute part of a research contract entitled "Selected Values of Properties of Chemical Compounds: Organic Nitrogen Compounds" between TRC and the Office of Standard Reference Data of the National Institute for Standards and Technology (formerly National Bureau of Standards).

Part 1 (this report) contains thermodynamic data of the following organic nitrogen compounds: methanamine, ethanamine, 1- and 2-propanamine, benzenamine, and 2-, 3-, and 4-methylbenzenamine. Literature data were evaluated for the following properties: normal boiling, freezing and triple-point temperatures, critical constants, vapor pressure, enthalpy of vaporization, density, second virial coefficients, solid, liquid, and gas heat capacity and enthalpy of combustion. The ideal gas thermodynamic properties were calculated by statistical mechanical methods.

Estimates of precision were assigned to all the experimental data, and temperature dependent selected data were obtained from smoothing equations. Coefficients of the smoothing equations are listed. Where appropriate, estimates of inaccuracy limits are provided for recommended values.

1.2. Organization of the Report

The details of the smoothing equations, the recommended coefficients as well as the recommended values at selected temperatures for each compound are discussed for each property in the appropriate sub-sections of Sec. 2. Merits of the available experimental and spectroscopic data are discussed for each compound in Sec. 3. The organization is by property rather than compound.

1.3. References and Literature Coverage

Most of the selected values are based on experimental measurements of either thermodynamic properties or spectra. The majority of the information is from pertinent journals and periodicals. Additional information came from private and government reports, theses, and other sources. The majority of the data was taken from the original documents. Chemical Abstracts, other reviews, and the TRC Source files were used to obtain references to the primary sources.

1.4. Symbols, Units, Standard States, Temperature Scale and Naming Conventions

Symbols used are those recently recommended by the International Union of Pure and Applied Chemistry (IU-PAC) (1988-121) (1982-150), and the units used are either multiples or sub-multiples of the base SI units. The fundamental constants recommended by the Committee on Data for Science and Technology (CODATA) of the International Council of Scientific Union (ICSU) in 1987 (1987-158) and the relative atomic masses recommended by IU-PAC in 1985 (1986-333) were used for all calculations. Some of the results are in dimensionless forms derived with the gas constant of 8.31451 J mol⁻¹ K⁻¹. The relative molar masses are listed in Table 23. The standard states of the elements used in the calculation of the enthalpy of formation were the

ideal gas at 0.1 MPa for $\rm H_2$ and $\rm N_2$ and graphite for carbon. Where there was adequate documentation for the temperature scale used, the data were converted to the International Practical Temperature Scale of 1968 (IPTS-68) (1976-175); otherwise, values other than those for vapor pressures were used without conversion. There was a slight statistical advantage to making temperature scale corrections to vapor pressure data.

IUPAC nomenclature (1979-194) is used for the compound names. The accepted names, Chemical Abstracts registry numbers, empirical formulas, and some of the more commonly used synonyms are as follows:

methanamine, 74-89-5, CH₅N, aminomethane, methylamine;

ethanamine, 75-04-7, C₂H₇N, aminoethane, ethylamine;

1-propanamine, 107-10-8, C₃H₉N, 1-aminopropane, *n*-propylamine, propylamine;

2-propanamine, 75-31-0, C₃H₉N, 2-aminopropane, 2-propylamine, isopropylamine;

benzenamine, 62-53-3, C₆H₇N, aniline, phenylamine, aminobenzene;

2-methylbenzenamine, 95-53-4, C₇H₉N, 2-aminotoluene, *o*-aminotoluene, 2-methylaniline, *o*-methylaniline, *o*-toluidine, 1-amino-2-methylbenzene;

3-methylbenzenamine, 108-44-1, C₇H₉N, 3-aminotoluene, *m*-aminotoluene, 3-methylaniline, *m*-methylaniline, *m*-toluidine, 1-amino-3-methylbenzene:

4-methylbenzenamine, 106-49-0, C₇H₉N, 4-aminotoluene, *p*-aminotoluene, 4-methylaniline, *p*-methylaniline, *p*-toluidine, 1-amino-4-methylbenzene.

1.5. Procedures for Evaluation, Processing, and Selection of Data

The following steps were used in this compilation:

- (i) Search the scientific literature, identify the sources of data and record the pertinent numerical values in the TRC Database.
- (ii) Rate and evaluate the available data on the basis of accuracy and reliability and sort out the "best" numerical values.
- (iii) Convert the data to a uniform set of units and conditions and adjust them to the current set of fundamental constants and relative molar masses.
- (iv) Make preliminary choice of "reliable" values and, where appropriate, fit them to standard functions of temperature, pressure or other variables for further testing.
- (v) Test the preliminary choices for internal thermodynamic consistency and make necessary adjustments to achieve consistency to within the experimental uncertainty.
- (vi) Calculate the values of the derived properties from the final choices of the basic input data.
 - (vii) Estimate the uncertainties in the selected values.

The evaluation of the available data was based entirely on the judgment of the compilers, and no rigorous rules can be stated. Considerations were given to sample purity and experimental technique as described in the publications, as well as to the reputation of the authors for reliable work.

Normally, more weight was given to a value obtained as the principal objective of an investigation rather than as a byproduct of some other study. Often the best values were obvious. However, in many cases, after eliminating the obviously inconsistent data, several reported values of about comparable reliability were left. In such cases a properly weighted combination of the values was chosen. In some situations it was necessary to combine data of different reliability to obtain the final selections. For example, a series of accurate measurements of the vapor pressure of a specific compound was available over a certain range of temperature and another series of less reliable values was available outside this range. To obtain a smoothed set of selected values over the extended temperature range it was necessary to fit both sets of data to the same function of temperature. It was more common to have several sets of data of varying reliability for various temperature ranges which partially or completely overlapped. In fitting all of these data to a single function of temperature, more weight was given to the more reliable values. However, in some cases, the resulting equation did not reproduce the best data as well as desired, so the less reliable data were rejected. While there are cases in which the values of density or vapor pressure, as calculated from the selected equation, do not reproduce all data to within the imprecisions of the original data, such discrepancies are small and not much greater than the experimental uncertainty.

1.6. Fitting to Equations

Coefficients to smoothing equations were determined by weighted least squares, where the weights in the squared deviation functions were the reciprocals of the variances in the deviation functions (1967-292), and the variances were determined from estimates of the imprecisions in the observed variables. Data were given zero weight either if they were obviously discordant with sets deemed most reliable, or if their inclusion would place undue weight on a particular point or region in the fit. Estimates of imprecision $\sigma(x)$ in the experimental observations x are given in the form

$$\sigma(x) = \sigma_{\iota}(x) + x\sigma_{\iota}(x), \tag{1}$$

where the values of the constants $\sigma_c(x)$ and $\sigma_f(x)$ are tabulated in the tables that summarize sources and ranges of experimental data.

Imprecisions in the values derived from the fitting equations were determined by propagation of errors with the inverse of the normal equations for the weighted least-squares process, variance-covariance matrix (1944-236), (1986-789). The square roots from the principal diagonal of these matrices were used to calculate the standard deviations $\sigma(A_i)$ listed with each of their associated parameters A_i in the appropriate tables. The off-diagonal elements were normalized by dividing the elements in each row and each column by the respective square root of the diagonal belonging to the row or column to give elements $C(A_i, A_j)$ in the correlation matrix. The diagonal elements of the correlation matrix $C(A_i, A_j)$ are unity. Imprecision in the values for a function, $Y(A_1, A_2, ...)$ of the parameters $A_1, A_2, ...$, was calculated from

$$\sigma(Y) = \left[\sum_{i} \sum_{j} (\partial Y / \partial A_{i}) \sigma(A_{i}) \times C(A_{i}, A_{j}) (\partial Y / \partial A_{j}) \sigma(A_{j}) \right]^{1/2}.$$
 (2)

In many instances the parameters A_i are highly correlated so that the absolute values of $C(A_i,A_j)$ are close to unity and the right hand side of Eq. (2) is close to a perfect square with mixed signs on the cross product terms. The extent of these correlations required that the number of digits listed for the constants is greater than is apparently warranted by the imprecision in each of the parameters.

In instances where parameters with known imprecisions were constrained to predetermined values, the contributions from their imprecisions were determined by perturbing each constrained parameter in question by its imprecision and then repeating the least squares process. The estimated imprecisions of the derived values of the properties are shown on the plots of deviations from the fitting equations.

2. Recommended Values 2.1. Freezing, Normal Boiling, and Critical Temperatures with Critical Pressure and Volume

The selected freezing (T_m) , normal boiling (T_b) (at 101.325 kPa) and critical temperatures (T_c) , with the selected critical pressure (p_c) and critical volume (V_c) and the estimated uncertainties are listed in Table 1. The experimental data considered in the selections are discussed in Sec. 3.1. The values for the normal boiling temperature were derived from the Cox equation used for fitting the vapor pressure data.

2.2. Vapor Pressure

The vapor pressure (p_{sat}) measurements were smoothed with the Cox equation (1936-431):

$$\ln(p_{\text{sat}}/p_{\text{ref}}) = A_x [1 - 1/(T/T_{\text{ref}})],$$
 where

$$\ln A_x = A_0 + A_1 (T/T_{\text{ref}}) + A_2 (T/T_{\text{ref}})^2.$$
 (3b)

 $T_{\rm ref}$ and $p_{\rm ref}$ are a reference temperature and pressure, respectively. In this work, the boiling temperature T_b at atmospheric pressure (101.325 kPa) was chosen as the reference temperature $T_{\rm ref}$. Values of the parameters A_i and T_b with their associated imprecisions are listed in Table 2, and the correlation matrix for the Cox equation coefficients is listed in Table 2a. The values of vapor pressures at selected temperatures are listed in Table 3.

We also report constants for the Antoine equation because the equation is commonly used to fit vapor pressure measurements over a limited pressure range, and the majority of TRC tables contain values calculated from either the Antoine or extended Antoine equation (1988-191). The coefficients of the Antoine equation were determined for the following three pressure ranges: (a) triple point pressure p_{tp} to 20 kPa; (b) 20 kPa to 200 kPa; and (c) 100 kPa to the critical pressure p_c . For the first two pressure ranges, the three parameter Antoine equation was used:

TABLE 1. Selected freezing, normal boiling, and critical temperatures with critical pressure and volume.

Compound	$rac{T_{ m m}}{ m K}$	$rac{T_{ m b}}{ m K}$	$rac{T_c}{ extbf{K}}$	$rac{p_c}{ ext{MPa}}$	$rac{V_{ m c}}{{ m cm}^3 \cdot { m mol}^{-1}}$
	1 70 700 1 0 010		400 7 1 0 0		100 1 0
Methanamine	179.708 ± 0.01^a	266.80 ± 0.02	430.7 ± 0.2	7.614 ± 0.015	120 ± 6
Ethanamine	192.62 ± 0.05	289.74 ± 0.06	456.2 ± 1.0	5.63 ± 0.11	181 ± 5
1-Propanamine	188.389 ± 0.01^a	320.370 ± 0.002	497 ± 1	4.72 ± 0.08	228 ± 11
2-Propanamine	178.011 ± 0.01^a	304.905 ± 0.002	471.9 ± 0.5	4.54 ± 0.06	221 ± 11
Benzenamine	267.133 ± 0.01^a	457.32 ± 0.08	699 ± 2	4.89 ± 0.12	280 ± 14
2-Methylbenzenamine	$\textbf{256.8} \pm \textbf{0.1}$	473.49 ± 0.04	707 ± 2	4.37 ± 0.12	333 ± 17
3-Methylbenzenamine	241.9 ± 0.1	476.52 ± 0.04	707 ± 2	4.28 ± 0.12	333 ± 17
4-Methylbenzenamine	316.9 ± 0.1	473.57 ± 0.08	706 ± 2	4.58 ± 0.14	340 ± 17

a triple point temperature

TABLE 2. Coefficients of the Cox equation (Eq. 3) for vapor pressure.

Compound	A_0	$\sigma(A_0)^a$	A_1	$\sigma(A_1)^a$	A_2	$\sigma(A_2)^a$	$T_{ m b}/{ m K}$	$\sigma(T_{ m b})/{ m K}^a$	$rmswd^b$
Methanamine	2.84924	0.00670	-0.51838	0.01353	0.15900	0.00614	266.797	0.016	0.60
Ethanamine	2.90190	0.02633	-0.64109	0.04701	0.20419	0.01976	289.738	0.055	0.65
1-Propanamine	2.91580	0.00554	-0.68989	0.00944	0.22235	0.00392	320.369	0.002	0.18
2-Propanamine	2.93670	0.00296	-0.74722	0.00564	0.24909	0.00256	304.905	0.002	0.31
Benzenamine	2.88571	0.01401	-0.58271	0.03131	0.18054	0.01617	457.318	0.079	1.08
2-Methylbenzenamine	3.18501	0.02530	-1.18083	0.04953	0.45370	0.02282	473.490	0.037	0.62
3-Methylbenzenamine	3.09998	0.02487	-0.98036	0.04841	0.36137	0.02209	476.522	0.039	0.61
4-Methylbenzenamine	3.07126	0.03643	-0.94617	0.07333	0.35468	0.03490	473.573	0.082	0.43

a see section 1.6

TABLE 2a. Correlation matrix a for the Cox equation coefficients.

Compound	$C(A_0,A_1)$	$C(A_0, A_2)$	$C(A_0, T_{ m b})$	$C(A_1, A_2)$	$C(A_1, T_{\mathrm{b}})$	$C(A_2, T_{\mathrm{b}})$
Methanamine	-0.99581	0.98380	0.50320	-0.99524	-0.55310	0.56901
Ethanamine	-0.99291	0.97980	-0.40649	-0.99637	0.38245	-0.35579
1-Propanamine	-0.99740	0.98844	-0.37025	-0.99663	0.36209	-0.34843
2-Propanamine	-0.99419	0.97603	-0.15302	-0.99310	0.12990	-0.10631
Benzenamine	-0.99484	0.98158	0.52424	-0.99529	-0.58443	0.61114
2-Methylbenzenamine	-0.99773	0.99206	-0.00176	-0.99809	-0.03142	0.05625
3-Methylbenzenamine	-0.99706	0.99069	-0.16781	-0.99801	0.14007	-0.11718
4-Methylbenzenamine	-0.99817	0.99356	-0.37395	-0.99851	0.33522	-0.29986

a see section 1.6

b rmswd = root-mean-squared-weighted deviation

TABLE 3. Values of vapor pressures calculated from the Cox equation (Eq. 3) at selected temperatures.

190	T K	p _{sat} kPa	T K	p _{sat} kPa	$\frac{T}{K}$	p _{sat} kPa	$\frac{T}{K}$	p _{sat} kPa	T K	p _{sat} kPa	$\frac{T}{K}$	<i>p</i> sa kP
190					Μe	ethanamin	.e				•	
200	179.708	0.178	230	13.85	280	177.9	320	704	370	2455	420	631
210	190	0.541	240	25.59	290	261.8	330	935	380	3022	430	744
Ethanamine 192.62		1.406		44.57	298.15		340	1218	390	3681	430.7	753
Ethanamine 192.62 0.143 240 7.89 290 102.4 330 408 380 1435 430 3 200 0.311 250 14.59 298.15 140.9 340 543 390 1768 440 4 210 0.804 260 25.4 300 151.0 350 709 400 2154 450 5 220 1.87 270 42.2 310 216.0 360 910 410 2600 456.2 5 230 3.99 280 67.0 320 300.8 370 1151 420 3111 1-Propanamine 188.389 0.00927 250 3.148 300 45.601 360 350.06 420 1361.9 480 3 200 0.03877 260 5.955 310 68.596 370 455.04 430 1639.6 490 4 210 0.1144 270 10.633 320 99.980 380 581.9 440 1956.8 497 4 210 0.1144 270 10.633 320 99.980 380 581.9 440 1956.8 497 4 220 0.3008 280 18.040 330 141.67 390 733.2 450 2317.2 230 0.7150 290 29.259 340 195.75 400 911.8 460 2724 240 1.5581 298.15 42.125 350 264.43 410 1120.3 470 3184 2-Propanamine 178.011 0.00790 240 3.721 298.15 78.045 350 423.6 410 1626.8 470 4 190 0.03815 250 7.138 300 83.951 360 549.0 420 1957 471.9 4 200 0.1194 260 12.865 310 122.22 370 700.2 430 2336 210 0.3284 270 21.964 320 172.85 380 880.1 440 2769 220 0.8080 280 35.752 330 238.24 390 1092.1 450 3261 230 1.807 290 55.808 340 320.94 400 1339.7 460 3820 Benzenamine 267.133 0.00651 350 2.032 430 46.82 510 339 590 1318 670 3 280 0.0206 360 3.30 440 62.9 520 413 600 1517 680 4 290 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 290 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298.15 0.0867 380 7.95 460 108.6 540 596 620 1981 699 4 300 0.0992 390 11.85 470 139.7 550 708 630 2248 310 0.199 400 17.24 480 17.4 560 835 640 2541 320 0.691 420 34.22 500 276.4 580 1139 660 3211		3.286			300		350	1561	400			
192.62	220	7.01	270	116.86	310	519.1	360	1971	410	5314		
200					E	hanamine	•					
210	192.62	0.143	240	7.89	290	102.4	330	408	380	1435	430	369
220	200			14.59	298.15	140.9	340		390	1768	440	435
188.389 0.00927 250 3.148 300 45.601 360 350.06 420 1361.9 480 3 200 0.03877 260 5.955 310 68.596 370 455.04 430 1639.6 490 4 210 0.1144 270 10.633 320 99.980 380 581.9 440 1956.8 497 4 220 0.3008 280 18.040 330 141.67 390 733.2 450 2317.2 230 0.7150 290 29.259 340 195.75 400 911.8 460 2724 240 1.5581 298.15 42.125 350 264.43 410 1120.3 470 3184 2-Propanamine 178.011 0.00790 240 3.721 298.15 78.045 350 423.6 410 1626.8 470 4 190 0.03815 250 7.138 300 83.951 360 549.0 420 1957 471.9 4 200 0.1194 260 12.865 310 122.22 370 700.2 430 2336 210 0.3284 270 21.964 320 172.85 380 880.1 440 2769 220 0.8080 280 35.752 330 238.24 390 1092.1 450 3261 230 1.807 290 55.808 340 320.94 400 1339.7 460 3820 Benzenamine 267.133 0.00651 350 2.032 430 46.82 510 339 590 1318 670 3 280 0.0206 360 3.30 440 62.9 520 413 600 1517 680 4 298 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298 15 0.0867 380 7.95 460 108.6 540 596 620 1981 699 4 300 0.0992 390 11.85 470 139.7 550 708 630 2248 300 0.0992 390 11.85 470 139.7 550 708 630 2248 310 0.199 400 17.24 480 177.4 560 835 640 2541 320 0.379 410 24.54 490 222.6 570 978 650 2862 330 0.691 420 34.22 500 276.4 580 1139 660 3211					300	151.0	350	709	400	2154	450	511
1-Propanamine 188.389 0.00927 250 3.148 300 45.601 360 350.06 420 1361.9 480 3 200 0.03877 260 5.955 310 68.596 370 455.04 430 1639.6 490 4 210 0.1144 270 10.633 320 99.980 380 581.9 440 1956.8 497 4 220 0.3008 280 18.040 330 141.67 390 733.2 450 2317.2 230 0.7150 290 29.259 340 195.75 400 911.8 460 2724 2240 1.5581 298.15 42.125 350 264.43 410 1120.3 470 3184 2-Propanamine 178.011 0.00790 240 3.721 298.15 78.045 350 423.6 410 1626.8 470 4 190 0.03815 250 7.138 300 83.951 360 549.0 420 1957 471.9 4 200 0.1194 260 12.865 310 122.22 370 700.2 430 2336 210 0.3284 270 21.964 320 172.85 380 880.1 440 2769 220 0.8080 280 35.752 330 238.24 390 1092.1 450 3261 230 1.807 290 55.808 340 320.94 400 1339.7 460 3820 Benzenamine 267.133 0.00651 350 2.032 430 46.82 510 339 590 1318 670 3 280 0.0206 360 3.30 440 62.9 520 413 600 1517 680 4 290 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298.15 0.0867 380 7.95 460 108.6 540 596 620 1981 699 4 300 0.0992 390 11.85 470 139.7 550 708 630 2248 310 0.199 400 17.24 480 177.4 560 835 640 2541 320 0.379 410 24.54 490 222.6 570 978 650 2862 330 0.691 420 34.22 500 276.4 580 1139 660 3211					310	216.0		910	410	2600	456.2	562
188.389	230	3.99	280	67.0	320	300.8	370	1151	420	3111		
200					1-P	ropanami	ne					
210	188.389	0.00927	250	3.148	300	45.601	360	350.06	420	1361.9	480	370
220 0.3008 280 18.040 330 141.67 390 733.2 450 2317.2 230 0.7150 290 29.259 340 195.75 400 911.8 460 2724 240 1.5581 298.15 42.125 350 264.43 410 1120.3 470 3184 2-Propanamine 178.011 0.00790 240 3.721 298.15 78.045 350 423.6 410 1626.8 470 4 190 0.03815 250 7.138 300 83.951 360 549.0 420 1957 471.9 4 190 0.1194 260 12.865 310 122.22 370 700.2 430 2336 210 0.3284 270 21.964 320 172.85 380 880.1 440 2769 220 0.8080 280 35.752 330 238.24 390 1092.1 450 3261 230 1.807 290 55.808 340 320.94 400 1339.7 460 3820 **Benzenamine** *	200	0.03877	260	5.955	310	68.596	370	455.04	430	1639.6	490	427
230	210	0.1144	270	10.633	320	99.980	380	581.9	440	1956.8	497	472
240 1.5581 298.15 42.125 350 264.43 410 1120.3 470 3184 2-Propanamine 178.011 0.00790 240 3.721 298.15 78.045 350 423.6 410 1626.8 470 4 190 0.03815 250 7.138 300 83.951 360 549.0 420 1957 471.9 4 200 0.1194 260 12.865 310 122.22 370 700.2 430 2336 210 0.3284 270 21.964 320 172.85 380 880.1 440 2769 220 0.8080 280 35.752 330 238.24 390 1092.1 450 3261 230 1.807 290 55.808 340 320.94 400 1339.7 460 3820 Benzenamine 267.133 0.00651 350 2.032 430 46.82 510 339 590 1318 670 3 280 0.0206 360 3.30 440 62.9 520 413 600 1517 680 4 290 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298.15 0.0867 380 7.95 460 108.6 540 596 620 1981 699 4 300 0.0992 390 11.85 470 139.7 550 708 630 2248 310 0.199 400 17.24 480 177.4 560 835 640 2541 320 0.379 410 24.54 490 222.6 570 978 650 2862 330 0.691 420 34.22 500 276.4 580 1139 660 3211	220	0.3008	280	18.040	330	141.67	390	733.2	450	2317.2		
2-Propanamine 178.011 0.00790 240 3.721 298.15 78.045 350 423.6 410 1626.8 470 4 190 0.03815 250 7.138 300 83.951 360 549.0 420 1957 471.9 4 200 0.1194 260 12.865 310 122.22 370 700.2 430 2336 210 0.3284 270 21.964 320 172.85 380 880.1 440 2769 220 0.8080 280 35.752 330 238.24 390 1092.1 450 3261 230 1.807 290 55.808 340 320.94 400 1339.7 460 3820 Benzenamine 267.133 0.00651 350 2.032 430 46.82 510 339 590 1318 670 3 280 0.0206 360 3.30 440 62.9 520 413 600 1517 680 4 290 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298.15 0.0867 380 7.95 460 108.6 540 596 620 1981 699 4 300 0.0992 390 11.85 470 139.7 550 708 630 2248 310 0.199 400 17.24 480 177.4 560 835 640 2541 320 0.379 410 24.54 490 222.6 570 978 650 2862 330 0.691 420 34.22 500 276.4 580 1139 660 3211	230	0.7150	290	29.259	340	195.75	400	911.8	460	2724		
178.011 0.00790 240 3.721 298.15 78.045 350 423.6 410 1626.8 470 4 190 0.03815 250 7.138 300 83.951 360 549.0 420 1957 471.9 4 200 0.1194 260 12.865 310 122.22 370 700.2 430 2336 210 0.3284 270 21.964 320 172.85 380 880.1 440 2769 220 0.8080 280 35.752 330 238.24 390 1092.1 450 3261 230 1.807 290 55.808 340 320.94 400 1339.7 460 3820 Benzenamine 267.133 0.00651 350 2.032 430 46.82 510 339 590 1318 670 3 280 0.0206 360 3.30 440 62.9 520 413 600 1517 680 4 290 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298.15 0.0867 380 7.95 460 108.6 540 596 620 1981 699 4 300 0.0992 390 11.85 470 139.7 550 708 630 2248 310 0.199 400 17.24 480 177.4 560 835 640 2541 320 0.379 410 24.54 490 222.6 570 978 650 2862 330 0.691 420 34.22 500 276.4 580 1139 660 3211	240	1.5581	298.15	42.125	350	264.43	410	1120.3	470	3184		
190					2-P	ropanami	ne					
200 0.1194 260 12.865 310 122.22 370 700.2 430 2336 210 0.3284 270 21.964 320 172.85 380 880.1 440 2769 220 0.8080 280 35.752 330 238.24 390 1092.1 450 3261 230 1.807 290 55.808 340 320.94 400 1339.7 460 3820 Benzenamine 267.133 0.00651 350 2.032 430 46.82 510 339 590 1318 670 3 280 0.0206 360 3.30 440 62.9 520 413 600 1517 680 4 290 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298.15 0.0867 380 7.95 460 108.6 540 596 620 1981 699 4 300 0.0992 390 11.85 470 139.7 550 708 630 2248 310 0.199 400 17.24 480 177.4 560 835 640 2541 320 0.379 410 24.54 490 222.6 570 978 650 2862 330 0.691 420 34.22 500 276.4 580 1139 660 3211	178.011	0.00790	240	3.721	298.15	78.045	350	423.6	410	1626.8	470	445
210 0.3284 270 21.964 320 172.85 380 880.1 440 2769 220 0.8080 280 35.752 330 238.24 390 1092.1 450 3261 230 1.807 290 55.808 340 320.94 400 1339.7 460 3820 Benzenamine 267.133 0.00651 350 2.032 430 46.82 510 339 590 1318 670 3 280 0.0206 360 3.30 440 62.9 520 413 600 1517 680 4 290 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298.15 0.0867 380 7.95 460 108.6 540 596 620 1981 699 4 300 0.0992 390 11.85 470 139.7 550 708 630 2248 310 0.199 400 17.24 480 177.4 560 835 640 2541 320 0.379 410 24.54 490 222.6 570 978 650 2862 330 0.691 420 34.22 500 276.4 580 1139 660 3211	190	0.03815	250	7.138	300	83.951	360	549.0	420	1957	471.9	458
220 0.8080 280 35.752 330 238.24 390 1092.1 450 3261 230 1.807 290 55.808 340 320.94 400 1339.7 460 3820 Benzenamine 267.133 0.00651 350 2.032 430 46.82 510 339 590 1318 670 3 280 0.0206 360 3.30 440 62.9 520 413 600 1517 680 4 290 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298.15 0.0867 380 7.95 460 108.6 540 596 620 1981 699 4 300 0.0992 390 11.85 470 139.7 550 708 630 2248 310 0.199 400 17.24 480 177.4 560 835 640 2541 320 0.379 410 24.54 490 222.6 570 978 650 2862 330 0.691 420 34.22 500 276.4 580 1139 660 3211	200	0.1194	260	12.865	310	122.22	370		430	2336		
Benzenamine 267.133 0.00651 350 2.032 430 46.82 510 339 590 1318 670 3 280 0.0206 360 3.30 440 62.9 520 413 600 1517 680 4 290 0.0467 370 5.19 450 83.3 530 498 610 1738 690 4 298.15 0.0867 380 7.95 460 108.6 540 596 620 1981 699 4 300 0.0992 390 11.85 470 139.7 550 708 630 2248 310 0.199 400 17.24 480 177.4 560 835 640 2541 320 0.379 410 24.54 490 222.6 570 978 650 2862 330 0.691 420 34.22 500 276.4 580 1139 660 3211		0.3284		21.964								
Benzenamine 267.133 0.00651 350												
267.133	230	1.807	290	55.808	340	320.94	400	1339.7	460	3820		
$\begin{array}{cccccccccccccccccccccccccccccccccccc$					Ве	nzenamin	e					
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	267.133	0.00651	350	2.032	430	46.82	510	339	590	1318		359
298.15 0.0867 380 7.95 460 108.6 540 596 620 1981 699 4 300 0.0992 390 11.85 470 139.7 550 708 630 2248 310 0.199 400 17.24 480 177.4 560 835 640 2541 320 0.379 410 24.54 490 222.6 570 978 650 2862 330 0.691 420 34.22 500 276.4 580 1139 660 3211	280	0.0206	360	3.30	440		520	413	600			400
300 0.0992 390 11.85 470 139.7 550 708 630 2248 310 0.199 400 17.24 480 177.4 560 835 640 2541 320 0.379 410 24.54 490 222.6 570 978 650 2862 330 0.691 420 34.22 500 276.4 580 1139 660 3211	290			5.19	450	83.3	530	498	610			445
310 0.199 400 17.24 480 177.4 560 835 640 2541 320 0.379 410 24.54 490 222.6 570 978 650 2862 330 0.691 420 34.22 500 276.4 580 1139 660 3211		0.0867	380	7.95	460						699	488
320 0.379 410 24.54 490 222.6 570 978 650 2862 330 0.691 420 34.22 500 276.4 580 1139 660 3211		0.0992	390	11.85	470							
330 0.691 420 34.22 500 276.4 580 1139 660 3211												
340 1.208			420	34.22	500	276.4	580	1139	660	3211		
	340	1.208										

TABLE 3. Continued.

2-Methylbenzenamine 256.8	p _{sat} kPa	T K	p _{sat} kPa	$rac{T}{\mathbf{K}}$	<u>p_{sat}</u> kPa	$rac{T}{K}$	$rac{p_{ ext{sat}}}{ ext{kPa}}$	$rac{T}{\mathbf{K}}$	$rac{p_{ ext{sat}}}{ ext{kPa}}$	$\frac{T}{K}$	$rac{p_{\mathtt{sat}}}{\mathtt{kPa}}$	TK
256.8						namine	hvlbenzei	2-Mei				
270								_ 1/20				
270	2141	650	681	570	149.6	490	15.28	410	0.321	330	0.000469	256.8
280	2436											
290	2765											
298.15	3135					520					0.0153	290
300	3549					530						298.15
310	4012	700			409	540				380	0.0362	300
320 0.164 400 10.53 480 118.6 560 578 640 1877 3-Methylbenzenamine 241.9 0.000058 320 0.135 410 13.37 500 176.4 590 920 680 250 0.000172 330 0.265 420 19.13 510 219.2 600 1070 690 260 0.00058 340 0.494 430 26.77 520 269.7 610 1238 700 270 0.00179 350 0.879 440 36.75 530 328.7 620 1426 707 280 0.00497 360 1.50 450 49.54 540 397 630 1637 290 0.0126 370 2.47 460 65.69 550 476 640 1871 298.15 0.0255 380 3.94 470 85.78 560 567 650 2133 300 0.0298 390 6.08 480 110.4 570 670 660 2423 310 0.0655 400 9.14 490 140.4 580 787 670 2746 4-Methylbenzenamine 316.9 0.132 390 6.82 460 71.0 530 350 600 1141 670 330 0.317 400 10.18 470 92.5 540 423 610 1321 680 340 0.583 410 14.80 480 118.8 550 507 620 1524 690 350 1.02 420 21.05 490 150.7 560 604 630 1750 700 360 1.73 430 29.3 500 188.9 570 714 640 2003 706	4370					550	92.89					
241.9												
250						namine	hylbenzer	3-Met				
260	3104	680	920	590	176.4	500	13.37	410	0.135	320	0.000058	241.9
270	3502	690	1070	600	219.2	510	19.13	420	0.265	330	0.000172	250
280	3943	700	1238	610	269.7	520	26.77	430	0.494	340	0.00058	260
290	4280	707	1426	620	328.7	530	36.75	440	0.879	350	0.00179	270
298.15			1637	630	397	540	49.54	450	1.50	360	0.00497	280
300 0.0298 390 6.08 480 110.4 570 670 660 2423 310 0.0655 400 9.14 490 140.4 580 787 670 2746 4-Methylbenzenamine 316.9 0.132 390 6.82 460 71.0 530 350 600 1141 670 330 0.317 400 10.18 470 92.5 540 423 610 1321 680 340 0.583 410 14.80 480 118.8 550 507 620 1524 690 350 1.02 420 21.05 490 150.7 560 604 630 1750 700 360 1.73 430 29.3 500 188.9 570 714 640 2003 706			1871	640	476	550	65.69	460	2.47		0.0126	290
310 0.0655 400 9.14 490 140.4 580 787 670 2746 4-Methylbenzenamine 316.9 0.132 390 6.82 460 71.0 530 350 600 1141 670 330 0.317 400 10.18 470 92.5 540 423 610 1321 680 340 0.583 410 14.80 480 118.8 550 507 620 1524 690 350 1.02 420 21.05 490 150.7 560 604 630 1750 700 360 1.73 430 29.3 500 188.9 570 714 640 2003 706			2133	650	567	560	85.78	470	3.94	380	0.0255	298.15
4-Methylbenzenamine 316.9 0.132 390 6.82 460 71.0 530 350 600 1141 670 330 0.317 400 10.18 470 92.5 540 423 610 1321 680 340 0.583 410 14.80 480 118.8 550 507 620 1524 690 350 1.02 420 21.05 490 150.7 560 604 630 1750 700 360 1.73 430 29.3 500 188.9 570 714 640 2003 706			2423	660	670	570	110.4					
316.9 0.132 390 6.82 460 71.0 530 350 600 1141 670 330 0.317 400 10.18 470 92.5 540 423 610 1321 680 340 0.583 410 14.80 480 118.8 550 507 620 1524 690 350 1.02 420 21.05 490 150.7 560 604 630 1750 700 360 1.73 430 29.3 500 188.9 570 714 640 2003 706			2746	670	787	580	140.4	490	9.14	400	0.0655	310
330 0.317 400 10.18 470 92.5 540 423 610 1321 680 340 0.583 410 14.80 480 118.8 550 507 620 1524 690 350 1.02 420 21.05 490 150.7 560 604 630 1750 700 360 1.73 430 29.3 500 188.9 570 714 640 2003 706						namine	hylbenzer	4-Met	•			
330 0.317 400 10.18 470 92.5 540 423 610 1321 680 340 0.583 410 14.80 480 118.8 550 507 620 1524 690 350 1.02 420 21.05 490 150.7 560 604 630 1750 700 360 1.73 430 29.3 500 188.9 570 714 640 2003 706	2953	670	1141	600	350	530	71.0	460	6.82	390	0.132	316.9
340 0.583 410 14.80 480 118.8 550 507 620 1524 690 350 1.02 420 21.05 490 150.7 560 604 630 1750 700 360 1.73 430 29.3 500 188.9 570 714 640 2003 706	3344											
350 1.02 420 21.05 490 150.7 560 604 630 1750 700 360 1.73 430 29.3 500 188.9 570 714 640 2003 706	3779											
3 60 1.73 4 30 29.3 500 188.9 570 714 640 2003 706	4263											
	4580											
370 2.82 440 40.0 510 234.4 580 839 650 2286		-	2286	650	839	580	234.4	510	40.0	440	2.82	370
380 4.45 450 53.7 520 288.1 590 981. 660 2601										450	4.45	380

$$ln(p_{sat}/kPa) = A_a - B_a/(T/K + C_a).$$
 (4)

For the higher pressure range, an extended Antoine equation was used:

$$\log_{10}(p_{\text{sat}}/\text{kPa}) = A_a - B_a/(T/\text{K} + C_a) + D_a X_a^n + E_a X_a^8 + F_a X_a^{12},$$
 (5)

where $X_a = (T - T_a^\circ)/T_c$, $D_a = \log_{10}e = 0.43429$, T_c is the critical temperature and T_a° was determined from the nearest integer value of Celsius temperature at which the vapor pressure is 130 kPa. The coefficients for the mediumand high-pressure Antoine equation were adjusted to yield the same normal boiling temperature as the Cox equation within the uncertainty of the data. The coefficients are listed in Table 4.

TABLE 4. Coefficients^a of the Antoine equation (Eqs. 4 and 5) over the following ranges: a, triple point to 20 kPa; b, 20 kPa to 200 kPa; c, 100 kPa to critical pressure.

Compound	Range	Aa	$B_{\mathbf{a}}$	$C_{\mathbf{a}}$	$rac{T_a^{ m o}}{ m K}$	n	$E_{\mathbf{a}}$	$F_{\mathbf{a}}$	$T_{\mathbf{c}}$
Methanamine	a	6.1302	918.423	-46,47					
MC III	b	6.4613	1010.93	-39.94					
	c	6.4613	1010.93	-39.94	273.15	4.2347	-197.27	10989.	430.7
Ethanamine	ь	6.1203	964.494	-55.34					
	c	6.1203	964.494	-55.34	296.15	2.3232	-101.37	5974.	456.2
1-Propanamine	Ъ	6.0574	1047.18	-61.91					
	c	6.0574	1047.18	-61.91	328.15	3.4191	145.88	-5001.	497.
2-Propanamine	ь	6.0462	1000.85	-57.26					
	c	6.0462	1000.85	-57.26	328.15	2.4996	-99.29	21689.	471.9
Benzenamine	a	7.8189	2526.56	-13.50					
	b	6.2533	1590.91	-82.81					
	c	6.2533	1590.91	-82.81	470.15	4.6070	2871.	-545673.	699.
2-Methylbenzenamine	a	4.9997	1004.63	-148.36					
	ь	6.0032	1488.77	-101.07					
	c	6.0032	1488.77	-101.07	485.15	1.9968	2684.9	-284086.	707.
3-Methylbenzenamine	a	6.0845	1491.71	-107.97					
	b	5.9726	1462.13	-107.96					
	c	5.9726	1462.13	-107.96	490.15	1.4196	792.9	-84601.	707.
4-Methylbenzenamine	a.	5.2555	1109.60	-138.97					
	b	6.2867	1669.16	-83.84					
	c	6.2867	1669.16	-83.84	485.15	2.5203	2632.3	-787906.	706.

^a In Eq. 5, $D_a = \log_{10} e = 0.43429$

2.3. Saturated Liquid and Vapor Density

The selected experimental values for the density along the saturation curve ρ_1 were fitted to the equation:

$$\rho_l = \rho_c \left[1 + A_1 x^{\epsilon} + x \sum_i A_i x^{(i-2)/m} \right], \tag{6}$$

where i=2 to 4, m=2, $\epsilon=0.35$, $x=(1-T/T_c)$, ρ_I is the saturated liquid density, and ρ_c is the density at the critical temperature T_c . The upper limit on the sum depended upon the extent of the data available. Various values of ϵ and m were tested; however, the available data were not sufficiently precise nor measured in sufficient detail near the critical point to provide adequate sensitivity to the choice of the values. The results indicated that there is a statistical advan-

tage to using nonzero values of ϵ and values of m > 1. The value of ϵ is a commonly accepted approximation (1975-232). Equation (6) was used to reproduce the most significant terms from the complete expansion by Ley-Koo and Green (1977-189) for the liquid density near the critical point as well as terms for classical equations of state (1970-254). The coefficients, standard errors, and correlation matrix for Eq. (6) are listed in Tables 5 and 5a. The smoothed values of the densities from Eq. (6) are listed in Table 6.

Experimental values of the critical density were not available for several of the substances considered here. In such cases they were estimated from extrapolations of the rectilinear density:

$$(\rho_l + \rho_g)/2 = \rho_c + \alpha_m (1 - T/T_c),$$
 (7)

TABLE 5. Coefficients^a and their standard errors^b for Eq. 6 representing densities of the liquids.

Compound	A1	$\sigma(A_1)$	A_2	$\sigma(A_2)$	A_3	$\sigma(A_3)$	A ₄	$\sigma(A_4)$	rmswd ^c
Methanamine	2.72756	0.05765	-3.70256	0.46822	7.26323	0.93600	-3.71045	0.56658	4.21
Ethanamine	2.02707	0.00832	0.68726	0.04276	0.09905	0.04446			5.89
1-Propanamine	2.28708	0.01384	-0.40213	0.06078	0.97521	0.05656			6.37
2-Propanamine	1.93035	0.01071	0.27646	0.04759	0.41244	0.04388			1.13
Benzenamine	2.73925	0.09103	-3.12474	0.58812	5.30157	0.99722	-2.14627	0.51938	2.50
2-Methylbenzenamine	1.98053	0.00303	0.82364	0.00440					2.78
3-Methylbenzenamine	1.91047	0.00496	0.78919	0.00724					1.39
4-Methylbenzenamine			0.82247	0.00898					2.66

^a see table 7 for values of ρ_c and Table 1 for T_c

TABLE 5a. Correlation matrix" for coefficients in Eq. 6 representing densities of the liquids.

Compound	$C(A_1,A_2)$	$C(A_1,A_3)$	$C(A_1,A_4)$	$C(A_2,A_3)$	$C(A_2,A_4)$	$C(A_3,A_4)$
Methanamine	-0.98128	0.95547	-0.92847	-0.99432	0.98217	-0.99656
Ethanamine	-0.95509	0.89910		-0.98774		
1-Propanamine	-0.98951	0.97018		-0.99489		
2-Propanamine	-0.99510	0.98668		-0.99782		
Benzenamine	-0.99695	0.99117	-0.98320	-0.99849	0.99439	-0.99870
2-Methylbenzenamine	-0.99799					
3-Methylbenzenamine	-0.99822					
4-Methylbenzenamine	-0.99844					

a see section 1.6

where ρ_c and α_m are tabulated in Table 7 with their standard errors and correlation coefficient. The ratios α_m/ρ_c are also listed to show the approximate constancy of their values. The selected values of T_c were used in these fits. The liquid densities (ρ_l) were the experimental values selected in Sec. 3.3, and the vapor densities (ρ_g) were determined from the second virial coefficients selected in Sec. 2.4 and values of the vapor pressure derived from the Cox equation. The range of

the data was limited to the region where the compressibility factor of the vapor $(p_{\rm sat}/RT\rho_g)$ was >0.8. For the benzenamines, second virial coefficients were not available, so the range was limited to where the vapor pressure was >1 bar. This procedure was tested with data where critical densities were available, see Table 15, and was shown to give reasonable agreement with experimental values of the critical density.

b see section 1.6

c rmswd = root-mean-squared-weighted deviation

TABLE 6. Densities of saturated liquid calculated from Eq. 6 at selected temperatures.

$\frac{T}{K}$	$\frac{\rho_l}{\mathrm{kg}\cdot\mathrm{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho_l}{\mathrm{kg}\cdot\mathrm{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho_l}{\mathrm{kg}\cdot\mathrm{m}^{-3}}$	$\frac{T}{K}$	$\frac{ ho_l}{ m kg\cdot m^{-3}}$	$\frac{T}{K}$	$\frac{\rho_l}{\mathrm{kg}\cdot\mathrm{m}^{-3}}$	<u>T</u>	$\frac{\rho_l}{\mathrm{kg}\cdot\mathrm{m}^{-3}}$
				N	/lethanan	nine					
179.708 190 200 210 220	788.3 778.1 767.9 757.5 746.9	230 240 250 260 270	736.0 724.9 713.5 702.0 690.2	280 290 298.15 300 310	678.2 665.9 655.8 653.4 640.7	320 330 340 350 360	627.6 614.2 600.3 586.0 570.9	370 380 390 400 410	555.1 538.0 519. 497. 470.	415 420 425 430 430.7	453. 432. 401. 330. 258.
					Ethanam	ine					
192.62 200 210 220 230 240	793.1 785.5 775.2 764.7 754.1 743.4	250 260 270 280 290 298.15	732.4 721.3 709.9 698.4 686.6 676.7	300 310 320 330 340 350	674.5 662.0 649.3 636.1 622.5 608.4	360 370 380 390 400 410	593.6 578.2 561.8 544.4 525.6 504.9	420 425 430 435 440 445	481.7 468.8 454.6 438. 420. 398.	450 452 454 455 456 456.2	369. 353. 332. 316. 284. 248.
				1-	Propana	mine					
188.389 200 210 220 230 240	820.2 809.0 799.3 789.7 779.9 770.2	250 260 270 280 290 298.15	760.3 750.4 740.5 730.45 720.30 711.94	300 310 320 330 340 350	710.03 699.64 689.09 678.3 667.4 656.3	360 370 380 390 400 410	644.9 633.1 621.0 608.5 595.5 581.8	420 430 440 450 460 470	567.3 551.8 535.0 516. 495. 470.	480 485 490 495 496 497	439. 418. 391. 345. 326. 259.
				2-	Propana	mine					
178.011 190 200 210 220 230	805.2 793.7 784.1 774.3 764.5 754.58	240 250 260 270 280 290	744.53 734.37 724.07 713.64 703.05 692.28	298.15 300 310 320 330 340	683.36 681.32 670.14 658.71 647.01 634.99	350 360 370 380 390 400	622.61 609.8 596.5 582.6 568.1 552.6	410 420 430 440 450 455	536.0 518.1 498. 475. 448. 432.	460 465 468 470 471 471.9	412. 386. 364. 343. 325. 268.
				F	Benzenam	ine					
267.133 280 290 298.15 300 310 320 330 340	1044.0 1033.12 1024.55 1017.54 1015.94 1007.29 998.60 989.87 981.10	370 380 390 400 410 420	972.28 963.42 954.52 945.58 936.58 927.54 918.45 909.31 900.1		890.8 881.5 872.1 862.6 853.0 843.4 833.6 823.7 813.7	530 540 550 560 570 580 590 600 610	793.1 782.5 771.7 760. 749. 737. 724.	620 630 640 650 655 660 665 670	697. 682. 666. 648. 638. 627. 615. 602. 587.	680 685 690 695 696 697 698 699	569. 548. 520. 476. 463. 447. 423. 332.

TABLE 6. Continued.

T K	$\frac{\rho_l}{\mathrm{kg}\cdot\mathrm{m}^{-3}}$	T K	$\frac{\rho_l}{\text{kg}\cdot\text{m}^{-3}}$	<u>T</u>	$\frac{\rho_l}{\mathrm{kg}\cdot\mathrm{m}^{-3}}$	$rac{T}{\mathbf{K}}$	$\frac{\rho_l}{\text{kg}\cdot\text{m}^{-3}}$	T K	$\frac{\rho_l}{ m kg\cdot m^{-3}}$	<u>Т</u> К	$\frac{\rho_l}{\text{kg} \cdot \text{m}^{-3}}$
				2-1	/Iethylbenz	enami	ine				
256.8	1028.0	340	959.7	430	879.0	520	786.9	610	672.	690	498.
270	1017.5	350	951.1	440	869.4	530	775.	620	656.	695	477.
280	1009.47	360	942.4	450	859.7	540	764.	630	640.	698	461.
290	1001.35	370	933.7	460	849.9	550	752.	640	622.	700	449.
298.15	994.69	380	924.8	470	839.9	560	740.	650	603.	702	434.
300	993.18	390	915.9	480	829.7	570	727.	660	582.	704	415.
310	984.92	400	906.8	490	819.3	580	714.	670	559.	705	402.
320	976.60	410	897.7	500	808.7	590	700.	680	532.	706	385.
330	968.20	420	888.4	510	797.9	600	686.	685	516.	707	321.
				3-N	/ethylbenz	enami	ine				
241.9	1029.0	330	959.13	430	871.9	530	770.	630	637.	685	515.
250	1022.7	340	950.8	440	862.6	540	759.	640	620.	690	497.
260	1015.0	350	942.4	450	853.1	550	747.	645	611.	695	476.
270	1007.2	360	934.0	460	843.4	560	735.	650	601.	698	460.
280	999.4	370	925.4	470	833.6	570	723.	655	591.	700	448.
290	991.51	380	916.8	480	823.6	580	710.	660	580.	702	434.
298.15	985.00	390	908.0	490	813.5	590	697.	665	569.	704	415.
300	983.52	400	899.2	500	803.1	600	683.	670	557.	705	402.
310	975.47	410	890.2	510	792.5	610	668.	675	545.	706	3 85.
320	967.34	420	881.1	520	781.	620	653.	680	53 1.	707	321.
				4-M	[ethylbenz	enami	me				
316.9	966.8	400	895.3	480	818.8	560	729.	640	612.	690	487.
330	956.01	410	886.2	490	808.5	570		650	593.	695	465.
340	947.61	420	877.0	500	798.0	580		660	573.	698	448.
350	939.13	430	867.7	510	787.3	590		665	561.	700	435.
360	930.56	440	858.2	520	776.4	600	676.	670	549.	702	419.
370	921.9	450	848.6	530	765.2	610		675	536.	704	396.
380	913.1	460	838.8	540	753.	620	646.	680	522.	705	378.
390	904.2	470	828.9	550	741.	630	630.	685	506.	706	315.

TABLE 7. Coefficients and standard errors^a of Eq. 7 for the rectilinear diameter line (from low reduced temperature density data).

Compound	$rac{ ho_{ m c}}{ m kg/m^3}$	$rac{\sigma(ho_{ m c})}{{ m kg/m^3}}$	$rac{lpha_{ m m}}{ m kg/m^3}$	$\frac{\sigma(\alpha_{ m m})}{{ m kg/m}^3}$	$C(ho_{ m c}, lpha_{ m m})$	$\frac{lpha_{ m m}}{ ho_{ m c}}$
Methanamine	258.14	0.36	235.34	0.86	-0.9837	0.9117
Ethanamine b	253.79	0.31	248.43	0.77	-0.9855	0.9789
1-Propanamine	259.58	0.24	242.25	0.62	-0.9801	0.9332
2-Propanamine ^b	253.90	0.24	240.80	0.61	-0.9619	0.9484
Benzenamine	332. 51	0.17	307.43	0.33	-0.9900	0.9246
2-Methylbenzenamine	321.31	0.81	304.28	1.43	-0.9951	0.9470
3-Methylbenzenamine	321.67	1.08	295.34	1.93	-0.9955	0.9181
4-Methylbenzenamine	315.17	0.75	305.76	1.47	-0.9961	0.9702

a see section 1.6

2.4. Second Virial Coefficients

The data available for densities below vapor saturation were limited and only second virial coefficients B in the equation of state

$$p/\rho RT = 1 + B\rho \tag{8}$$

were evaluated. The selected values of the second virial coefficient were smoothed using

$$B = A_b + C_b e^{(D_b/I)}. (9)$$

For correlation of data of limited range, this equation was cast into reduced form,

$$B = A_r \rho_c + C_b e^{D_r(\Gamma_c/I)}, \tag{10}$$

where the values of A_r and D_r were determined from the data for methylamine with the critical constants from Table 1. The coefficients to Eq. (9) are listed in Table 8 where, if the imprecision is not listed for a coefficient, the value was estimated with the aid of Eq. (10). Values of the second virial coefficient at selected temperatures are listed in Table 9.

TABLE 8. Coefficients of Eq. 9 with their correlation coefficients^a for the second virial coefficients.

Compound	$rac{A_{ m b}}{{ m cm}^3/{ m mol}}$	$rac{\sigma(A_{ m b})}{{ m cm}^3/{ m mol}}$	$rac{C_{ m b}}{{ m cm}^3/{ m mol}}$	$rac{\sigma(C_{ m b})}{{ m cm}^3/{ m mol}}$	$\frac{D_{\mathrm{b}}}{\mathrm{K}}$	$\frac{\sigma(D_{\mathrm{b}})}{\mathrm{K}}$	${ m rmswd}^b$	$C(A_b, C_b)$	$C(A_b, D_b)$	$C(C_b, D_b)$
Methanamine	15.50	5.02	-30.28	1.87	822	16	1.1	-0.9927	-0.9872	0.9990
Ethanamine	23.50		-46.74	2.27	852	16	16.9			0.9947
1-Propanamine	29.45		-47.51	0.44	928		0.9			
2-Propanamine	28.50		-44.43	0.73	881		1.5			

^a see section 1.6 ^b rmswd = root-mean-squared-weighted deviation

 $[^]b$ data not used for adopted ho_c ; experimental data available.

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TABLE 9. Second virial coefficients calculated from Eqs. 9 and 10 at selected temperatures.

$\frac{\overline{T}}{K}$	B	$\frac{T}{K}$	<u>B</u>	$\frac{T}{K}$	<u>B</u>	$\frac{T}{K}$	<u>B</u>	$\frac{T}{K}$	<u>B</u>	$\frac{T}{K}$	B
<u>K</u>	cm ³ ·mol ⁻¹	<u>K</u>	cm ³ ·mol ⁻¹	<u> </u>	$cm^3 \cdot mol^{-1}$	V	$cm^3 \cdot mol^{-1}$	<u> </u>	$cm^3 \cdot mol^{-1}$	K	cm ³ ·mol ⁻¹
					Methanan	nine					
170	-3790	260	-699	340	-324	430	-189	520		610	-101
180	-2890	270	-620	350	-301	440	-180	530		620	-98
190	-2270	280	-554	360	-281	450	-172	540		630	-96
200	-1820	290	-499	370	-263	460	-165	550		640	-93
210	-1500	298.15	-461	380	-247	470	-158	560		650	-91
220	-1250	300	-453	390	-233	480	-152	570	-112	660	-89
230	-1060	310	-413	400	-220	490	-146	580	-109	670	-87
240	-910	320	-379	410	-209	500	-141	590	-106	680	-85
250	-795	330	-350	420	-198	510	-136	600	-103		
					Ethanam	ine					
240	-1600	280	-956	310	-706	350	-509	390	-391	430	-315
250	-1380	290	-858	320	-646	360	-474	400	-369	440	-300
260	-1210	298.15		330	-594	370	-443	410	-349	450	-286
270	-1070	300	-776	340	-549	380	-416	420	-331	460	-274
					1-Propana	mine	; ·				
250	-1910	270	-1440	290	-1136	300	-1018	320	-834	340	600
											-698
260	-1650	280	-1277	298.15	5 -1038	310	-918	330	-761	350	-643
					2-Propana	mina					
					2-1 10 harra	пппе	i				
250	-1470	270	-1132	290	-898	300	-809	320	-668	340	-564
260	-1287	280	-1004	298.15		310	-733	330	-612	350	-522
								200		300	
-											

2.5. Enthalpy of Vaporization or Sublimation

Enthalpies of vaporization from the literature were tested for consistency through the Claperyon equation with our selections of vapor pressure, liquid density, and second virial coefficient data. Values listed are the molar enthalpy of vaporization from the condensed phase x to the ideal gas $\Delta_x^{g,id}H$ rather than to the saturated vapor Δ_x^gH . The selection of values was made from the combined data. Recommended values are listed in Table 10.

2.6. Enthalpy of Combustion and Formation

The enthalpies of combustion were usually available for

the substances in the condensed phase (either liquid or crystal). Accepted values for the enthalpies of formation of the combustion products at 298.15 K, listed in Table 21 (1978-115), were used to derive enthalpies of formation. Enthalpies of vaporization and the second virial coefficients given in this report were used to derive enthalpies of formation for the ideal gas. The results were tested against values estimated from enthalpies of formation of related compounds. If the inconsistencies appeared to be too large and the experimental values were of suspected merit, the estimated values of the enthalpies of formation were adopted. Recommended values of enthalpies of formation in the condensed and ideal gas state at 298.15 K are listed in Table 11.

TABLE 10. Enthalpy of vaporization or sublimation and conversion to the ideal gas at 298.15 K

Compound	phase x	$\Delta_x^{\mathbf{g},\mathrm{id}} H^a/\mathrm{kJ}\cdot\mathrm{mol}^{-1}$
Methanamine	l	$24.74{\pm}0.10$
Ethanamine	l	$26.66{\pm}0.20$
1-Propanamine	l	$31.37{\pm}0.10$
2-Propanamine	l	$28.57 {\pm} 0.10$
Benzenamine	l	$55.83 {\pm} 0.10$
2-Methylbenzenamine	l	$62.7 {\pm} 0.5$
3-Methylbenzenamine	l	$62.7 {\pm} 0.5$
4-Methylbenzenamine	s	$78.8 {\pm} 0.5$

^a Uncertainties are standard error estimates.

TABLE 11. Selected enthalpies of formation a,b at 0 and 298.15 K for the ideal gas and condensed phases.

	Ide	al gas	liquid or crystal		
Temperature	0 K	298.15 K	298.15	K	
Compound	$\Delta_f H^{\circ}/\mathrm{kJ}\cdot\mathrm{mol}^{-1}$			phase ^c	
Methanamine	-7.82 ± 0.41	$-22.53{\pm}0.41$	-47.27 ± 0.40	l	
Ethanamine	$\mathbf{-26.65} \pm 0.51$	-47.47 ± 0.51	-74.13 ± 0.50	l	
1-Propanamine	$\mathbf{-42.36} \pm 0.39$	$-70.10 {\pm} 0.39$	$-101.47{\pm}0.38$	l	
2-Propanamine	-56.90 ± 0.68	-83.70 ± 0.68	$-112.27{\pm}0.67$	l	
Benzenamine	-65.58 ± 0.81	87.46 ± 0.81	31.63 ± 0.80	l	
2-Methylbenzenamine	84.28 ± 2.1	56.4 ± 2.0	-6.3 ± 2.1	l	
3-Methylbenzenamine	$\textbf{83.37} \pm \textbf{2.1}$	54.6 ± 2.0	-8.1 ± 2.1	l	
4-Methylbenzenamine	83.96 ± 2.1	55.3 ± 2.0	-23.5 ± 2.1	s	

^a for formation reactions $nC(graphite) + (m/2)H_2(g) + (1/2)N_2(g) \rightarrow C_nH_mN(s,l, or g)^c$

2.7. Condensed Phase Heat Capacities and Related Thermal Properties

Where calorimetric data for the condensed phases were available to near 10 K, the dimensionless thermodynamic

functions C_{sat}/R , $\Delta_0'S/R$, $\Delta_0'G/RT$ and Δ_0^TH/RT along the vapor saturation lines were derived from numerical integrations of the heat-capacity data and from the enthalpies of transition. The results are listed in Table 12.

^b uncertainties are two standard error estimates.

c s for crystal, l for liquid, and g for gas.

TABLE 12. Thermodynamic properties for the condensed phases at vapor saturation. a

T	$rac{C_{ extsf{sat}}}{R}$	$\frac{\Delta_0^T S}{R}$	$rac{-\Delta_0^T G}{RT}$	$\frac{\Delta_0^T H}{RT}$
	,	Methanamine (cII)		
0	0.000	0.000	0.000	0.000
10	0.068	0.023	0.006	0.017
15	0.224	0.076	0.019	0.057
20	0.497	0.174	0.044	0.129
25	0.813	0.319	0.084	0.235
30	1.168	0.498	0.138	0.360
35	1.546	0.705	0.204	0.502
40	1.935	0.937	0.281	0.657
45	2.322	1.188	0.367	0.820
50	2.659	1.450	0.462	0.988
60	3.279	1.989	$\boldsymbol{0.672}$	1.317
70	3.841	2.539	0.899	1.640
80	4.272	3.080	1.138	1.942
90	4.729	3.609	1.383	2.226
100	5.181	4.132	1.632	2.500
101.469	5.209	4.207	1.669	2.539
	•	Methanamine (cI)		
101.469	5.185	4.367	1.669	2.698
110	5.447	4.796	1.895	2.901
120	5.716	5.282	2.157	3.125
130	5.973	5.749	2.416	3.334
140	6.162	6.200	2.670	3.530
150	6.431	6.633	2.920	3.713
160	6.664	7.055	3.165	3.890
170	6.914	7.467	3.406	4.061
179.708	7.170	7.858	3.636	4.222
2.0		Methanamine (l)	0.000	1.222
179.708	11.960	11.963	3.636	8.327
180	11.957	11.982	3.650	8.332
190	11.905	12.627	4.105	8.521
200	11.952	13.239	4.547	8.692
210	12.045	13.824	4.975	8.850
220	12.077	14.385	5.390	8.995
230	12.258	14.926	5.793	9.134
240	12.212	15.447	6.184	9.134 9.263
250	12.174	15.944	6.565	9.203 9.379
260	12.174	16.426	6.935	9.491
270	12.111	16.880	7.295	
280	12.111	17.323		9.585
290 290			7.645	9.678
298.15	12.264	17.753	7.986	9.767
	12.279	18.093	8.258	9.836
300	12.282	18.169	8.319	9.851

^a The percentage imprecision in the listed properties is 2 for 10 to 50 K and 0.2 above 50 K.

TABLE 12. Continued.a

T K	C _{sat} R	$\frac{\Delta_0^T S}{R}$	$\frac{-\Delta_{0}^TG}{RT}$	$\frac{\Delta_0^T H}{RT}$
		1 Proposanino (a	.)	
0	0.000	1-Propanamine (c	0.000	0.000
10	0.138	0.046	0.012	0.035
15	0.138	0.154	0.012	0.116
20	0.874	0.134	0.040	0.110
25	1.381	0.585	0.162	0.423
30	1.899	0.883		0.626
35	2.410		0.257	
40	2.410 2.900	1.214 1.569	0.369 0.497	0.844 1.071
45	3.355	1.936	0.637	1.300
50	3.786	2.312	0.785	1.527
60	4.580	2.312 3.075	1.103	1.971
70	5.266	3.832	1.439	2.394
80	5.879			2.792
90	6.434	4.577 5.301	1.785 2.136	3.166
100	6.947	6.007	2.130 2.487	3.519
110	7.429	6.691	2.839	3.852
120	7.894	7.358	3.188	4.170
130	8.338	8.008	3.534	4.474
140	8.786	8.642	3.876	4.766
150	9.251	9.264	4.215	5.049
160	9.751	9.876	4.550	5.327
170	10.303	10.484	4.881	5.603
180	10.951	11.091	5.208	5.882
188.389	11.516	11.601	5.480	6.119
100.000	11.010	1-Propanamine (l		0.110
188.389	18.482	18.606	5.480	13.126
190	18.512	18.766	5.595	13.171
200	18.683	19.717	6.274	13.443
210	18.814	20.633	6.938	13.694
220	18.923	21.514	7.582	13.930
230	19.021	22.354	8.206	14.149
240	19.103	23.165	8.810	14.355
250	19.174	23.951	9.404	14.546
260	19.245	24.701	9.977	14.726
270	19.314	25.431	10.536	14.895
280	19.387	26.131	11.079	15.054
290	19.470	26.815	11.613	15.205
298.15	19.549	27.354	12.035	15.322
300	19.569	27.475	12.126	15.349
310	19.677	28.119	12.634	15.487
320	19.807	28.748	13.127	15.619
330	19.961	29.357	13.611	15.748
340	20.146	29.956	14.084	15.876

^a The percentage imprecision in the listed properties is 2 for 10 to 50 K, and 0.2 above 50 K.

TABLE 12. Continued.a

K	$rac{C_{\mathtt{sat}}}{R}$	$\frac{\Delta_0^T S}{R}$	$rac{-\Delta_0^T G}{RT}$	$\frac{\Delta_0^T H}{RT}$
		2-Propanamine (<i>a)</i>	
0	0.000	0.000	0.000	0.000
10	0.270	0.092	0.023	0.068
15	0.746	0.290	0.076	0.212
20	1.299	0.577	0.163	0.414
25	1.859	0.926	0.280	0.647
30	2.381	1.312	0.419	0.893
35	2.858	1.716	0.576	1.140
40	3.287	2.126	0.744	1.382
45	3.669	2.536	0.920	1.615
50	4.022	2.941	1.102	1.839
60	4.022 4.661	3.732	1.475	2.257
70				
	5.221	4.493	1.852	2.640
80	5.749	5.225	2.228	2.997
90	6.254	5.931	2.601	3.330
100	6.756	6.617	2.968	3.648
110	7.257	7.284	3.330	3.953
120	7.751	7.936	3.687	4.249
130	8.266	8.577	4.038	4.538
140	8.809	9.209	4.385	4.824
150	9.399	9.836	4.728	5.109
160	10.070	10.464	5.067	5.397
170	10.878	11.098	5.403	5.695
178.011	11.551	11.613	5.670	5.942
		2-Propanamine (!)	
178.011	17.576	16.558	5.670	10.892
180	17.646	16.759	5.796	66.878
190	17.978	17.719	6.395	11.325
200	18.265	18.650	6.983	11.664
210	18.511	19.546	7.562	11.986
220	18.721	20.411	8.125	12.287
230	18.895	21.247	8.679	12.572
240	19.033	22.058	9.222	12.837
250	19.154	22.838	9.750	13.089
260	19.265	23.588	10.264	13.323
270	19.374	24.319	10.772	13.546
280	19.483	25.024	11.270	13.756
290	19.601	25.713	11.758	13.955
298.15	19.710	26.256	12.146	14.111
300	19.735	26.378	12.231	14.146
310	19.879	27.027	12.699	14.328
320	20.038	27.661	13.157	14.504

^a The percentage imprecision in the listed properties is 2 for 10 to 50 K, and 0.2 above 50 K.

TABLE 12. Continued.a

$\frac{T}{K}$	$rac{C_{\mathtt{sat}}}{R}$	$rac{\Delta_{0}^{T}S}{R}$	$rac{-\Delta_{f 0}^T G}{RT}$	$rac{\Delta_0^T H}{RT}$
		antina ayan ayan ayan ayan in ayan ayan aya		and the second s
		Benzenamine (c)		
0	0.000	0.000	0.000	0.000
10	0.159	0.053	0.013	0.040
15	0.508	0.176	0.045	0.132
20	1.037	0.393	0.103	0.290
25	1.586	0.683	0.189	0.494
30	2.137	1.023	0.299	0.724
35	2.628	1.391	0.429	0.963
40	3.030	1.772	0.573	1.200
45	3.490	2.156	0.727	1.429
50	3.831	2.543	0.889	1.653
60	4.443	3.298	1.228	2.070
70	4.952	4.022	1.576	2.446
80	5.423	4.713	1.925	2.788
90	5.883	5.379	2.272	3.107
100	6.279	6.020	2.615	3.405
110	6.724	6.639	2.953	3.686
120	7.181	7.243	3.286	3.958
130	7.615	7.834	3.613	4.222
140	8.106	8.417	3.935	4.482
150	8.623	8.994	4.253	4.741
160	9.130	9.567	4.567	4.999
170	9.701	10.138	4.878	5.259
180	10.259	10.708	5.186	5.521
190	10.843	11.278	5.492	5.786
200	11.429	11.849	5.796	6.054
210	12.035	12.421	6.097	6.324
220	12.680	12.996	6.398	6.598
230	13.321	13.573	6.697	6.876
240	13.969	14.154	6.996	7.158
250	14.582	14.737	7.294	7.443
260	15.177	15.320	7.591	7.729
267.133	15.570	15.736	7.803	7.933

The percentage imprecision in the listed properties is 2 for 10 to 50 K, and 0.2 above 50 K.

TABLE 12. Continued.a

$\frac{T}{K}$	$rac{C_{\mathtt{Sat}}}{R}$	$\frac{\Delta_0^T S}{R}$	$rac{-\Delta_{0}^{T}G}{RT}$	$rac{\Delta_{f 0}^T H}{RT}$
	-			
		Benzenamine (l)		
267.133	22. 511	20.482	7.803	12.679
270	22.525	20.722	7.939	12.783
280	22.699	21.544	8.410	13.133
290	22.818	22.343	8.877	13.466
298.15	23.082	22.979	9.254	13.725
300	23.109	23.122	9.339	13.783
310	23.328	23.882	9.796	14.086
320	23.65 7	24.628	10.248	14.380
330	23.892	25.360	10.695	14.665
340	24.071	26.076	11.137	14.939
350	24.291	26.777	11.574	15.203
360	24.495	27.464	12.005	15.459
370	24.678	28.138	12.432	15.705
380	24.865	28.798	12.854	15.944
390	25.053	29.447	13.272	16.175
400	25.241	30.083	13.684	16.399
410	25.427	30.709	14.092	16.617
420	25.738	31.327	14.495	16.833
430	25.831	31.934	14.893	17.041
440	25.925	32.529	15.287	17.242
450	26.019	33.112	15.677	17.436
460	26.113	33.685	16.062	17.623

^a The percentage imprecision in the listed properties is 2 for 10 to 50 K, and 0.2 above 50 K.

2.8. Ideal Gas Thermal Functions

The thermodynamic properties of the ideal gas were calculated from spectroscopically derived data with standard statistical mechanical methods for a rigid-rotor, harmonic-oscillator molecular model with modifications for internal rotations and inversion about the nitrogen atom. The ideal gas thermodynamic properties in dimensionless units (i.e., divided by R) include heat capacity (C_p°/R), entropy $\Delta_0^T S^{\circ}/R$, Gibbs energy function $\Delta_0^T G^{\circ}/RT$, enthalpy func-

tion $\Delta_0^I H^\circ / RT$, enthalpy of formation $\Delta_j H^\circ / RT$, and Gibbs energy of formation $\Delta_j G^\circ / RT$. Calculations were made from 0 to 1500 K at a standard state pressure of 0.1 MPa. Wherever possible, the calculated entropies and heat capacities were compared with those derived from calorime tric measurements.

The calculated results are listed in Table 13. Details of the calculations and the selection of the spectroscopic data are given in Section 3.8.

TABLE 13. Thermodynamic properties for the ideal gas at 0.1 MPa.

$^{T}_{ ext{K}}$	$\frac{-\Delta_0^T G^{\circ}}{RT}$	$\frac{\Delta_0^T H^o}{RT}$	$\frac{\Delta_0^T S^{\circ}}{R}$	$\frac{C_p^o}{R}$	$\frac{\Delta_{\mathbf{f}}H^{\mathbf{o}}}{RT}$	$rac{\Delta_{\mathbf{f}}G^{\mathbf{o}}}{RT}$
			Methanami	ne		
0	0.000	0.000	0.000	0.000	infinite	infinite
50	16.872	4.014	20.885	4.029	-24.776	-13.89
100	19.672	4.096	23.767	4.364	-16.150	0.094
150	21.360	4.248	25.609	4.733	-12.628	5.889
200	22.605	4.413	27.018	5.091	-10.830	9.250
273.16	24.019	4.679	28.698	5.751	-9.418	12.397
298.15	24.433	4.780	29.212	6.020	-9.088	13.205
300	24.462	4.787	29.250	6.041	-9.066	13.261
400	25.901	5.248	31.149	7.237	-8.072	15.724
500	27.127	5.766	32.893	8.426	-7.320	17.442
600	28.226	6.300	34.526	9.493	-6.688	18.719
700	29.236	6.825	36.061	10.429	-6.136	19.708
800	30.181	7.32 8	37.509	11.251	-5.645	20.494
900	31.072	7.805	38.877	11.976	-5.205	21.133
1000	31.918	8.255	40.172	12.615	-4.807	21.661
1100	32.724	8.677	41.402	13.179	-4.448	22.067
1200	33.497	9.074	42.570	13.676	-4.123	22.475
1300	34.238	9.445	43.682	14.113	-3.828	22.793
1400	34.950	9.792	44.743	14.498	-3.561	23.067
1500	35.637	10.117	45.755	14.836	-3.318	23.304
			Ethanamin	e		
0	0.000	0.000	0.000	0.000	infinite	infinite
50	19.102	4.297	23.399	4.826	-73.077	-55.33
100	22.214	4.699	26.913	5.396	-41.865	-16.53
150	24.185	5.047	29.232	6.094	-30.552	-1.99
200	25.685	5.400	31.085	6.837	-24.820	5.927
273.16	27.448	5.951	33.399	8.117	-20.221	12.914
298.15	27.978	6.152	34.130	8.604	-19.149	14.634
300	28.016	6.168	34.183	8.640	-19.076	14.752
400	29.908	7.039	36.946	10.663	-16.006	19.785
500	31.576	7.955	39.531	12.529	-13.933	23.121
600	33.107	8.853	41.960	14.121	-12.373	25.518
700	34.536	9.705	44.241	15.470	-11.127	27.328
800	35.885	10.500	46.384	16.633	-10.093	28.744
900	37.164	11.239	48.404	17.653	-9.213	29.881
1000	38.385	11.927	50.311	18.557	-8.450	30.811
1100	39.552	12.567	52.118	19.362	-7.781	31.514
1200	40.671	13.163	53.834	20.079	-7.187	32.236
1300	41.747	13.720	55.467	20.717	-6.658	32.790
1400	42.783	14.241	57.024	21.285	-6.182	33.265
1500	43.782	14.728	58.510	21.791	-5.754	33.677

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TABLE 13. Continued.

$^{T}_{ m K}$	$rac{-\Delta_{0}^{T}G^{\mathrm{o}}}{RT}$	$\frac{\Delta_0^T H^o}{RT}$	$rac{\Delta_{f 0}^T S^{f o}}{R}$	$\frac{C_p^o}{R}$	$rac{\Delta_{\mathbf{f}}H^{\mathbf{o}}}{RT}$	$rac{\Delta_{\mathbf{f}}G^{\mathbf{o}}}{RT}$
			1-Propanan	ine		
			-			
0	0.000	0.000	0.000	0.000	infinite	infinite
50	22.591	4.173	26.763	4.618	-114.285	-90.542
100	25.647	4.743	30.390	$\boldsymbol{6.022}$	-64.391	-30.311
150	27.692	5.384	33.076	7.273	-46.437	-8.067
200	29.325	5.998	35.324	8.413	-37.322	3.918
273.16	31.326	6.886	38.212	10.267	-29.986	14.356
298.15	31.942	7.199	39.141	10.965	-28.278	16.902
300	31.987	7.222	39.209	11.018	-28.162	17.076
400	34.242	8.533	42.775	13.910	-23.298	24.455
500	36.291	9.883	46.174	16.600	-20.056	29.286
600	38.210	11.201	49.412	18.929	-17.638	32.719
700	40.032	12.452	52.483	20.924	-15.715	35.289
800	41.772	13.621	55.393	22.646	-14.122	37.280
900	43.440	14.709	58.148	24.141	-12.769	38.864
1000	45.042	15.718	60.761	25.442	-11.598	40.147
1100	46.585	16.655	63.240	26.576	-10.573	41.097
1200	48.072	17.524	65.596	27.563	-9.668	42.083
1300	49.507	18.330	67.837	28.424	-8.865	42.825
1400	50.893	19.078	69.971	29.175	-8.147	43.455
1500	52.233	19.774	72.007	29.832	-7.505	43.995
			2-Propanam	ine		
0	0.000	0.000	0.000	0.000	infinite	infinite
50	20.409	4.137	24.546	4.615	-149.316	-123.356
100	23.465	4.795	28.260	6.261	-81.836	-45.626
150	25.548	5.525	31.073	7.676	-57.961	-17.588
200	27.234	6.228	33.462	8.992	-45.842	-2.739
273.16	29.324	7.235	36.559	11.011	-36.043	9.952
298.15	29.972	7.581	37.554	11.732	-33.764	13.003
300	30.019	7.607	37.627	11.786	-33.609	13.211
400	32.400	9.012	41.412	14.643	-27.193	21.923
500	34.561	10.401	44.962	17.202	-23.038	27.517
600	36.575	11.721	48.296	19.379	-20.035	31.438
700	38.476	12.951	51.426	21.233	-17.715	34.346
800	40.280	14.088	54.368	22.831	-15.842	36.584
900	42.001	15.139	57.140	24.222	-14.283	38.358
1000	43.647	16.109	59.756	25.438	-12.957	39.792
1100	45.225	17.007	62.232	26.501	-11.812	40.867
1200	46.741	17.837	64.578	27.430	-10.813	41.956
1300	48.199	18.607	66.807	28.243	-9.933	42.787
1400	49.605	19.321	68.926	28.954	-9.154	43.493
1500	50.961	19.985	70.946	29.577	-8.460	44.101

TABLE 13. Continued.

T K	$rac{-\Delta_0^T G^{\mathbf{o}}}{RT}$	$rac{\Delta_0^T H^o}{RT}$	$\frac{\Delta_0^T S^{\mathbf{o}}}{R}$	$\frac{C_p^o}{R}$	$rac{\Delta_{\mathrm{f}} H^{\mathrm{o}}}{RT}$	$rac{\Delta_{\mathrm{f}}G^{\mathrm{o}}}{RT}$
			Benzenami	ne		
	0.000	0.000	0.000			
0	0.000	0.000	0.000	0.000	infinite	infinite
50	21.881	4.288	26.169	4.323	-166.485	-151.393
100	24.887	4.461	29.349	5.160	-89.048	-65.698
150	26.781	4.955	31.735	6.796	-62.329	-35.359
200	28.298	5.655	33.953	8.756	-48.823	-19.462
273.16	30.240	6.902	37.143	11.896	-37.845	-6.033
298.15	30.864	7.367	38.231	12.982	-35.280	-2.836
300	30.910	7.401	38.311	13.062	-35.106	-2.618
400	33.303	9.337	42.639	17.127	-27.886	6.404
500	35.593	11.245	46.838	20.505	-23.262	12.097
600	37.803	13.021	50.823	23.195	-19.987	16.033
700	39.933	14.633	54.566	25.344	-17.515	18.920
800	41.983	16.085	58.069	27.096	-15.564	21.126
900	43.955	17.392	61.346	28.550	-13.976	22.865
1000	45.849	18.571	64.420	29.776	-12.652	24.267
1100	47.670	19.638	67.308	30.820	-11.529	25.208
1200	49.421	20.608	70.029	31.716	-10.563	26.380
1300	51.106	21.493	72.599	32.489	-9.724	27.191
1400	52.729	22.303	75.032	33.158	-8.989	27.884
1500	54.293	23.046	77.340	33.740	-8.341	28.482
		2 -]	Methylbenzen	amine		
0	0.000	0.000	0.000	0.000	infinite	infinite
50	22.945	4.464	27.409	4.872	189.934	213.153
100	26.186	4.999	31.185	6.398	87.584	121.326
150	28.362	5.826	34.188	8.600	54.762	92.940
200	30.170	6.809	36.979	10.930	38.562	79.630
273.16	32.522	8.382	40.904	14.450	25.661	69.732
298.15	33.280	8.941	42.22 1	15.661	22.751	67.612
300	33.335	8.983	42.318	15.750	22.557	67.472
400	36.231	11.262	47.494	20.366	14.920	62.146
500	38.986	13.492	52.478	24.326	10.666	59.315
600	41.633	15.576	57.209	27.564	8.066	57.618
700	44.179	17.484	61.663	30.207	6.382	56.511
800	46.629	19.215	65.844	32.392	5.248	55.737
900	48.984	20.784	69.768	34.224	4.464	55.167
1000	51.249	22.208	73.457	35.778	3.912	54.727
1100	53.427	23.503	76.930	37.105	3.516	54.127
1200	55.524	24.685	80.209	38.245	3.228	54.081
1300	57.543	25.767	83.310	39.228	3.015	53.831
1400	59.489	26.760	86.249	40.080	2.856	53.614
1500	61.367	27.673	89.040	40.820	2.733	53.421

TABLE 13. Continued.

$\frac{T}{ ext{K}}$	$rac{-\Delta_{f 0}^T G^{f o}}{RT}$	$\frac{\Delta_0^T H^o}{RT}$	$\frac{\Delta_0^T S^{\circ}}{R}$	$\frac{C_p^o}{R}$	$\frac{\Delta_{\mathrm{f}} H^{\circ}}{RT}$	$rac{\Delta_{\mathrm{f}}G^{\mathrm{o}}}{RT}$				
						· · · · · · · · · · · · · · · · · · ·				
3-Methylbenzenamine										
0	0.000	0.000	0.000	0.000^{-}	infinite	infinite				
50	23.784	4.784	28.568	4.805	188.679	210.739				
100	27.135	4.975	32.110	5.815	86.772	119.590				
150	29.255	5.582	34.838	7.860	53.994	91.521				
200	30.974	6.441	37.415	10.203	37.800	78.431				
273.16	33.197	7.932	41.130	13.837	24.923	68.769				
298.15	33.915	8.480	42.395	15.090	22.026	66.713				
300	33.968	8.521	42.489	15.183	21.832	66.577				
400	36.729	10.793	47.521	19.941	14.253	61.452				
500	39.380	13.041	52.421	23.999	10.058	58.764				
600	41.947	15.153	57.100	27.309	7.512	57.172				
700	44.431	17.088	61.519	30.002	5.873	56.147				
800	46.829	18.846	65.675	32.225	4.780	55.438				
900	49.142	20.439	69.581	34.087	4.031	54.921				
1000	51.372	21.884	73.256	35.662	3.510	54.525				
1100	53.520	23.200	76.720	37.007	3.141	53.962				
1200	55.591	24.400	79.991	38.161	2.877	53.947				
1300	57.588	25.497	83.086	39.156	2.685	53.725				
1400	59.515	26.504	86.020	40.016	2.544	53.532				
1500	61.376	27.431	88.806	40.764	2.438	53.359				
		4-1	Methylbenzer	namine						
0	0.000	0.000	0.000	0.000	infinite	infinite				
50	23.079	4.767	27.846	4.730	190.079	212.861				
100	26.413	4.959	31.373	5.855	87.465	121.020				
150	28.533	5.593	34.126	7.937	54.477	92.716				
200	30.258	6.469	36.726	10.279	38.182	79.502				
273.16	32.492	7.973	40.465	13.918	25.223	69.734				
298.15	33.213	8.524	41.737	15.173	22.308	67.652				
300	33.266	8.565	41.831	15 .2 66	22.113	67.515				
400	36.041	10.848	46.889	20.029	14.485	62.316				
500	38.706	13.102	51.808	24.081	10.261	59.580				
600	41.284	15.217	56.501	27.380	7.693	57.953				
700	43.778	17.152	60.930	30.062	6.038	56.901				
800	46.184	18.909	65.093	32.275	4.931	56.171				
900	48.505	20.500	69.005	34.128	4.171	55.637				
1000	50.741	21.943	72.684	35.697	3.639	55.227				
1100	52.895	23.256	76.151	37.036	3.262	54.652				
1200	54.970	24.453	79.424	38.186	2.990	54.627				
1300	56.972	25.549	82.520	39.176	2.791	54.397				
1400	58.902	26.553	85.456	40.034	2.644	54.195				
1500	60.766	27.478	88.244	40.779	2.532	54.016				
1000	00.100	21.410	00.244	40.119	2.332	94.010				

3. Data Sources

3.1. Freezing, Normal Boiling, and Critical Temperatures with Critical Pressure and Volume

3.1.1. Freezing and Normal Boiling Temperatures

The selected values of the normal boiling temperatures $(p_{\text{sat}} = 101.325 \text{ kPa})$ were determined from the least-squares fits to the Cox equation. If a reliable value for the triple-point temperature was available, this was selected rather than the freezing point, because unspecified impurities usually alter freezing points much more than the change that one atmosphere of nonreacting air over the sample would produce in establishing the difference between the freezing point and the triple point. In addition, prolonged exposure of an amine to air produces a significant amount of impurities which cannot be easily characterized. Measured values of the freezing and normal boiling temperature, along with estimated uncertainties are listed in Table 14.

Methanamine. Our selected value for the boiling temperature agrees with the results of Holmberg (1962-353), Aston et al. (1937-248), Hsia (1931-328), Plank and Vahl (1931-336), and Gibbs (1905-45) within our estimated uncertainties of those measurements. The value of Berthoud (1917-30) is about 1 K low, primarily due to inaccurate low pressure measurements. The majority of his measurements were at pressures much higher than atmospheric pressure.

The selected value of the freezing temperature was based primarily on the careful triple-point temperature determination of Aston *et al.* (1937-248) who used a well-characterized sample having an impurity of 0.025 mole %. The result of Timmermans and Mattaar (1921-17), although high, agrees with our recommendation to within the estimated uncertainty. The estimated uncertainty of 0.1 K given by Emeleus and Briscoe (1937-434) appears optimistic. Other measurements of the atmospheric boiling temperature, generally of lower accuracy, are listed in (1889-19), (1905-45), (1931-269), (1950-248), (1952-41), (1952-42).

Ethanamine. Our selected value for the boiling temperature agrees with the results of Timmermans (1912-127 and 1914-135), Lecat (1946-272), Holmberg (1962-353), Lempe et al. (1966-195) and Anderson and Shimanskaya (1969-163) within the respective estimated uncertainties. The selected freezing temperature was based primarily on the results of Timmermans (1914-135). The boiling temperature of Landenburg and Krugel (1900-32) is about 2 K higher than the selected value and their freezing temperature is about 2 K lower, both of which indicates an appreciable amount of low volatility impurity. Other measurements of the atmospheric boiling temperature, generally of lower accuracy, are listed in (1850-2), (1872-18), (1896-26), (1899-19), (1912-10), (1950-248).

1-Propanamine. Our selected value for the boiling temperature was based on the ebulliometric measurements of Osborn and Douslin (1968-206). It also agrees with that of Krichevtsov and Komarov (1970-165) within the limits of their uncertainty. The other published data are higher, which is consistent with the presence of involatile impurities in the samples. The selected value of the freezing tempera-

ture was based on the triple point temperature of Finke et al (1972-140). It agrees with the freezing temperature value of Vasil'ev et al. (1971-154) within the estimated uncertain ties; however, the value of Timmermans and Mattaar (1921 17) is almost 2 K higher. Other measurements of the atmospheric boiling temperature, generally of lower accuracy, are listed in (1862-2), (1869-15), (1872-26), (1882-30), (1886-28), (1889-26), (1895-49), (1896-5), (1900-73), (1919-64), (1924-82), (1948-262), (1949-167), (1950-248), (1951-569), (1952-42), (1952-385), (1968-195).

2-Propanamine. Our selected value for the boiling temperature agrees with the results of Osborn and Douslin (1968-206) within the estimated uncertainties. The presence of impurities probably account for the high values of Timmermans (1921-19), Costello and Bowden (1959-218) and Holmberg (1962-353). The selected value of the freezing temperature comes from the triple-point temperature value published by Finke et al. (1972-140) and is 6 K higher than the value published by Timmermans (1921-19), confirming a considerable impurity in the Timmermans sample. Other measurements of the atmospheric boiling temperature, generally of lower accuracy, are listed in (1895-49), (1909-1), (1949-166), (1949-167), (1968-195), (1970-5).

Benzenamine. The selected value of the boiling temperature agrees within the estimated uncertainties with the published results. The selected value of the freezing temperature was based upon the adiabatic calorimetric result for the triple-point temperature by Hatton et al. (1962-3) whose sample was 99.98 mole % pure. The agreement with other results listed are commensurate with the purities and accuracies of the temperature measurements. Other measurements of the atmospheric boiling temperature, generally of lower accuracy, are listed in (1850-10), (1884-15), (1888-39), (1896-28), (1902-64), (1912-127), (1914-135), (1914-136), (1916-232), (1920-95), (1923-73), (1924-167), (1926-91), (1930-279), (1935-68), (1937-254), (1941-332), (1944-125), (1946-272), (1950-531), (1954-670), (1954-674), (1960-289), (1962-363), (1965-333), (1966-203), (1979-93).

2-Methylbenzenamine. Our selected value for the boiling temperature agrees with the published results within the estimated uncertainties. The freezing temperatures are grouped about two distinct values, one around 249 K and the other around 257 K. The low values were ascribed to a metastable phase which melts at around 249 K. The selected value was based on the results of Timmermans (1921-19), (1952-50). Other measurements of the atmospheric boiling temperature, generally of lower accuracy, are listed in (1896-28), (1920-95), (1921-19), (1932-79), (1944-125), (1946-272), (1960-288), and (1951-569).

3-Methylbenzenamine. Our selected value for the boiling temperature agrees with the published results within the estimated uncertainties. The selected value of the freezing temperature was based on the results of Timmermans and Hennaut-Roland (1935-68). It is 0.8 K higher than that of Dreisbach and Martin (1949-120), but it agrees with the other published values within the estimated uncertainties. Other measurements of the atmospheric boiling temperature, generally of lower accuracy, are listed in (1896-28),

TABLE 14. Available freezing and normal boiling temperatures

T _b	$rac{\sigma(T_{ m b})^a}{ m K}$	$rac{T_{ m m}}{ m K}$	$\frac{\sigma(T_{ m m})^a}{ m K}$	Author(s)	Ref.
			Methana	amine	
266.45	0.5	_	~	Gibbs	1905-45
265.60	0.09	_	-	Berthoud	1917-30
_	_	180.65	1.0	Timmermans and Mattaar	1921-17
266.56	0.1		_	Plank and Vahl	1931-336
266.70	0.05	_	_	Hsia	1931-328
	_	179.70	0.07	McNeight and Smyth	1936-137
266.87	0.09	179.71^{b}	0.05	Aston et al.	1937-248
		180.05	0.3	Emeleus and Briscoe	1937-434
267.05	0.2	180.05	0.4	Roberts et al.	1939-387
266.65	0.2	_	-	Holmberg	1962-353
			Ethana	mine	
_	-	187.95	0.5	Landenburg and Krugel	1899-19
292.65	2.0	189.4	1.0	Landenburg and Krugel	1900-32
289.70	0.2	-	_	Timmermans	1910-58
289.70	0.2	***		Timmermans	1912-127
289.75	0.2	192.60	0.2	Timmermans	1914-135
_	_	189.99	0.2	Timmermans	1921-19
-	_	192.15	0.5	Pohland and Mehl	1933-369
289.75	0.2	192.15	0.3	Roberts et al.	1939-387
289.75	0.05	_		Lecat	1946-272
289.75	1.0	_	-	James	1952-42
289.75	0.5			Holmberg	1962-353
289.80	0.05		_	Lempe et al.	1966-195
290.15	1.0	_	~	Anderson and Shimanskaya	1969-163
			1-Propan	amine	
320.95	0.3	190.15	0.1	Timmermans and Mattaar	1921-17
322.4	0.2	_	_	Butler et al.	1935-366
322.85	0.5		~	Lecat	1946-272
322.15	1.0	-		Glaser and Rüland	1957-76
321.6	1.0	_		Costello and Bowden	1959-218
321.8	1.0	-	-	Holmberg	1962-353
321.65	0.5		_	Sudaricov et al.	1963-316
320.379	0.005	_	-	Osborn and Douslin	1968-206
321.0	1.0		_	Krichevtsov and Komarov	1970-165
	_	188.36	0.07	Vasil'ev et al.	1971-154
_	_	188.389^{b}	0.005	Finke et al.	1972-140

 $[^]a$ See section 1.6. b triple point temperature corrected to IPTS-68

TABLE 14. Continued.

$\frac{T_{\mathbf{b}}}{\mathbf{K}}$	$rac{\sigma(T_{ m b})^a}{ m K}$	$\frac{T_{\mathrm{m}}}{\mathrm{K}}$	$\frac{\sigma(T_{\mathbf{m}})^a}{K}$	Ref.	
			2-Propan	amine	
306.15	0.3	171.95	0.6	Timmermans	1921-19
304.8	0.5	_	_	Koob et al.	1951-62
306.0	1.0	_	-	Costello and Bowden	1959-21
307.15	1.5		_	Holmberg	1962-35
304.926	0.001		-	Osborn and Douslin	1968-20
305.01	0.2	_	_	Komarov and Krichevtsov	1969-16
_	-	178.019^{b}	0.005	Finke et al.	1972-14
			Benzena	mine	
_	_	267.05	0.1	Timmermans	1909-11
457.55	0.5	<u>-</u>	_	Timmermans	1910-58
_	_	266.95	0.05	Timmermans	1912-12
457.50	0.2	_	_	Knowles	1920-94
_	_	267.1	0.05	Lang	1928-19
457.45	0.5	_	_	Buehler et al.	1932-79
-	_	266.86	0.05	Parks et al.	1933-94
457.35	0.1		-	Green and Spinks	1945-17
457.05	0.1	266.85	0.05	Dreisbach and Martin	1949-12
_	_	267.01	0.1	Timmermans	1952-50
_	_	267.12	0.15	Witschonke	1954-24
_	_	266.6 1	0.1	Rock and Sieg	1955-60
_	_	267.13	0.07	McDonald et al.	1959-10
457.85	0.3	_	_	Costello and Bowden	1959-21
457.25	0.3	_	-	Ellis and Razavipour	1959-30
457.5	0.5	_	_	Sheveleva et al.	1959-30
457.09	0.5	_	-	Kurtyka	1961-26
457.03	0.15	_	_	Stadnicki	1962-32
-	-	267.133^{b}	0.005	Hatton et al.	1962-3
457.65	0.4	_		Katti and Chaudhri	1964-29
457.25	0.3	_	_	Campbell et al.	1968-21
-	_	267.10	0.05	Brunet and Gubbins	1969-16
457.65	0.5	267.65	0.4	Pawlowski and Wieckowska	1980-66

 $[^]a$ See section 1.6. b triple point temperature corrected to IPTS-68

TABLE 14. Continued.

$rac{T_{\mathbf{b}}}{\mathbf{K}}$	$rac{\sigma(T_{ m b})^a}{ m K}$	$rac{T_{ m m}}{ m K}$	$\frac{\sigma(T_{\mathbf{m}})^{a}}{\mathrm{K}}$	Ref.	
			2-Meth	ylbenzenamine	
-	_	257.7	0.7	Knoevenagel	1907-127
473.85	0.2	(248.8)	0.2	Timmermans	1914-135
-	-	256.75	0.3	Timmermans	1921-19
-	_	(248.75)	0.3	Timmermans	1921-19
472.85	0.5	-	_	Grimm and Patrick	1923-73
472.99	0.2	-	-	Berliner and May	1927-2
473.45	0.3	-	-	Lecat	1930-279
473.55	0.05	<u> </u>		Timmermans and Hennaut-Roland	1935-68
473.45	0.07	(249.47)	0.05	Dreisbach and Martin	1949-120
-	_	256.75	0.5	Timmermans	1952-50
473.35	0.3	_		Kurtyka	1961-263
473.35	0.5	-		Kurtyka and Kurtyka	1979-93
			3-Meth	ylbenzenamine	
~		242.15	0.4	O'Connor	1924-186
476.30	0.2	241.65	0.4	Dessart	1926-22
476.01	0.2	-	_	Berliner and May	1927-2
476.3	0.05	-	_	Timmermans	1927-21
476.35	0.3	-	-	Lecat	1930-279
476.15	0.5	_	-	Buehler et al.	1932-79
476.55	0.05	241.92	0.05	Timmermans and Hennaut-Roland	1935-68
476.2	0.1			Lecat	1943-221
476.49	0.07	242.75	0.05	Dreisbach and Martin	1949-120
_		241.9	0.3	Timmermans	1952-50
476.35	0.2		-	Glaser and Rüland	1957-76
			4-Meth	ylbenzenamine	
_	_	316.85	0.3	Cauwood and Turner	1915-45
473.5	0.2		_	Berliner and May	1927-2
473.65	0.3	_	•	Lecat	1930-279
_	_	316.55	0.4	Buehler et al.	1932-79
_	-	316.15	0.5	Bernouli and Veillon	1932-307
473.70	0.3	316.9	0.1	Timmermans and Hennaut-Roland	1937-146
_	_	317.15	0.5	Barcelo et al.	1951-569
473.55		_	-		1957-76
_	_	316.85			1963-367
473.55	0.2	316.85	0.4	Glaser and Rüland Rastogi <i>et al.</i>	

 $[^]a$ See section 1.6. () indicates the melting point of metastable form

(1946-272), and (1951-569).

4-Methylbenzenamine. Our selected value for the boiling temperature agrees with the published results within the estimated uncertainties. The selected value of the freezing temperature was based on the results of Timmermans and Hennaut-Roland (1937-146). Other measurements of the atmospheric boiling temperature, generally of lower accuracy, are listed in (1896-28), (1946-272), and (1944-125).

3.1.2. Critical Temperature, Pressure, and Volume

Both measured and estimated values of the critical temperature, pressure, and volume are listed in Table 15.

Methanamine. Vincent and Chappius (1886-11) determined the critical temperature and critical pressure of methanamine for a sample that was reported to be pure. Berthoud (1917-30) also determined the critical temperature and critical pressure using samples prepared by Kahlbaum by alkylation of ammonia and subsequently purified by fractional crystallization followed by a number of fractional distillations over barium oxide. Kay and Young (1974-179) reported Weaver's value of the critical temperature and critical pressure of methanamine. The selected values are those determined by Weaver. The critical volume was estimated by a procedure (1989-1) based on those of Lydersen (1955-593) and Ambrose (1979-58) and calculated from the rectilinear diameter. The rectilinear diameter value was selected because the method gave good agreement with literature critical volumes for ethanamine and 2-propanamine, where the liquid and vapor densities were measured close to the critical temperature.

Ethanamine. The critical temperature and critical pressure were determined by Vincent and Chappius (1886-11), and Berthoud (1917-30). Pohland and Mehl (1933-369) reported the critical temperature and density. The purity of the sample used by Vincent and Chappius is unknown. The samples used by Berthoud and by Pohland and Mehl were reported to be "pure." The selected critical pressure was that obtained by extrapolation of the Cox equation to the selected critical temperature. The selected value of the critical volume was based on the measurements of Pohland and Mehl (1933-369); they used their vapor density measurements to 451 K and their liquid density measurements to 410 K with unpublished data from I. G. Faben. The critical volume was calculated from the equation for the rectilinear line given by $\frac{1}{2}(\rho_I + \rho_v)/(\text{kg m}^{-3}) = 248.5$ and Mehl, Pohland $+261.7(1-T/T_c)$ (from 300 to 456.2 K), with our selected critical temperature.

1-Propanamine. The critical temperature and critical pressure of 1-propanamine were determined by Vincent and Chappius (1886-11) and by Berthoud (1917-30). The critical temperature determined by Berthoud was selected. The samples used by Berthoud were prepared by Kahlbaum with

methods discussed above for methylamine. The selected critical pressure was that obtained by extrapolation of the Cox equation to the selected critical temperature. The estimated critical volume (1989-1) differed by 9 cm³ mol from the value calculated from the rectilinear diameter. The latter value was selected.

2-Propanamine. The only values available for this compound are those determined by Kobe and Mathews (1970-5). The samples used by these authors were purified by distillation. The critical constants determined by them are selected.

Benzenamine. The critical temperature and pressure were determined by Guye and Mallet (1902-63). Kudchadker et al. (1968-31) noted that these values have a considerable uncertainty. The experimental values agree with the estimated values (1989-1). The selected critical pressure was that obtained by extrapolation of the Cox equation to the experimental critical temperature. The selected critical volume was calculated from the rectilinear diameter, and this value disagrees considerably with the estimated value (1989-1).

2-Methylbenzenamine. The critical temperature and critical pressure of this compound were determined by Glaser and Rüland (1957-76). Their pressure seems inordinately low, but it roughly corresponds to the vapor pressure at their reported critical temperature, which is 13 K below our selected value. We deemed these values unreliable as they differ considerably from predicted values. The selected critical temperature was estimated by Somayajulu (1989-1). The selected critical pressure was that obtained by extrapolation of the Cox equation to the selected critical temperature. The selected critical volume was calculated from the rectilinear diameter.

3-Methylbenzenamine. The critical temperature and critical pressure determined by Glaser and Rüland (1957-76) were considered unreliable. The selected value of the critical temperature was estimated by Somayajulu (1989-1). The agreement between the experimental and the estimated values of p_{ϵ} and T_{ϵ} is somewhat better than that for 2-methylbenzenamine. The selected critical pressure was that obtained by extrapolation of the Cox equation to the selected critical temperature. The selected critical volume was calculated from the rectilinear diameter.

4-Methylbenzenamine. Both the critical temperature and critical pressure determined by Glaser and Rüland (1957-76) disagree with estimated values (1979-58), (1989-1). The calculated value of the pressure from the Cox equation at the experimental critical temperature is significantly higher than the experimental value of the critical pressure. The estimated critical temperature (1989-1) was selected. The selected critical pressure was obtained from the Cox equation, and the selected critical volume was calculated from the rectilinear diameter.

TABLE 15. Measured and estimated critical properties.

T _c K	$\frac{\sigma(T_{ m c})^a}{ m K}$	р _с МРа	$rac{\sigma(p_{ m c})^a}{ m MPa}$	$rac{V_{ m c}}{{ m cm}^3 \cdot { m mol}^{-1}}$	$rac{\sigma(V_{ m c})^a}{{ m cm}^3 \cdot { m mol}^{-1}}$	Author(s)	Ref.
				Methana	mine		
428	2	7.30	0.3	~		Vincent and Chappius	1886-11
430	1	7.56	0.1	_	_	Berthoud	1917-30
430.7	0.2	7.614	0.015		_	Kay and Young	1974-18
130.8	0.5	7.65	0.05	138	10	Li and Kiran	1988-83
132.1^{b}	1.0^b	7.13^b	0.05 0.2^b	127^b	5^b	Somaya julu	1989-1
102.1	1.0	$7.532^{b,c}$	$0.2 \\ 0.03^{b,c}$	$120^{b,d}$	$6^{b,d}$	TRC – this work	1303-1
-	_	1.532	0.03-,-	120*,-	0-,-	Inc – tms work	
				Ethanar	nine		
150	10	6.69	1.0	-	_	Vincent and Chappius	1886-11
156.4	1	5.63	0.5	_	_	Berthoud	1917-30
156.2	1	_	_	181.4	5	Pohland and Mehl	1933-36
155^{b}	1.0^b	5.74^b	0.2^b	181.9^{b}	2^b	Somayajulu	1989-1
-	_	$5.63^{b,c}$	$0.11^{b,c}$	$177.6^{b,d}$	$5^{b,d}$	TRC - this work	
				1-Propana	amine		
491	10	5.07	1.0		_	Vincent and Chappius	1886-11
197	1	4.74	0.5	-	_	Berthoud	1917-30
197	1.5	4.73	0.2	_	_	Glaser and Rüland	1957-76
192^b	2^{b}	4.78^{b}	0.2^b	237^b	5^b	Somayajulu	1989-1
-	_	$4.72^{b,c}$	$0.08^{b,c}$	$228^{b,d}$	$11^{b,d}$	TRC - this work	1303-1
				2-Propana	amine		
171.9	0.5	4.54	0.05	22 1	5	Kobe and Mathews	1970-5
169^b	2^b	4.63^{b}	0.2^b	235^b	5^{b}	Somayajulu	1989-1
-	_	$4.54^{b,c}$	$0.06^{b,c}$	$233^{b,d}$	$11^{b,d}$	TRC - this work	2000 2
				Benzena	mine		
699	2	5.31	0.5	-	_	Guye and Mallet	1902-64
399	6	_	_		_	Livingston et al.	1980-5
599^b	2^b	5.3^b	0.2^b	293^b	5^b	Somayajulu	1989-1
	_	$4.89^{b,c}$	$0.12^{b,c}$	$280^{h,d}$	$14^{b,d}$	TRC – this work	-000 1
				2-Methylbens	zenamine		
694	2	3.75	0.3	_	_	Glaser and Rüland	1957-76
706 ^b	2^{b}	4.44^{b}	0.5^b	-	_	Ambrose	1979-58
707 ^b	$\frac{1}{2^b}$	4.58^{b}	0.1^b	348^b	5^b	Somayajulu	1989-1
	_	$4.37^{b,c}$	$0.12^{b,c}$	$333^{b,d}$	$17^{b,d}$	TRC – this work	1000-1

TABLE 15. Continued.

$rac{T_{ extbf{c}}}{ extbf{K}}$	$rac{\sigma(T_{ m c})^a}{ m K}$	$rac{p_{ m c}}{ m MPa}$	$rac{\sigma(p_{ m c})^a}{ m MPa}$	$\frac{V_{\rm c}}{{ m cm}^3 \cdot { m mol}^{-1}}$	$rac{\sigma(V_{ m c})^a}{{ m cm}^3 \cdot { m mol}^{-1}}$	Author(s)	Ref.
			3	-Methylbenzer	amine		
709	2	4.15	0.3	_	_	Glaser and Rüland	1957-76
706^b	2^b	4.17^b	0.5^b	_	_	Ambrose	1979-58
707^b	2^b	4.32^b	0.1^b	348^b	5^b	Somayajulu	1989-1
-	-	$4.28^{b,c}$	$0.12^{b,c}$	$333^{b,d}$	$17^{\boldsymbol{b},\boldsymbol{d}}$	TRC - this work	
			4	-Methylbenzer	namine		
667	5	2.38	0.7	_	_	Glaser and Rüland	1957-76
702^b	2^b	4.17^b	0.5^b	_		Ambrose	1979-58
706^b	2^b	4.45^b	0.1^b	348^b	$5^{m{b}}$	Somayajulu	1989-1
_	_	$4.58^{b,c}$	$0.14^{b,c}$	$340^{b,d}$	$17^{b,d}$	TRC - this work	

^a See section 1.6; ^b estimated values; ^c from Cox vapor pressure equation with selected T_c in Table 1;

3.2. Vapor Pressure

The temperature and pressure ranges over which measurements of vapor pressure have been reported are listed in Table 16. Also included are the method of measurement as well as the estimated accuracy in both the temperature and pressure. If the data were determined by an ebulliometric (dynamic) method these were given greater weight among measurements made on samples with equal purity and with equal accuracies. This preference arises because the ebulliometric methods expel light gases that may remain in the samples when they are subjected to static measurements. The smoothed vapor pressure values listed in Table 3 were calculated using the Cox equation [Eq. (3)]. The coefficients of the equation are listed in Table 2, and the coefficients of the Antoine and the extended Antoine equations [Eq. (4) and (5), respectively] are listed in Table 4 for the eight compounds involved in this study.

Methanamine. Felsing and Thomas (1929-227), Hsia (1931-328), Emeleus and Briscoe (1937-434) and Wolff et al. (1964-344 and 1968-205) used static methods to measure the vapor pressure of methanamine; owing to questions of the degree of outgassing, their data were excluded. Aston et al. (1937-248) used a highly purified sample (99.975 mole %) and a static method for measuring the vapor pressure. They showed their vapor pressure values were the same after 50 mole % of the sample was removed by distillation. Their data were given the highest weight. To cover temperatures up to the critical temperature, the data of Wolff et al. (1962-354) and of Berthoud (1917-30) were used but were given less weight than that of Aston et al. Percent deviations

of the experimental values from the vapor pressures calculated from the Cox equation are shown in Fig. 1.

Ethanamine. Bittrich et al. (1962-170) used an ebulliometric method to measure the vapor pressure at temperatures up to 288 K and a static method at higher temperatures. They used a static method in their later work (1963-320), and it was excluded from the fit.

Berthoud (1917-30) measured the vapor pressure between the boiling and the critical temperatures, and Wolff et al. (1964-344) measured the vapor pressure up to the boiling temperature using a static method. All these data were used in fitting the vapor pressure equations. The data by Pohland and Mehl (1933-369) and by Roberts et al. (1939-387) were excluded.

Percent deviations of the experimental values from the vapor pressures calculated from the Cox equation are plotted in Fig. 2.

1-Propanamine. For 1-propanamine the data by Glaser and Rüland (1957-76), by Srivastava et al. (1986-5), and isolated points from references (1941-101 and 1968-195) were excluded. All other available data were used but the data of Osborn and Douslin (1968-206) were given the highest weight while Berthoud's (1917-30) were given the lowest. Figure 3 shows that percent deviations from the vapor pressures calculated from the Cox equation are less than $\pm 1\%$ except for the data of Glaser and Rüland which showed deviations as much as -11% at 360 K. Their values were excluded from Fig. 3 to permit more resolution on the plot.

2-Propanamine. The low-temperature data (lower than 273 K) of Osborn and Douslin (1968-206) were measured by a static method using an inclined-piston apparatus. These

^d from fit to rectilinear diameter line with selected T_c in Table 1.

TABLE 16. Available vapor pressure data.

Range K	$\frac{\sigma(T)^a}{K}$	Range kPa	$\frac{\sigma_{\mathrm{c}}(p_{\mathrm{sat}})^a}{\mathrm{kPa}}$	$10^3 \cdot \sigma_f(p_{\mathrm{sat}})^a$	sl^b	Meth.c	Author(s) Re	f
				Methanamin	е			
266-370	0.05	96-2400	0.1	1.5	1	S	Berthoud	1917-
80-427	0.05	2500-7460	0.04	2.0	1	S	Berthoud	1917-
93-263	0.01	0.9 - 87	0.01	1.5	0	S	Felsing and Thomas	1929-
96-282	0.05	86-198	0.01	1.5	0	\mathbf{U}	Hsia	1931-
90-267	0.005	0.5 - 103	0.001	0.3	1	S	Aston et al.	1937-
16-263	0.01	5-86	0.01	1.5	0	S	Emeleus and Briscoe	1937-
18-293	0.1	6-292	0.01	1.5	i	S	Wolff and Hopfner	1962-
18-293	0.1	6-292	0.01	1.5	Ō	Š	Wolff et al.	1964-
53-293	0.1	53-292	0.01	1.5	0	S	Wolff and Wurtz	1968-
				Ethanamine				
88-404	0.05	96-2400	0.1	1.5	1	S	Berthoud	1917-
17-456.3	0.05	3000-5600	0.04	2.0	1	S	Berthoud	1917-
11-297	0.1	1-140	0.05	1.0	0	S	Pohland and Mehl	1933-
23-283	0.05	3 -78	0.03	2.0	0	S	Roberts et al.	1939-
75-288	0.05	50-93	0.1	2.0	1	E S	Bittrich et al.	1962-
97-323	0.05	130-326	0.1	2.0	1	S	Bittrich et al.	1962-
73-323	0.05	50-327	0.05	1.5	0	S	Bittrich et al.	1963-
18-293	0.1	1-116	0.01	1.5	1	S	Wolff et al.	1964-
				1-Propanamir	ie			
20-451	0.05	96-2400	0.1	1.5	1	S	Berthoud	1917-
60-496	0.05	2700-4740	0.04	2.0	1	S	Berthoud	1917-
22-485	0.5	101-4050	0.05	1.5	0	S	Glaser and Rüland	1957-
43-293	0.1	4-34	0.01	1.5	1	S	Wolff et al.	1964-
96-351	0.001	39-270	0.01	0.15	1	$ ilde{\mathbf{E}}$	Osborn and Douslin	1968-
97-348	0.005	42-250	0.01	1.0	0	S	Srivastava et al.	1986-
				2-Propanamir	ıe			
77-305	0.55	29-100	0.1	2.5	0	U	Colpy et al.	1941-1
13-243	0.001	0.4-4.5	0.0005	0.15	1	S	Osborn and Douslin	1968-2
13-334 05-471	$0.001 \\ 0.025$	0.4-270 100-4540	0.002 0	$0.15 \\ 1.5$	1 1	E S	Osborn and Douslin Kobe and Mathews	1968-2 1970 -
	0.020	100 1010	Ü	Benzenamin	_	5	Kobe and Mathews	1970 -
50-458	0.05	2-100	0.01	1.5	0	S	Ramsay and Young	1005
03-457	0.05	19-101	0.01	1.5	Õ	Š	Ramsay and Young	1885-2 1886-0
04-456	0.05	20-103	0.01	1.5	Õ	Š	Neubeck	1887-
16-457	0.01	0.1-101	0.05	1.0	ŏ	Š	Kahlbaum	1898-
04-457	0.2	20-101	0.05	2.0	ŏ	$\ddot{\mathbf{E}}$	Beckmann and Liesche	1915-
65-424	0.05	4-39	0.01	1.0	ĭ	$\ddot{\mathbf{E}}$	Garrick	1927-
73 643	0.1	149-2677	0.1	2.0	î	Ē	Lastovtsev	1937-
73-323	0.02	0.01-0.4	0.005	2.0	ō	$\mathbf{\tilde{G}}$	Gurevich and Sigalovskaya	1027
30-388	0.05	0.7-11	0.05	1.5	ŏ	Š	Gould et al.	1947-
86-457	0.01	10-101	0.05	1.5	ŏ	S	Dreisbach and Shrader	
24-353	0.02	0.4-2.4	0.007	2.0	Ö	S	Holtzlander and Riggle	1949-1
67-353	0.05	0.007-2.4	0.001	1.5	1	S		1955-0
63-457	0.01	3.8-101	0.015	1.5	0	S	Roeck and Sieg	1955-2
76-458	0.05	6.8-105	0.013	1.5	1	E E	Crutzen et al.	1957-4
38-457	0.01	53-101	0.07	1.5	0	E	McDonald et al.	1959-1
34-457	0.01	53-101 53-101	0.07	1.5	0	E	Stadnicki Stadnicki	1962-3
34-457	0.01	53-101 53-101	0.07	1.5		E.	Stadnicki	1962-3
34-457	0.01				0	E	Stadnicki	1962-3
34-451 13-453	0.01	53-101	0.07	1.5	1	E	Stadnicki	1963-3
エヴーズジン		0.3-88	0.1	2.0	0	S	Danov and Shinyaeva	1965-
	$0.05 \\ 0.01$	0.08-0.5	0.005	1.0	0	S	Pannetier et al.	1965-
98-323	41.111	0.05 - 1.1	0.005	1.0	0	S	Campbell et al.	1968-2
98-323 98-341		0 10 7 0	0.05					
98-323 98-341 08-371	0.5	0.13-5.3	0.05	2.0	0	S	Gopal and Rizvi	
98-323 98-341 08-371 13-387 77-393		0.13-5.3 0.25-10.5 0.02-13	0.05 0.003 0.003	2.0 0.35 0.35	0 0 1	S S S	Gopal and Rizvi Maher and Smith Maher and Smith	1968-2 1979-9 1980-2

TABLE 16. Continued.

Range K	$rac{\sigma(T)^a}{{ m K}}$	Range kPa	$rac{\sigma_{ m c}(p_{ m sat})^a}{ m kPa}$	$10^3 \cdot \sigma_f(p_{\mathrm{sat}})^a$	sl ^b	Meth.c	Author(s)	Ref.
				2-Methylbenz	enami	ine		
415-472 319-473 392-473 473-690	0.1 0.01 0.01 0.1	20-101 0.1-101 7.6-101 101-3500	0.1 0.05 0.05 0.05	5.0 1.0 1.5 2.0	0 1 1 1	S S E S	Neubeck Kahlbaum Dreisbach and Shrader Glaser and Rüland	1887-59 1898-2 1949-113 1957-76
				3-Methylbenze	enami	ne		
422-476 323-383 394-476 476-704	0.1 0.01 0.01 0.1	19-101 0.1-5 7.6-101 101-4050	0.1 0.05 0.05 0.05	5.0 1.0 1.5 2.0	0 1 1 1	S S E S	Neubeck Kahlbaum Dreisbach and Shrader Glaser and Rüland	1887-59 1898-2 1949-113 1957-76
				4-Methylbenz	enami	ne		
416-474 320-380 473-641	0.1 0.01 0.1	18-101 0.1-5 101-2026	0.1 0.05 0.05	5.0 1.0 2.0	0 1 1	S S S	Neubeck Kahlbaum Glaser and Rüland	1887-59 1898-2 1957-76

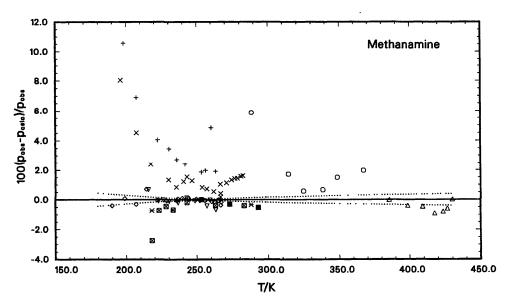


Fig. 1. Percent deviation of experimental vapor pressures for methanamine from the Cox equation. O, △ Berthoud (1917-30)*; + Felsing and Thomas (1929-227); ×Hsia (1931-328); ♦ Aston et al. (1937-248)*; ♥ Emeleus and 205); with * after reference number for data used in fitting.

 ^a See section 1.6.
 ^b 1 for data selected and 0 for data not selected for least squares fit.
 ^c Method of measurement: S, static; E, ebulliometric; G, gas saturation; and U, unspecified.

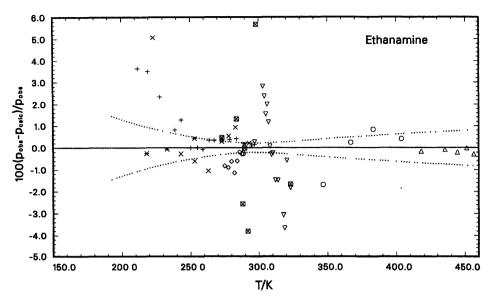


Fig. 2. Percent deviation of experimental vapor pressures for ethanamine from the Cox equation. O,Δ Berthoud (1917-30)*; + Pohland and Mehl (1933-369); ×Roberts et al. (1939-387); Bittrich et al. (1962-170)*, ◊ by dynamic method, ∇ static; ⊠ Bittrich et al. (1963-320); ×Wolff et al. (1964-344)*; with * after reference number for data used in fitting.

data were given lower weight than their higher temperature data which were obtained by an ebulliometric method. Kobe and Mathews (1970-5) only gave an equation for their measured values which were focused to determine the critical temperature; however, they did measure a near atmospheric

pressure boiling temperature that is in good agreement (0.04 kPa) with our recommended value. The data of Osborn and Douslin (1968-206) along with 16 values calculated at temperatures from 345 K to T_c for the data of Kobe and Mathews (1970-5) were used to fit the Cox equation. The distri-

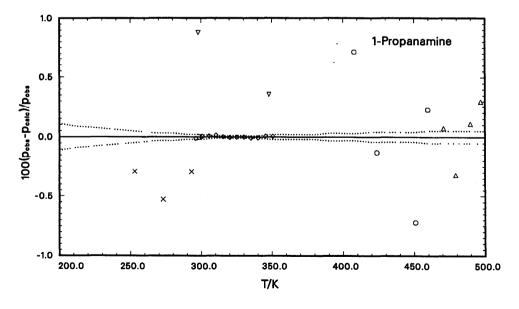


FIG. 3. Percent deviation of experimental vapor pressures for 1-propanamine from the Cox equation. O,Δ Berthoud (1917-30)*; ×Wolff et al (1964-344)*; Osborn and Doulsin (1968-206)*; ∇ Srivastava et al. (1986-5); with * after reference number for data used in fitting.

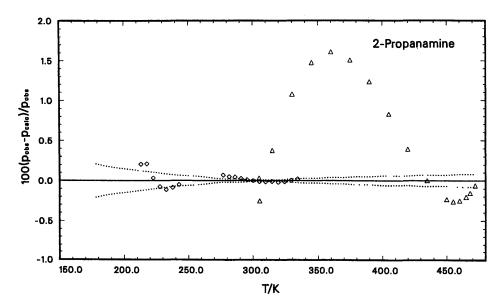


Fig. 4. Percent deviation of experimental vapor pressures for 2-propanamine from the Cox equation. ○ Colpy et al. (1941-101); △ Kobe and Mathews (1970-5)*; ♦ Osborn and Douslin (1968-206)*; with * after reference number for data used in fitting.

bution of the calculated values that were used is shown in Fig. 4.

Copley et al. (1941-101) reported vapor pressure data at 277.7 and 405.4 K. The purity and the method of measurement were not specified. Their vapor pressure values were 7.7 and 4% lower than those of Osborn and Douslin. The single point at 63.7 kPa reported in (1968-195) is in good agreement, 0.06%, with the selected values. The percent deviations of the experimental values from vapor pressures calculated from the Cox equation are shown in Fig. 4. Also shown are percent deviations from the Cox equation for 16 values calculated from the equation of Kobe and Mathews (1970-5).

Benzenamine. Many vapor pressure data have been reported for benzenamine in the last hundred years. In the nineteenth century, Ramsay and Young (1885-25, 1886-62 and 1887-58) and Kahlbaum (1898-2) measured the vapor pressure. Beckmann and Liesche (1915-88) used a sample of unspecified purity and their uncertainties were high. Holtzlander and Riggle (1955-604), and Crutzen et al. (1957-486) used static methods on samples of unspecified purities. Rock and Sieg (1955-2) and Gurevich and Sigalovskaya (1937-437) used gas saturation methods. Danov and Shinyaeva (1965-382), Gopal and Rizvi (1968-210), Gould et al. (1947-337), Campbell et al. (1968-211) and Dreisbach and Shrader (1949-113) used static methods, and their uncertainties were very high. The data of Maher and Smith (1979-94) were less precise than expected. The above mentioned data along with isolated points reported in references (1932-116, 1953-610, 1954-622, 1962-363, 1974-136) were not given weight in this evaluation.

Garrick (1927-156), Lastovtsev (1937-438), Mc-

Donald et al. (1959-109), and Stadnicki (1962-32, 1962-33, 1962-34, 1963-321) used ebulliometric methods in measuring the vapor pressure, and their data were used in this evaluation. However only one of the apparently repeated sets of data by Stadnicki was used. The data of Maher and Smith (1980-20) were also used; they used static methods on carefully purified and degassed samples. Percent deviations of the experimental values from those calculated from the Cox equation are shown in Fig. 5.

2-Methylbenzenamine. The data of Neubeck (1887-59) and the single point of reference (1921-19) were not used in the evaluation. The vapor pressures that Kahlbaum (1898-2) and Dreisbach and Shrader (1949-113) measured up to the boiling temperature and that Glaser and Rüland (1957-76) measured between the boiling and critical temperatures were selected for further evaluation. At low temperatures, the data of Dreisbach and Shrader were given higher weight than that of Kahlbaum, although the latter covered a wider range of temperature. The deviations of the experimental values from those calculated from the Cox equation are shown in Fig. 6. The data of Kahlbaum shows significant deviations at the lowest temperatures for this compound as well as for the other benzenamines considered in this work.

3-Methylbenzenamine. The data of Kahlbaum (1898-2) and Dreisbach and Shrader (1949-113) were used at low temperatures and the data of Glaser and Rüland (1957-76) were used at high temperatures. The data of Neubeck (1887-59) and the isolated point reported in reference (1921-19) were not used in the analysis. Percent deviations of the experimental vapor pressures from values calculated with the Cox equation are shown in Fig. 7.

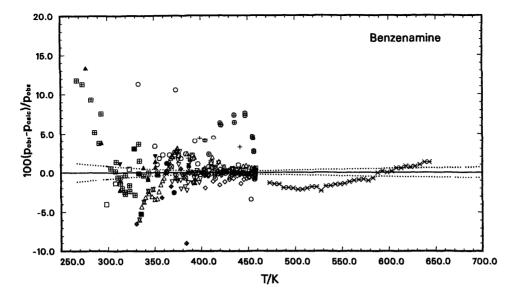


Fig. 5. Percent deviation of experimental vapor pressures for benzenamine from the Cox equation. ○ Ramsay and Young (1885-25); × Ramsay and Young (1886-62); ⊕ Ramsay and Young (1887-58); △ Kahlbaum (1898-2); ◇ Beckmann and Liesche (1915-88); ▽ Garrick (1927-156)*; × Lastovtsev (1937-438); ⊠ Gurevich and Sigalovskaya (1937-437); ◇ Gould et al. (1947-337); + Dreisbach and Shrader (1949-113)*; △ Holtzlander and Riggle (1955-604); □ Roeck and Sieg (1955-2)*; ⊗ Crutzen et al (1957-486); □ McDonald et al. (1959-109)*; ♦ Stadnicki (1962-32, 1962-33, 1962-34, 1963-321*); ○ Danov and Shinyaeva (1965-382); □ Pannetier et al. (1965-388); ■ Campbell et al. (1968-211); ● Gopal and Rizvi (1968-210); ▼ Maher and Smith (1979-94); ▲ Maher and Smith (1980-20)*; with * after reference number for data used in fitting.

4-Methylbenzenamine. The final evaluation was made with the measurements made by Kahlbaum (1898-2) up to the boiling temperature and by Glaser and Rüland (1957-76) between the boiling and critical temperatures. The re-

sults of Neubeck (1887-59) and the single point at 373 K (1895-49) were excluded. Percent deviations of experimental values from those calculated with the Cox equation are shown in Fig. 8.

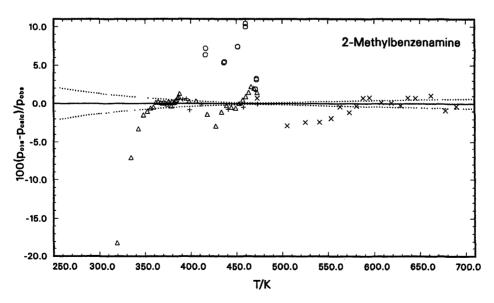


Fig. 6. Percent deviation of experimental vapor pressures for 2-methylbenzenamine from the Cox equation. O Neubeck (1887-59); Δ Kahlbaum (1898-2)*; + Dreisbach and Shräder (1949-113)*; ×Glaser and Rüland (1957-76)*; with * after reference number for data used in fitting.

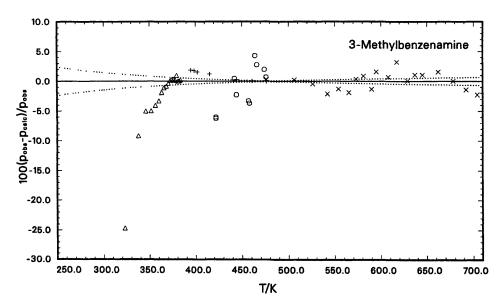


FIG. 7. Percent deviation of experimental vapor pressures for 3-methylbenzenamine from the Cox equation. O Neubeck (1887-59); \triangle Kahlbaum (1898-2)*; + Dreisbach (1949-113)*; \times Glaser and Rüland (1957-76)*; with * after reference number for data used in fitting.

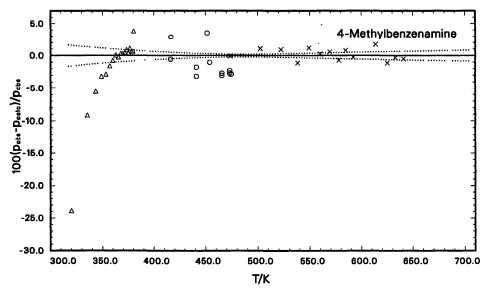


FIG. 8. Percent deviation of experimental vapor pressures for 4-methylbenzenamine from the Cox equation. O Neubeck (1887-59); \triangle Kahlbaum (1898-2)*; \times Glaser and Rüland (1957-76)*; with * after reference number for data used in fitting.

3.3. Saturated Liquid Density

The temperature and density ranges over which measurements of density have been reported are listed in Table 17. Also included are the estimated accuracies for both temperature and pressure along with the number of experimental determinations. For some compounds either vapor densities or rectilinear diameter lines were reported and are noted in this section. Details of measurements at isolated temperatures are not given in the table, but are discussed in the text.

Methanamine. The values of Felsing and Thomas (1929-227) and of Isakova et al. (1966-198) were used to fit Eq. (6). The values of the latter were about 0.25% lower than the former in the region of overlap, 281 to 293 K. The values of Le Fevre and Russell (1947-335) were about 0.35% lower than the selected values while that of Hofmann (1889-19) was in good agreement with the selections. The root-mean-square-weighted-deviation for the fit to Eq. (6) with four adjustable constants was four times higher than expected for an optimum fit and a proper choice of experimental imprecisions. The cyclic sign changes in the deviations, Fig. 9, indicated that Eq. (6) was not entirely adequate; however, additional terms in Eq. (6) were not warranted by the data.

Ethanamine. The values of Swift (1942-92), Barcelo et al. (1950-529), and Pohland and Mehl (1933-369) were selected in determining the three coefficients in Eq. 6; the temperature range of the values was too limited to justify inclusion of a fourth term. The selected values and the remaining values (1850-2, 1889-26, 1910-58, and 1912-127) were consistent with the experimental values as shown by the deviations from Eq. (6), see Fig. 10. Measurements reported at

single temperatures by (1850-7) and (1889-19) were not given any weight in the evaluation.

1-Propanamine. The values reported by Vogel (1948-262) and Costello and Bowden (1959-218) were selected, and were represented to within their experimental imprecisions by Eq. (6) with three adjustable parameters. The deviations are shown in Fig. 11. The remaining values at isolated temperatures (1952-385, 1968-195) and those prior to 1920 (1872-26, 1886-28, 1889-26, 1891-28, 1893-55, 1895-49, 1910-66, and 1919-64) were represented to within 0.3%. Larger deviations were found for the values from the remaining literature, (1869-15) 1.2%; (1970-165) 10%.

2-Propanamine. The values used in determining the three constants in the density equation were those of Vogel (1948-262) and of Costello and Bowden (1959-218). The values from the references, (1868-12, 1895-49, 1954-310, 1968-195, and 1969-165), that reported only one or two points were not included in the fit; however, they were within the expected accuracy of the data used in the fit. The excluded results of Shirai (1956-45) showed slightly more scatter, as much as 0.2%, than had been anticipated from the assigned imprecisions. The results of Hough *et al.* (1950-523) were as much as 1% higher than the accepted values.

Kobe and Mathews (1970-5) used isochoric measurements to determine liquid and vapor densities up to the critical temperature, but they only reported their value of the critical density and the constants for the rectilinear diameter $\frac{1}{2}(\rho_1 + \rho_g)/(\text{kg m}^{-3}) = 268.2 - 218.8(1 - T/T_c)$ (from 453 to 471.9 K). Their values of the critical temperature and density were used as constraints on the density equation.

Benzenamine. Over 200 separate values of the density at varied temperatures have been reported in the literature as

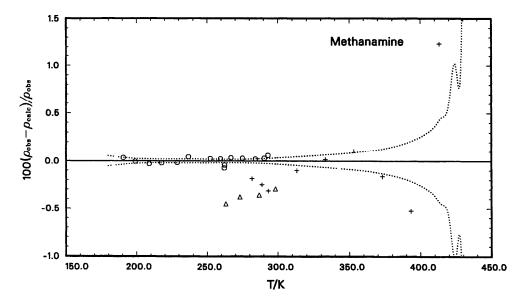


FIG. 9. Percent deviation of experimental saturated liquid densities for methanamine from Eq. (6). O Felsing and Thomas (1929-227)*; \triangle Le Fevre and Russell (1947-335); + Isakova et al. (1966-198)*; with * after reference number for data used in fitting.

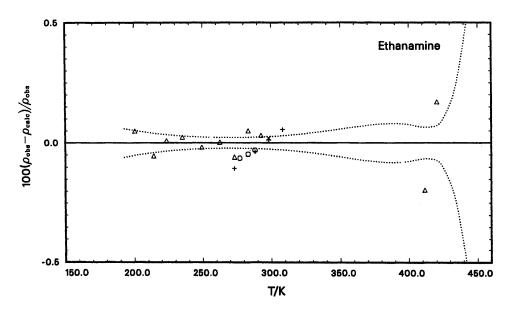


Fig. 10. Percent deviation of experimental saturated liquid densities for ethanamine from Eq. (6). O Perkin (1889-26); Δ Pohland and Mehl (1933-369)*; + Swift (1942-92)*; ×Barcelo et al. (1950-529); with * after reference number for data used in fitting.

summarized in Table 17. The four constants in the density equation were determined from the values for which a one is in the sl column of Table 17. Additional data not indicated in Table 17 are available at isolated points (1850-10, 1880-2,

1888-35, 1888-39, 1894-56, 1895-49, 1898-2, 1902-64, 1909-133, 1910-58, 1912-127, 1913-73, 1913-163, 1914-108, 1920-94, 1924-127, 1931-211, 1932-116, 1933-418, 1937-254, 1945-173, 1949-535, 1949-536, 1957-486, 1959-304, 1960-

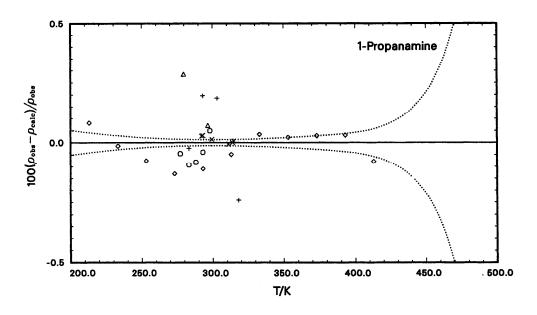


Fig. 11. Percent deviation of experimental saturated liquid densities for 1-propanamine from Eq. (6). ○ Perkin (1889-26); △ Gladstone (1891-28); + Turner and Merry (1910-66); × Vogel (1948-262)*; ♦ Costello and Bowden (1959-218)*; with * after reference number for data used in fitting.

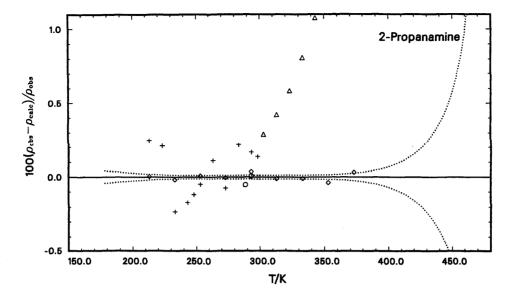


FIG. 12. Percent deviation of experimental saturated liquid densities for 2-propanamine from Eq. (6). ○ Bruhl (1895-49); △ Hough et al. (1950-523); + Shirai (1956-45); ◇ Costello and Bowden (1959-218)*; with * after reference number for data used in fitting.

289, 1962-363, 1963-325, 1965-333, 1967-225, 1975-33, 1985-372, 1987-70, and 1988-53). The selected values were within a few 0.01% of those from the fitting equation as shown in Fig. 13. The results from references (1953-611 and 1953-615) were much more inconsistent than were anticipated. Two extensive data sets published before 1900 (1887-59 and 1896-28) were persistently low by about 0.25%. The apparent precision of the results reported by Neubeck (1887-59) is enigmatic in light of the way his results have approximately constant deviations for each of the four benzenamines examined in this work. These deviations are not consistent with systematic errors in either temperature or density for the entire collection of data; they have been ascribed tentatively to impurities in his samples.

2-Methylbenzenamine. The temperature range of the available data was so limited that only two constants in the fitting equation could be obtained reliably. As indicated in Table 17, values from a number of sources were used for the fit; they were represented to within better than $\pm 0.1\%$. Data at isolated points (1894-56, 1895-49, 1896-50, 1898-2, 1902-73, 1913-73, 1914-154, 1915-104, 1924-127, 1936-383, and 1960-288) were not indicated in Table 17. The results of Neubeck (1887-59) were persistently high by about 0.25% in the region of overlap with the remaining data; this precluded their use of the values reported near 472 K. All of the remaining values were represented with the fitting equation to within the experimental imprecisions. Deviations from

the fitting equation for some of the experimental data are shown in Fig. 14.

3-Methylbenzenamine. Values were available over a limited range of temperatures, and only two constants could be determined for the fitting equation. The values included in the fit, indicated in Table 17, were represented with the fitting equation to better than \pm 0.1%. The values by Neubeck (1887-59), by Perkin (1896-28), and by Dessart (1926-22) were systematically higher than the accepted values by about 0.6%, 0.2%, and 0.4%, respectively. Those of Bingham and Spooner (1932-308) showed a statistically significant trend in their deviations, and those of Hatem (1949-488) were less precise than had been anticipated. Some isolated points considered (1895-49, 1898-2, 1924-127, 1913-163, and 1936-383) were not indicated in Table 17. Deviations from the fitting equation for some of the experimental data are shown in Fig. 15.

4-Methylbenzenamine. Two constants were determined for the fitting equation with the values available over the limited temperature range indicated in Table 17. The selected values were fit to better than $\pm 0.1\%$. The rejected values from sets over appreciable temperature ranges by Neubeck (1887-59) and Perkin (1896-28) showed significant trends in their deviations. Isolated points (1893-55, 1895-49, 1913-163, and 1913-178) were not indicated in Table 17. Deviations from the fitting equation for some of the experimental data are shown in Fig. 16.

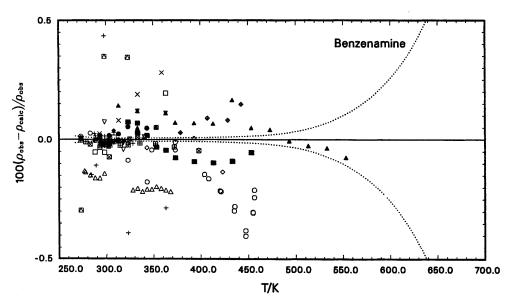


Fig. 13. Percent deviation of experimental saturated liquid densities for benzenamine from values calculated from Eq. (6). ○ Neubeck (1887-59); + Perkin (1892-22); + Jahn and Moeller (1894-43); △ Perkin (1896-28); △ Livingston et al. (1908-112); + Patterson and Findlay (1912-148)*; + Thole et al. (1913-178)*; + Herz (1914-137); □ Tyrer (1914-103)*; ⊗ Bramley (1916-233)*; ○ Bingham et al. (1920-95)*; ◇ Buehler et al. (1932-79); ● Azim et al. (1933-35)*; ⊕ Timmermans (1935-68)*; + Gibson and Loeffier (1939-114); ◇ Friend et al. (1937-125)*; × Vogel (1948-262); □ Hatem (1949-42)*; + Dreisbach and Martin (1949-120)*; Hough et al. (1950-523)*; ● Naumova (1953-615); + Tartakovskaya and Sukharev (1953-611); □ Naumova and Prokop'eva (1953-614); ▲ Kovalenko and Trifonov (1954-674)*; ▲ Costello and Bowden (1959-218)*; ∨ Lindberg and Stenholm (1966-203)*; ⊠ Sumer and Thompson (1967-58)*; × Deshpande and Bhatgadde (1968-223, 1971-17)*; ♦ Katz et al. (1971-157)*; ▼ Papepu et al. (1985-160)*; with * after reference number for data used in fitting.

TABLE 17. Available saturated liquid density data.

Range K			$rac{ ext{Range}}{ ext{kg}\cdot ext{m}^{-3}} \qquad rac{10^2\sigma(ho_l)/ ho_l^a}{ ext{kg}\cdot ext{m}^{-3}} sl^b$		N°	Author(s)	Ref.
			Me	ethan	amin	e	
190-293	0.05	778-663	0.01	1	15	Felsing and Thomas	1929-227
263-298	0.1	695-654	0.02	0	4	Le Fevre and Russell	1947-335
282-413	0.2	675-466	0.02	1	9	Isakova et al.	1966-198
			\mathbf{E}	thana	mine		
277-288	0.3	701-689	0.01	0	3	Perkin	1889-26
201-420	0.01	785-684	0.01	1	11	Pohland and Mehl	1933-369
273-288	0.01	706-688	0.005	1	4	Swift	1942-92

^a See section 1.6.

^b 1 for data selected and 0 for data not selected for least square fit.

^c Number of experimental values.

TABLE 17. Continued.

Range K	$rac{\sigma(T)^a}{ ext{K}}$	$\frac{\text{Range}}{\text{kg} \cdot \text{m}^{-3}}$	$rac{10^2 \sigma(ho_l)/ ho_l^a}{ m kg\cdot m^{-3}}$	sl^b	N^c A	author(s)	Ref.
			1-P	ropana	mine		
277-298	0.3	733-712	0.01	0	5	Perkin	1889-2
283-318	0.1	727-689	0.01	0	4	Turner and Merry	1910-6
292-315	0.1	718-695	0.03	1	8		1948-2
213-413	0.2	797-577	0.04	1		S	1959-2
			2-P1	ropana	mine		
303-343	0.003	680-638	0.01	0	5	Hough et al.	1950-5
213-298	0.02	773-684	0.02	0	11	Shirai	1956-4
213-373	0.2	771-592	0.04	1	9	Costello and Bowden	1959-2
			Ber	nzenan	nine		
404-456	0.1	922-873	0.03	0	13	Neubeck	1887-5
284-363	0.1	1028-958	0.04	0	2	Perkin	1892-2
287-289	0.1	1027-1024	0.05	0	2	Jahn and Moeller	1894-4
277-368	0.2	1034-954	0.06	0	15	Perkin	1896-2
302-340	0.1	1013-981	0.03	0	3	Livingston et al.	1908-1
288-298	0.05	1026-1017	0.05	1	3	Patterson and Findlay	1912-1
298-323	0.2	1022-992	0.1	1	2	Thole et al.	1913-1
298-363	0.05	1017-962	0.03	0	3	Herz	1914-1
273-372	0.02	1030-952	0.01	1	9	Tyrer	1914-1
293-298	0.02	1021-1017	0.01	1	3	Hartung	1916-2
283-398	0.02	1039-929	0.02	1	9	Bramley	1916-2
273-373	0.02	1039-951	0.04	1	12	Bingham et al.	1920-9
323-423	0.03	996-905	0.02	0	5	Buehler et al.	1932-7
293-343	0.02	1022-978	0.01	1	6	Azim et al.	1933-3
273-303	0.01	1039-1013	0.01	1	3	Timmermans et al.	1935-6
305-333	0.04	1011-987	0.05	1	2	Weller	1935-3
273-328	0.02	1039-991	0.03	0	3	Gibson and Loeffler	1939-1
379-442	0.01	947-890	0.01	1	4	Friend et al.	1944-1
293-359	0.02	1022-967	0.05	0	4	Vogel	1948-2
288-308	0.001	1026-1009	0.05	1	5	Hatem	1949-4
293-298	0.01	1021-1017	0.02	1	2	Dreisbach and Martin	1949-1
323-453	0.003	996-878	0.01	1	10	Hough et al.	1950-5
303-333	0.03	1021-1004	0.05	0	3	Naumova	1953-6
298-398	0.03	1028-924	0.05	0	3	Tartakovskaya and Sukhar	
273-323	0.03	1036-999	0.05	0	3	Naumova and Prokop´eva	1953-6
293-363	0.03	1021-962	0.05	1	3	Kovalenko and Trifonov	1954-6
273-553	0.2	1039-779	0.04	1	15	Costello and Bowden	1959-2
298-318	0.01	1018-1000	0.03	1	3	Lindberg and Stenholm	1966-2
293-313	0.02	1022-1004	0.02	1	3	Sumer and Thompson	1967-5
298-318	0.01	1017-1000	0.02	1	3	Deshpande and Bhatgadde	
298-318	0.01	1017-1000	0.02	1	3	Deshpande and Bhatgadde	
298-313	0.01	1017-1005	0.02	1	4	Katz et al.	1971-1
298- 3 18	0.01	1017-1005	0.01	1	5	Papepu et al.	1985-1

 $[^]a$ See section 1.6. b 1 for data selected and 0 for data not selected for least square fit. c Number of experimental values.

TABLE 17. Continued.

Range K	$\frac{\sigma(T)^a}{K}$	Range kg·m ⁻³	$rac{10^2\sigma(ho_l)/ ho_l^a}{ m kg\cdot m^{-3}}$	sl^b	Nc	Author(s)	Ref.				
			2-Methy	ylbenz	enam	ine					
415-472	0.2	894-843	0.05	0	11	Neubeck	1887-59				
277-328	0.5	1011-971	0.05	0	12		1896-28				
273-303	0.05	1015-990	0.06	1	3		1900-10				
293-343	0.1	999-957	0.3	0	3		1914-108				
273-373	0.02	1015-931	0.04	1	14		1920-95				
323-423	0.03	974-889	0.03	0	5	•	1932-79				
273-303	0.05	1015-990	0.01	1	3	Timmermans et al.	1935-68				
398-466	0.03	907-845	0.05	1	7		1944-125				
293-298	0.01	998-994	0.03	1	2		1949-120				
291-308	0.05	1000-986	0.02	0	5	Hatem	1949-488				
3-Methylbenzenamine											
422-476	0.2	885-833	0.05	0	12	2 Neubeck	1887-59				
277-298	0.1	1004-990	0.05	0	6	Perkin	1896-28				
273-305	0.1	1009-983	0.03	0	5	Dessart	1926-22				
273-373	0.05	1005-922	0.01	1	8	Bingham and Spooner	1932-308				
298-423	0.03	985-881	0.03	0	6	Buehler	1932-79				
273-303	0.05	1005-980	0.01	1	3	Timmermans et al.	1935-68				
374-466	0.03	923-837	0.05	1	8	Friend and Hargreaves	1944-125				
293-298	0.02	988-984	0.02	1	2	Dreisbach and Martin	1949-120				
291-308	0.05	993-971	0.02	0	5	Hatem	1949-488				
			4-Methy	lbenz	enami	ine					
416-474	0.2	883-829	0.04	0	11	Neubeck	1887-59				
323-343	0.1	952-946	0.01	0	4		1896-28				
323-333	0.05	961-953	0.06	1	2	2 Dutoit	1900-10				
319-413	0.05	971-873	0.1	0	11	Beck	1907-112				
313-448	0.01	970-850	0.03	1	7	' Bramley	1916-233				
350-383	0.05	940-904	0.05	0	3	•	1932-307				
323-393	0.05	962-902	0.01	1	4	Buehler	1932-79				
318-333	0.01	966-954	0.01	1	4	Timmermans et al.	1937-146				
409-463	0.03	889-835	0.05	1	5	Friend and Hargreaves	1944-125				

^a See section 1.6.

b 1 for data selected and 0 for data not selected for least square fit.
 c Number of experimental values.

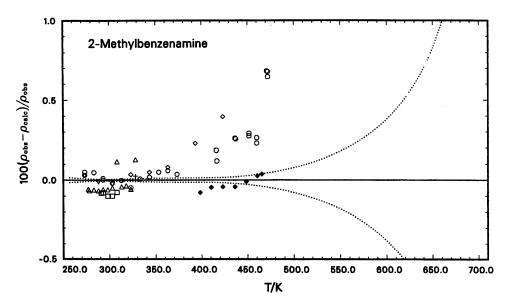


FIG. 14. Percent deviation of experimental saturated liquid densities for 2-methylbenzenamine from values calculated from Eq. 6. ○ Neuback (1887-59); △ Perkin (1896-28); ▽ Dutoit (1900-10)*; + Thole (1913-163); o Bingham et al. (1920-95)*; ◇ Buehler (1932-79); ◇ Friend and Hargreaves (1944-125)*; □ Hatem (1949-488); with * after reference number for data used in fitting.

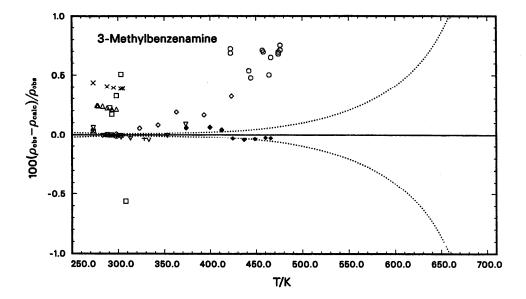


Fig. 15. Percent deviation of experimental saturated liquid densities for 3-methylbenzenamine from values calculated from Eq. (6). ○ Neuback (1887-59); △ Perkin (1896-28); + Thole (1913-163); × Dessart (1926-22); ▽ Bingham and Spooner (1932-308)*; ◇Buehler (1932-79); □ Timmermans et al. (1935-67)*; ◇ Friend and Hargreaves (1944-125)*; ⊕ Dreisbach and Martin (1949-120)*; □ Hatem (1949-488); with * after reference number for data used in fitting.

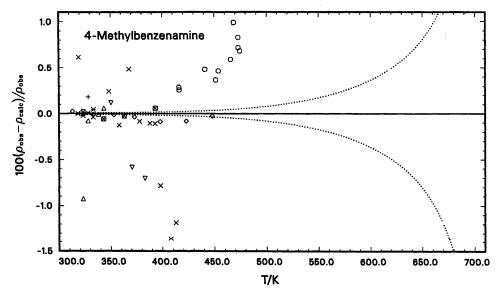


Fig. 16. Percent deviation of experimental saturated liquid densities for 4-methylbenzenamine from values calculated from Eq. (6). ○ Neuback (1887-59); △ Perkin (1896-28); ×Beck (1907-112); + Thole (1913-163); ◇ Bramley (1916-233)*; ▽ Bernoulli and Veillon (1932-307); □ Buehler (1932-79)*; ×Timmermans et al. (1937-146)*; with * after reference number for data used in fitting.

3.4. Second Virial Coefficients

The temperature ranges over which measurements of second virial coefficients have been made, along with the estimated uncertainties, are listed in Table 18.

Methanamine. The second virial coefficient data of Lambert and Strong (1950-430) were not used because of their high uncertainty. Only the values of Adam et al. (1976-113) were used to derive the recommended values from Eq. (9). Deviations of the experimental values from those calculated from the smoothing equation are shown in Fig. 17. The estimated uncertainties in the smoothed virial coefficients are ± 20 cm³ mol⁻¹ at 180 K, decreasing to ± 10 cm³ mol⁻¹ at 610 K.

Ethanamine. The values of Lambert and Strong (1950-430) were the only data available. The estimated uncertainty in the virial coefficients is \pm 50 cm³ mol⁻¹. The parameter A_b in Eq. (9) was constrained to conform with Eq. (10) for methanamine. If this parameter was allowed to be freely adjustable, the remaining parameters were not consistent with those for methanamine. The deviations of the values from those calculated from the smoothing equation are shown in Fig. 18.

1-Propanamine. Second virial coefficients were derived from the Claperyon equation with the enthalpy of vaporization data of Majer *et al.* (1979-78) and the Cox equation constants from Table 2. The derived values at 298.15,

313.15, and 328.15 K were (-1053 ± 20), (-822 ± 10), and (-769 ± 10) cm³ mol⁻¹, respectively. The value at 313.15 K seemed inconsistent with the other two points and was given zero weight. The values of both A_b and D_b in Eq. (9) were determined from the constants for methanamine in Eq. (10), and the value of C_b was determined by a least-squares fit.

2-Propanamine. Values of the second virial coefficient derived from enthalpies of vaporization determined by Majer *et al.* (1979-78) were (-806 ± 10) and (-721 ± 10) cm³ mol⁻¹ at 298.15 and 313.15 K, respectively. These were used to determine the constant C_b in Eq. (9) in a manner similar to that described above for 1-propanamine.

Benzenamine. The only data available were reported by Lagutkin et al. (1973-167) who used a virial equation with the first four virial coefficients and the data derived by Seshadri et al. (1969-168) from an empirical equation of state. The latter work used the Martin-Hou (1955-712) equation of state without volumetric data essential as input to reliably specify second virial coefficients. For these reasons we did not consider these results; however, they are listed in a recent compilation (1986-782) of virial coefficients.

No second virial coefficients or direct enthalpy of vaporization measurements were available for the remaining compounds.

TABLE 18. Available second virial coefficient data.

Range K	$rac{ ext{Range}}{ ext{cm}^3 \cdot ext{mol}^{-1}}$	$rac{\sigma(B)}{\mathrm{cm}^3 \cdot \mathrm{mol}^{-1}}$	sla	Author(s)	Ref.
		Methan	namine		
293 to 405	-535 to -220	50	0	Lambert and Strong	1950-430
296 to 550	-471 to -118	10	1	Adam et al.	1976-113
293 to 405	-821 to -345	Ethana	amine 1	Lambert and Strong	1950-430
		1-Propa	namine		
298 to 328	-1053 to -769	20	1	This work (derived)	
		2-Propa	namine	•	
298 to 313	-806 to -721	20	1	This work (derived)	

^a Selected if 1 and rejected if 0.

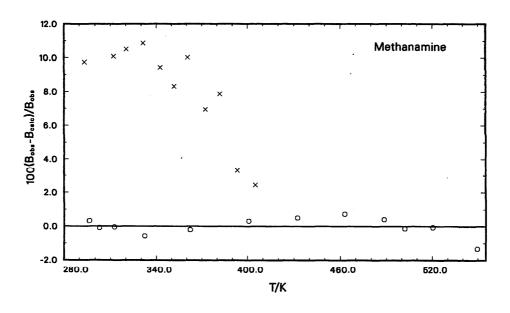


FIG. 17. Percent deviation of experimental second virial coefficients for methanamine from the smoothing equation. × Lambert and Strong (1950-430); O Adam et al. (1976-113)*; with * after reference number for data used in fitting.

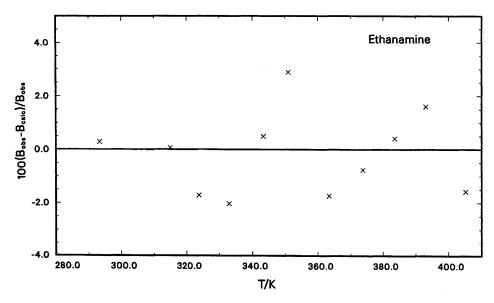


Fig. 18. Percent deviation of experimental second virial coefficients for ethanamine from the smoothing equation. ×Lambert and Strong (1950-430).

3.5. Enthalpies of Vaporization or Sublimation

Calorimetrically determined enthalpies of vaporization together with values calculated from vapor pressure data, along with estimated uncertainties are listed in Table 19.

Methanamine. Aston et al. (1937-248) determined calorimetrically the enthalpy of vaporization at 266.84 K. Using the enthalpies for the liquid and ideal gas and the second virial coefficients of this report, we corrected the value determined by Aston et al. (1937-248) to give the enthalpy of vaporization to the ideal gas state at 298.15 K reported in Table 10.

Ethanamine. No calorimetric value was available. The enthalpy of vaporization at 298.15 K was determined from vapor pressure data and corrected to the ideal gas state using the second virial coefficients of this report.

1-Propanamine. The enthalpy of vaporization was determined calorimetrically by Majer et al. (1979-78) at 298.15, 313.15, and 328.15 K and by Kusano and Saito (1976-127) at 298.15 K. We calculated the enthalpy of vaporization, corrected to the ideal gas state at 298.15 K, using the enthalpy of vaporization determined by Majer et al. (1979-78) at 298.15 K and the second virial coefficients of this report.

2-Propanamine. The enthalpy of vaporization was determined calorimetrically by Majer *et al.* (1979-78) at 298.15 and 313.15 K. Using the value at 298.15 K and the second virial coefficients of this report, we calculated the enthalpy of vaporization to the ideal gas state at 298.15 K.

Benzenamine. The enthalpy of vaporization of benzenamine was determined calorimetrically by Hatton et al. (1962-3) at 332.2 K and by Kusano and Wadsö (1971-2) at 298.15 K. These two determinations were consistent with those derived from the Claperyon equation. The value determined by Kusano and Wadsö was selected; corrections for gas imperfection were insignificant.

2-Methylbenzenamine. The enthalpy of vaporization to the ideal gas was calculated for 353.15 K from the Claperyon equation with the vapor pressure equation, and the value was corrected to 298.15 K using the enthalpies of the liquid and ideal gas. Corrections for gas imperfections were assumed to be insignificant.

3-Methylbenzenamine. The enthalpy of vaporization at 298.15 K was determined in a manner similar to that for 2-methylbenzenamine.

4-Methylbenzenamine. The enthalpy of vaporization at 353.15 K was calculated from the Claperyon equation with the vapor pressure equation of this report. This result was used to derive an enthalpy of sublimation to the ideal gas at 298.15 K. The value of the heat capacity of the liquid at 316.89 K compiled by Kudchadker and Wilhoit (1983-108) was used to calculate the enthalpy difference of the liquid to the triple-point temperature at 316.89 K. The enthalpy of fusion determined by Rastogi *et al.* (1963-367) and an estimated value of the heat capacity of the crystals $\left[C_{\text{sat}}(c)/R\right] \simeq C_{\text{sat}}(l)/R - 7$ was used to determine the enthalpy difference of the condensed phases from 316.89 to 298.15 K.

TABLE 19. Available enthalpy of vaporization and sublimation data at 298.15 K.

x^a	$\frac{T}{K}$	$\frac{\Delta_{\mathbf{x}}^{\mathbf{g}}H}{\mathbf{k}\mathbf{J}\cdot\mathbf{mol}^{-1}}$	$\frac{\sigma(\Delta_{\mathbf{x}}^{\mathbf{g}}H)^{b}}{\mathrm{k}\mathbf{J}\cdot\mathrm{mol}^{-1}}$	Method	sl	Author(s)	Ref.
				Methanamine			
•							
l	263.84	25.81	0.10	Calorimetry	1	Aston et al.	1937–218
l	298.15	24.17	0.20	Vapor press.	0	TRC - this work	
				Ethanamine			
l	298.15	26.27	0.20	Vapor press.	1	TRC - this work	
				1-Propanamine	:		
l	298.15	30.34	0.10	Calorimetry	0	Kusano and Saito	1976-127
ì	298.15	31.26	0.10	Calorimetry	1	Majer et al.	1979-78
ı	313.15	30.14	0.10	Calorimetry	0	Majer et al.	1979-78
1	328.15	28.92	0.10	Calorimetry	0	Majer et al.	1979-78
l	298.15	31.28	0.10	Vapor press.	0	TRC - this work	
				2-Propanamine	:		
ı	298.15	28.36	0.10	Calorimetry	1	Majer et al.	1979-78
l	313.15	27.19	0.10	Calorimetry	0	Majer et al.	1979-78
l	298.15	28.36	0.10	Vapor press.	0	TRC - this work	
				Benzenamine			
ı	333.15	52.95	0.10	Calorimetry	0	Hatton et al.	1962-3
1	298.15	55.83	0.10	Calorimetry	1	Kusano and Wadsö	1971-2
l	298. 15	56.13	0.20	Vapor press.	0	TRC - this work	
			2-]	Methylbenzenan	ine		
1	298.15	62.7	0.50	Vapor press.	1	TRC - this work	
			3-1	Methylbenzenan	ine		
l	298.15	62.7	0.50	Vapor press.	1	TRC – this work	
			4-1	Methylbenzenam	ine		
s	298.15	78.8	0.50	Vapor press.	1	TRC - this work	

^a Designation for condensed phase (x). ^b See section 1.6.

3.6. Enthalpies of Combustion and Formation

Several determinations for the enthalpies of combustion of these amino compounds were made near the turn of the century. Most of these measurements were made at room temperature which ranged from 15 °C to 20 °C. Thomsen (1905-2) made his measurements in the gas phase but for comparison we converted his values to the liquid state using

the selected enthalpies of vaporization. All values were corrected to 25 °C with appropriate heat capacity data. In general, these old values were found to deviate appreciably from recent determinations. The older data are included primarily for completeness, and we do not give them significant weight in our evaluation. The available enthalpy of combustion data along with estimated uncertainties are listed in Table 20. Enthalpies of formation were calculated using the enthalpies

TABLE 20. Available enthalpy of combustion data referred to 298.15 K.

ph ^a	$\frac{\Delta_{\mathrm{c}}U^{\mathrm{o}}/M}{\mathrm{k}\mathrm{J}\cdot\mathrm{g}^{-1}}$	$rac{2\sigma(\Delta_{ m c}U^{ m o}/M)^b}{{ m kJ\cdot g}^{-1}}$	$\frac{\Delta_{\mathrm{c}} H^{\mathrm{o}}}{\mathrm{kJ \cdot mol}^{-1}}$	$\frac{2\sigma(\Delta_{c}H^{\circ})^{b}}{\mathrm{kJ\cdot mol}^{-1}}$	Author(s)	Ref.
			Meth	anamine		
l	-33.94^{c}	0.10	-1056^{c}	5	Thomsen	1905-223
l	-34.44	0.45	-1071	15	Lemoult	1907-116
1	-33.78	0.30	-1051	10	Muller	1910-127
1	-34.095	0.013	-1060.8	0.4	Jaffe	1958-350
			Etha	anamine		
1	-37.99	0.10	-1716	5	Berthelot	1881-41
1	-37.93^{c}	0.10	-1710^{c}	5	Thomsen	1905-223
i	-37.85	0.30	-1710	15	Lemoult	1907-116
ì	-37.933	0.011	-1713.3	0.3	Jaffe	1958-350
•	~01.500	0.011	-1110.0	0.0	Jane	1300-000
			1-Pro	panamine		
l	-40.14^{c}	0.15	-2377^{c}	10	Thomsen	1905-223
l	-39.45	0.25	-2336	15	Lemoult	1907-116
l	-39.940	0.005	-2365.3	0.3	Smith and Good	1967-60
			2-Pro	panamine		
l	-39.758	0.008	-2354.5	0.5	Smith and Good	1967-60
			Benz	enamine		
1	-36.74	0.30	-3425	30	Petit	1889-4
1	-36.48	0.10	-3400	10	Stohman et al.	1890-2
i	-37.03^{c}	0.60	-3452^{c}	60	Thomsen	1905-223
ì	-36.44	0.10	-3397	10	Lemoult	1907-116
l	-36.67	0.20	-3418	20	Swarts	1919-41
l	-36.398	0.010	-3392.8	1.0	Huffman ^d	1942-*
l	-36.401	0.010	-3393.1	1.0	Anderson and Gilbert	1942-5
l	-36.415	0.010	-3394.4	1.0	Cole and Gilbert	1951-259
l	-36.400	0.009	-3393.0	0.8	Hatton et al.	1962-3
	_		_			

TABLE 20. Continued.

ph^{a}	$\frac{\Delta_{\rm c} U^{\circ}/M}{{ m kJ}\cdot{ m g}^{-1}}$	$rac{2\sigma(\Delta_{ m c}U^{\circ}/M)^b}{{ m k}{ m J}\cdot{ m g}^{-1}}$	$\frac{\Delta_{\mathrm{c}}H^{\mathrm{o}}}{\mathrm{k}\mathbf{J}\cdot\mathrm{mol}^{-1}}$	$\frac{2\sigma(\Delta_c H^\circ)^b}{\mathrm{kJ} \cdot \mathrm{mol}^{-1}}$	Author(s)	Ref.
			2-Methylben	zenamine		
1	-37.62	0.10	-4035	10	Petit	1889-4
1	-37.61	0.02	-4034.5	2	TRC – this worke	
			3-Methylben	zenamine		
1	-37.68	0.10	-4040	10	Petit	1889-4
1	-37.59	0.02	-4032.7	2	TRC - this worke	
			4-Methylben	zenamine		
s	-37.39	0.10	-4011	10	Petit	1889-4
s	-37.45	0.02	-4017.3	2	$\mathbf{TRC}-\mathbf{this}\mathbf{work^e}$	

a phase of substances for which measurements were made. b See section 1.6.

ormation of auxiliary substances listed in Table 21.

Methanamine. The value of Jaffe (1958-350) was pted. The early values reported by Thomsen (1905-2), Lemoult (1907-116), and by Muller (1910-127) agree a the selected value within their estimated uncertainties.

Ethanamine. The value of Jaffe (1958-350) was adopt-For historical background we list those by Thomsen 05-2), Berthelot (1881-41) and Lemoult (1907-116) ch agree with the selected value within the estimated unainties.

1-Propanamine. The value by Smith and Good (1967-, determined with a high-purity sample was adopted. We determined by Thomsen (1905-2) and Lemoult (1907-116). The value of the latter is particular-oor.

2-Propanamine. The selected value was determined by th and Good (1967-60) on a high-purity sample.

Benzenamine. There are several older determinations he enthalpy of combustion of benzenamine. They are se by Petit (1889-4), by Stohmann, (1890-2), by Thom-(1905-2), by Lemoult (1907-116), and by Swarts (1919-. An unpublished value determined by Huffman was list-

ed by Anderson and Gilbert (1942-5).

The measurements of Anderson and Gilbert (1942-5), Cole and Gilbert (1951-259), and Hatton *et al.* (1962-3) on high-purity samples at 298.15 K agree. The value determined by Hatton *et al.* (1962-3) was selected.

2-Methylbenzenamine. Petit (1889-4) determined the enthalpy of combustion of 2-methylbenzenamine in the liquid state at 298.15 K. The purity of the sample was stated to be above 99%. Owing to questions concerning the accuracy of these measurements, we deemed that estimated values would be more reliable. The enthalpy of combustion was estimated in the ideal gas state at 298.15 K using the enthalpies of formation of benzenamine, methylbenzene, and 1,2-dimethylbenzene as shown below:

 $\Delta_f H^{\circ}(2\text{-methylbenzenamine})$

=
$$\Delta_f H^{\circ}$$
(benzenamine) + $\Delta_f H^{\circ}$ (1,2-dimethylbenzene)

 $-\Delta_f H^{\circ}$ (methylbenzene).

This enthalpy of combustion was converted to a value for a liquid. Petit's value was 0.5 kJ mol⁻¹ more negative than our selected value. This agreement is probably fortuitous in

^c from original values for combustion of vapor at the boiling point.

^d Anderson and Gilbert listed the unpublished value of the enthalpy of combustion of benzenamine determined by Huffman.

e estimated.

TABLE 21. Enthalpies of formation of auxiliary substances at 298.15 K.

Compound	phase	$\Delta_{\mathbf{f}} H^{\circ}/\mathrm{kJ}\cdot\mathrm{mol}^{-1^{a}}$	Ref.
Carbon dioxide	g	-393.51 ± 0.13	1978-115
Water	g	$\bf-241.814\pm0.042$	1978-115
Water	ī	$\mathbf{-285.830} \pm 0.042$	1978-115
Methylbenzene	g	$\textbf{50.17} \pm \textbf{0.42}$	TRC tables
1,2-Dimethylbenzene	g	$\textbf{19.08} \pm \textbf{1.08}$	TRC tables
1,3-Dimethylbenzene	É	$\boldsymbol{17.32 \pm 0.75}$	TRC tables
1,4-Dimethylbenzene	g	$\textbf{18.03} \pm \textbf{1.00}$	TRC tables

^a Uncertainties are two standard errors, see section 1.6.

view of his poor value for benzenamine.

3-Methylbenzenamine. Petit (1889-4) determined the enthalpy of combustion of 3-methylbenzenamine in the liquid state at 298.15 K. The purity of the sample was stated to be above 99%. We estimated its enthalpy of formation in the ideal gas state at 298.15 K using the enthalpies of formation of benzenamine, methylbenzene, and 1,2-dimethylbenzene in a manner similar to that used for 2-methylbenzene. Our estimated value is 7.3 kJ mol⁻¹ less negative than Petit's result.

4-Methylbenzenamine. Petit (1889-4) determined the enthalpy of combustion of 3-methylbenzenamine in the solid state at 298.15 K. The purity of the sample was stated to be above 99%. We estimated its enthalpy of formation in the ideal gas state at 298.15 K using the enthalpies of formation of benzenamine, methylbenzene, and 1,4-dimethylbenzene in a manner similar to that used for 2-methylbenzene. Our estimated value is 6.3 kJ mol⁻¹ more negative than Petit's result.

3.7. Condensed Phase Calorimetric Properties

The available heat capacity and phase transition data for the condensed phases, along with estimated uncertainties, are listed in Table 22. Evaluation of thermodynamic properties of the substances in the condensed phases, i.e., crystals and liquid, required low-temperature heat-capacity measurements ($C_{\rm sat}$) in each condensed phase and temperatures and enthalpies of phase transitions ($T_{\rm tr}$ and $\Delta_{\rm tr} H$). Because the results for the solid phase were dependent upon thermal histories, sets of data were chosen to best represent the measurements on the equilibrium forms of the crystals. Weighted combinations of the liquid phase data were used in smoothing and integrating the heat capacity data. The integrations were performed with a spline function method which used six points at a time in least-squares fits to cubic functions with the constraints that the contiguous cubic

functions have continuity in value, slope, and curvature at their point of junction. The results were extrapolated to 0 K with fits of the data between 10 and 25 K to the Debye heat capacity function (1912-160). Corrections for heterophase premelting were made to the data prior to making the integrations. Where heat capacity and related enthalpy of transition data in the condensed phase did not extend to temperatures low enough to apply the third law of thermodynamics, the limited data were evaluated without attempts to derive related thermodynamic properties by integration. The calculated results are presented as $C_{\rm sat}/R$, $\Delta_0^T S/R$, $-\Delta_0^T G/R$, and $\Delta_0^T H/RT$. The data selections are discussed below.

Methanamine. The low-temperature heat capacity C_{sat} for crystal (12.71 to 176.91 K) and liquid (186.61 to 259.28 K) methanamine were measured by Aston et al. (1937-248). Aston and Eidinoff (1939-396) used a newly constructed adiabatic calorimeter to redetermine the heat capacity of the liquid over the temperature range 185 to 260 K. Their values, reported graphically, are in good agreement with the previous ones. The $C_{\rm sat}$, T_m , and $\Delta_{\rm tr}H$ values reported by Aston et al. (1937-248) were adopted for evaluation of the thermodynamic properties in the condensed phases. The heat capacities were recomputed on IPTS-68 and integrated by procedures described in the first paragraph of this section (3.7). Their data from series III, series IV, series VI at 259.3 K, series VII, series XIII, series XIV up to 102.6 K, and series XVIII were used in determining smoothed heat capacities. They were extended to 298.15 K [above the highest measurement temperature of 260.5 K by Aston et al. (1939-396) with a graphical extrapolation. The data from series I at 101.2 K and series XIV at 102.6 and 106.7 K were used to determine the enthalpy and entropy of transition at 101.469 K. The entropy of transition, 0.160 R, is 0.045 R higher than the value reported by Aston et al. (1939-396) owing to slightly different methods of subtracting the background heat capacity. The enthalpy of fusion

TABLE 22. Available heat capacity and phase transition data for the condensed phases.

		Heat C	apacity				Phase 7	Transition		Author(s)	Ref.
ph.	Range K	$\frac{\sigma(T)^a}{\mathrm{K}}$	$rac{\sigma_c(C_{ m sat})^a}{R}$	$\sigma_f(C_{ m sat})^a$	Pts.	Trans.	$^{T}_{ m K}$	$\frac{\Delta_{\mathrm{tr}} H}{\mathbf{J} \cdot \mathrm{mol}^{-1}}$	$\frac{\sigma(\Delta_{\mathrm{tr}}H)^a}{\mathrm{J}{\cdot}\mathrm{mol}^{-1}}$	Travitor (v)	
				-		Methanan	nine				
cII	12.71-101.20	0.05	0.025	0.005^c	59	cII⇌ cI	101.469	134.14	10	Aston et al.	1937-248
cI	101.83-176.91	0.01	0	0.01^{c}	44	$cI \rightleftharpoons l$	179.708	6133.6	42		
l	186.61-259.28	0.01	0	0.01	25		_	_	_		
l	185.0-260.0	0.01	0	0.01	_ b		_	-	-	Aston and Eidinoff	1939-396
						Ethanam	ine				
	-	_	_			$c \rightleftharpoons l$	192.65	-	_	Timmermans	1913-137
		_	-	_	_	$c \rightleftharpoons l$	192.15	_	-	Pohland and Mehl	1933-369
						1-Propana	mine				
l	298.15	-	-	0.001	1		-	_	-	Smith and Good	1967-60
l	298.15	_	_	0.005	1		-	-	_	Konicek and Wadsö	1971-11
\boldsymbol{c}	10-188.36	0.01	0.01	0.01^c	19	c ightleftharpoons l	188.36	10625	50	Vasil'ev et al.	1971-154
l	188.36-300	0.01	0	0.01	15		_	-	-		
\boldsymbol{c}	11.65-181.81	0.002	0.014	0.005^c	44	$c \rightleftharpoons l$	188.389	10975	4	Finke et al.	1972-140
l	189.96-334.56	0.002	0	0.00 1	19			_	-		
						2-Propana	mine				
l	313.15-343.15	0.003	0	0.004	4	_	_	_	_	Hough et al.	1950-523
l	298.15	_	_	0.00 1	1		-	-	-	Smith and Good	1967-60
l	298.15		_	0.005	1			-	_	Konick and Wadsö	1971-11
\boldsymbol{c}	11.56-172.50	0.002	0.023	0.005^c	45	$c \rightleftharpoons l$	178.011	7326.3	1	Finke et al.	1972-140
l	181.48-318.16	0.002	0	0.001	18			-			

<sup>a See section 1.6.
b Data reported graphically.</sup>

^c Values for solid within 20 K of phase transition temperature is three times as large.

TABLE 22. Continued.

		Heat C	apacity				Phase	Transitio	n	Author(s)	Ref.	
ph.	Range K	$\frac{\sigma(T)^a}{K}$	$rac{\sigma_e(C_{ m sat})^a}{R}$	$\sigma_f(C_{\mathrm{sat}})^a$	Pts.	Trans.	T K	$\frac{\Delta_{\mathrm{tr}}H}{\mathrm{J}\cdot\mathrm{mol}^{-1}}$	$\frac{\sigma(\Delta_{\mathrm{tr}}H)^a}{\mathrm{J}\cdot\mathrm{mol}^{-1}}$	Tunor(o)		
						Ronze	enamine					
1	290-465	0.01	0	0.05	4	Denze			_	von Reis	1881-5	
1	293.15-449.15	-	0	0.05	1				_	Louguinine	1902-9	
ì	293.15		0	0.03	1		***	_	-	Timofeev	1905-94	
i	291.15	_	0	0.02	1		_	_	_	Hartung	1915-94	
1	291.15-298.15	0.02	0	0.01	3		***		_	Hartung	1916-232	
1	274.23-332.02	0.01	0	0.01	12					Lang	1928-196	
l	303.15-412.75	0.01	0	0.04	22					Blacet et al.	1931-211	
ì	293.23-319.97	0.03	0	0.01	6		_	_	_	Ferguson and Miller	1933-387	
Ċ	93.50-236.30	0.15	0.06	0.01	12	$c \rightleftharpoons l$	266.8	10556	84	Parks et al.	1933-94	
l	275.70-298.20	0.15	0	0.01	3				-			
l	288	_	0	0.01	1		_	_		Radulescu and Jula	1934-351	
l	298.15-351.15	0.01	0	0.005	3		_	_	_	Ellyett	1937-435	
	_	_	_	_	_	$c \rightleftharpoons l$	267.3	10920	200	Ziegler and Andrews	1942-126	
l	323.15-453.15	0.003	0	0.006	10					Hough et al.	1950-523	
l	293	_		_	1		_	_	_	Crützen et al.	1957-486	
c	13.49-257.83	0.005	0.02	0.002^b	94	c ightleftharpoons l	267.13	10540	5	Hatton et al.	1962-3	
l	270.22-313.06	0.005	0	0.005	17			_	_			
l	298-318	_		_	_		-		_	Deshpande and Bhatagadde	1971-17	
l	298.15	_	0	0.005	1					Nichols and Wadsö	1975-49	
c	190-260			_	_ b	$c \rightleftharpoons l$	267	_		Lesbats and Lichanot	1987-147	
l	270-310	_	_	_	_ b			-	-			

 ^a See section 1.6.
 ^b Data reported graphically.
 ^c Values for solid within 20 K of phase transition temperature is three times as large.

TABLE 22. Continued.

		Heat (Capacity			Phase Transition			1	Author(s)	Ref.
ph.	Range K	$\frac{\sigma(T)^a}{K}$	$rac{\sigma_c(C_{ m sat})^a}{R}$	$\sigma_f(C_{\mathrm{sat}})^a$	Pts.	Trans.	T K	$\frac{\Delta_{\mathrm{tr}} H}{\mathrm{J \cdot mol^{-1}}}$	$\frac{\sigma(\Delta_{\mathrm{tr}}H)^a}{\mathrm{J}\cdot\mathrm{mol}^{-1}}$		
						2-Methylb	enzenam	ine			
l	294-485	0.1	0	0.1	4			_	_	von Reis	1881-5
l	293.15-469.15	_	0	0.05	1		_	_	_	Louguinine	1902-9
1	302.4-302.7	_	0	0.005	1		-	_	_	Kolossowsky and Udowenko	1934-365
l	288	_	0	0.02	1		-		-	Radulescu and Jula	1934-351
						3-Methylb	enzenam	ine			
l	302.4-302.9		0	0.005	1	-		-	-	Kolossowsky and Udowenko	1934-365
						4-Methylb	enzenam	ine			
l	293	_	-	0.02	1	·		_	_	Campbell and Campbell	1940-332
		_	_	_	_	$c \rightleftharpoons l$	316.85	18912	126	Rastogi et al.	1963-367

^a See section 1.6.

reported by Aston *et al.* (1939-396) was adopted in these calculations. The results are listed in Table 12.

The recalculated value of the entropy of the liquid at 298.15 K, $35.952 \text{ J K}^{-1} \text{ mol}^{-1}$, is slightly higher than the value reported by Aston *et al.* (1937-248), 35.90 J K⁻¹ mol⁻¹.

Ethanamine. No low-temperature thermal measurements have been reported. The only property data reported were $T_m = -80.5 \,^{\circ}\text{C}$ (1913-137) and $-81 \,^{\circ}\text{C}$ (1933-369); and $C_p(l, 298.15 \,\text{K}) = 130 \,^{\circ}\text{J} \,^{-1}$

1-Propanamine. The heat capacity of liquid 1-propanamine at 298.15 K was reported by Smith and Good (1967-60) [preliminary value from (1972-140)] and Konicek and Wadsö (1971-11). Using an adiabatic calorimeter, Vasil'ev et al. (1971-154) determined the heat capacity over the temperature range 60 to 300 K. They reported the enthalpy of fusion as 10625 J mol⁻¹ and the triple-point temperature as 188.36 K. The thermodynamic functions were calculated from 10 to 300 K.

Finke et al. (1972-140) determined the low-temperature calorimetric quantities for 1-propanamine from 12 K to near the normal boiling temperature. Values of $C_{\rm sat}$, T_m , and $\Delta_{\rm ti}$ H were measured by adiabatic calorimetry. Using integration procedures identical to those described in the preface to this section, they calculated the thermodynamic function for the crystal and liquid states. Their property values determined on IPTS-48 with the 1960 revision (1961-165) were corrected to those based on IPTS-68 and then were converted to dimensionless quantities for this work. They are presented in Table 12. The reported values of $C_{\rm sat}$ and S at 298.15 K (in J K⁻¹ mol⁻¹) are compared with those adopted in this work as follows: 162.51, 227.44 (1972-140); 166.4, 228.2 (1971-154); 160,—(1971-11); 162.3,—(1967-60); and 162.54, 227.43 (this work).

2-Propanamine. Hough et al. (1950-523) determined the isobaric heat capacities (C_p) of this compound in the temperatures range of 40 to 70 °C (313-343 K). The heat capacity at 298.15 K was reported by Smith and Good (1967-60) [preliminary value from (1972-140)] and by Konicek and Wadsö (1971-11), respectively. Finke et al. (1972-140) made low-temperature thermal measurements for 2-propanamine from 12 to 350 K, using adiabatic calorimetry. From these data they evaluated the thermodynamic quantities for this substance in the crystal and liquid states. Their values were adopted after making temperature scale corrections and converting to dimensionless units. Table 12 lists the results. A comparison of the values of heat capacity and entropy at 298.15 between the literature values and those adopted in this work is given below (in $J K^{-1} mol^{-1}$): 163.85, 218.32 (1972-140); 164, — (1971-11); 165.3, — (1967-60); 164.0, — (1950-523); and 163.88, 218.31 (this

Benzenamine. Heat capacities of benzenamine have been measured by many investigators: von Reis, 290 to 465 K (1881-5); Louguinine, 293.15 to 449.15 K (1902-9); Lang, 278.15 to 333.15 K (1928-196); Ferguson and Miller, 293 to 323 K (1933-387); Parks and Huffman, 94 to 298 K (1933-94); Radulescu and Jula, 288 K (1934-351); Hough et al., 323 to 453 K (1950-523); Crutzen et al., 293 K (1957-

486); Hatton et al., 13.49 to 313.06 K (1962-3); Deshpande and Bhatgadde, 298 to 318 K (1971-17); Nichols and Wadsö, 298.15 K (1975-49); and Lesbats and Lichanot, 200 to 310 K (1987-147). Lesbats and Lichanot reported their results at temperatures other than 298.15 K in graphical form only. Lesbats and Lichanot (1987-38) calculated the constant volume heat capacity of solid benzenamine from 203 to 263 K by adding Einstein functions associated with the internal modes of vibration to the Debye contributions for the crystal vibrations. We selected the data reported by Hatton et al. (1962-3) and Hough et al. (1950-523) for evaluation of the thermodynamic properties of benzenamine in the condensed phases.

The C_p data of Hough $et\,al$. (1950-523) were reconverted to $C_{\rm sat}$ with the vapor pressure equation and density equation of this report with the assumption that the coefficient of thermal expansion along the liquid saturation line was not significantly different than the coefficient of thermal expansion at constant pressure. The enthalpy of fusion of Hatton $et\,al$. (1962-3) was adopted.

The measurements were corrected to those based on the IPTS-68 in the evaluation procedures described above. The value of $C_{\rm sat}$ (l, 298.15 K) obtained was 191.91 J K⁻¹ mol⁻¹. The values reported in the literature for the same conditions were (in J K⁻¹ mol⁻¹): 192.5 (1881-5); 193.38 (1928-196); 190.92 (1933-94); 178.8 (1933-387); 191.05 (1962-3); 193.7 (1971-17); and 194.1 (1987-147). Our entropy at 298.15 K for benzenamine(l) is compared with the reported values as follows (in J K⁻¹ mol⁻¹): 191.6 (1933-94), 191.30 (1962-3), and 191.06 (this work). The calculated results are listed in Table 12.

2-Methylbenzenamine. No low-temperature thermal measurements have been reported in the literature. The heat capacity of 2-methylbenzenamine(l) at 288 K (1934-351) and 302.5 K (1934-150, 1934-365) was determined to be 201.7 and 209.6 J K⁻¹ mol⁻¹, respectively.

3-Methylbenzenamine. Low-temperature data were not available for evaluation of the thermodynamic properties of 3-methylbenzenamine in the condensed phases. The heat capacity of this compound at 302.7 K was reported as 216.9 J K⁻¹ mol⁻¹ by Kolosovskii and Udovenko (1934-150, 1934-365).

4-Mcthylbcnzenamine. No low-temperature thermal measurements for this compound were reported in the literature. The heat capacity at 293 K was determined as 124.3 J K $^{-1}$ mol $^{-1}$ (1940-332) and tabulated as 178.9 J K $^{-1}$ mol $^{-1}$ (1965-314). Both of these values seem low when compared with the values for the other two isomers. Temperature extrapolation of other data (1884-48, 1895-59) also give discordant values.

3.8. Ideal Gas Thermodynamic Properties

The statistical mechanical methods used for calculating of the ideal gas thermodynamic properties in the temperature range 0 to 1500 K at 1 bar are similar to those discussed in a previous article (1986-87), where several textbooks and pertinent review articles on statistical mechanics are cited. The molecular symmetry classifications used here follow

those of Wilson, Decius, and Cross (1955-691) and are cogently discussed by Cotton (1963-378).

Evaluations of translational, molecular rotational, and vibrational contributions to the thermodynamic properties of each compound were based on a rigid-rotor and harmonic-oscillator molecular model. The calculations required the molar mass (M), the three principal moments of inertia $(I_a, I_b,$ and $I_c)$ and a complete set of fundamental vibrational frequency assignments. The total number of frequencies required was 3N-3-L where N is the number of atoms in each molecule and L is the number of degrees of freedom treated as special inversion or rotational contributions. Contributions from internal rotations of $-NH_2$ and $-CH_3$ groups, and in some cases, those from inversion about the nitrogen atom were evaluated separately. Good general discussions concerning inversion have been given by Lister et al. (1978-125) and by Wollrab (1967-314).

The contributions of internal rotation and inversion were obtained from direct sums of the partition function with energy levels generated from solutions to the Schrödinger wave equation. The internal rotational potential function used in the Hamiltonian for these calculations was

$$V_r(\theta) = \frac{1}{2} V_n (1 - \cos n\theta), \tag{11}$$

where n = 2 for the -NH₂ rotation and n = 3 for the -CH₃ rotation, and θ is the angle of internal rotation. For the -CH₃ rotation in CH₃NH₂ the potential function

$$V_r(\theta) = \frac{1}{2} V_3 (1 - \cos 3\theta) + \frac{1}{2} V_6 (1 - \cos 6\theta)$$

was employed.

The procedures used for generating the internal rotation energy levels were the same as those employed by Lewis et al. (1972-222). Where available, the value of each internal rotational constant (F) was obtained from microwave spectroscopy. If one was unavailable, it was calculated from the reduced moment of inertia (I_r) of the rotating group, from

$$F = h / 8\pi^2 c I_r, \tag{12}$$

where the value of I, was calculated from molecular structural parameters. These parameters were either taken from experimental values obtained from other spectroscopic data or estimated by comparison with those for the other structurally related molecules. The internal rotation barrier height was usually determined from microwave spectra. Otherwise, it was derived from the observed torsional frequency, $\nu_{\rm tor}(0 \rightarrow 1)$ (1961-200).

The energy levels for inversion about the nitrogen atom were determined with procedures developed by Lanne (1970-13) for the following double-minimum-potential function

$$V_{w} = A_{d}(z^{4} + B_{d}z^{2}), (13)$$

where z is the relative motion displacement coordinate. Some of the constants for the potential function were available in the literature. For methanamine they were redetermined by a least-squares adjustment to reproduce the spectroscopically determined lowest transition frequencies. For ethanamine, 1-propanamine, and 2-propanamine, available

information was not adequate for determining the constants of Eq. (13); therefore, only a simple-harmonic-wagging (vibrational) motion was considered.

When vibrational frequency assignments and structural data were available for each rotational conformer arising from rotation about bonds between secondary or tertiary carbon atoms, the conformers were treated as different species with differing reduced moments of inertia and with contributions from the amine and methyl rotations. The total contributions were taken to be those for the equilibrium mixture. The differences in energy between the conformers and the degeneracy of the configurations were used in determining the composition of the mixture. The thermodynamic properties for the equilibrium mixtures of the conformers were calculated by conventional thermodynamic equilibrium calculations.

For evaluation of $\Delta_f H^\circ(T)$ and $\Delta_f G^\circ(T)$, the values of $\Delta_f H^\circ$ (298.15 K) were those of Table 11. The thermal functions for the elements C(graphite), $H_2(g)$, and $N_2(g)$ were values listed in the TRC Thermodynamic Tables-Non-Hydrocarbons (1988-192) adopted from the JANAF Thermochemical Tables (1985-249). The calculated heat capacity and entropy values are compared with available experimental results for each substance. They are also compared with other literature values obtained from computational methods. For the comparisons with entropy values obtained from condensed phase heat capacities, values of entropies of vaporization, expansion, and recompression were determined with the selected data in this report.

The details of the selection of data required for the calculations for each compound are discussed below.

Methanamine. The molecular structure of methanamine has been studied extensively by electron diffraction (1938-385, 1950-13), microwave (1947-355, 1952-615, 1953-626, 1954-678, 1954-681, 1955-612, 1956-575, 1957-497, 1957-498, 1971-167) and infrared (1964-409, 1967-261, 1968-228, 1982-85, 1987-94) spectroscopy. Takagi and Kojima (1971-167) determined the rotational, torsional, and inertial constants from microwave spectroscopy. Based upon the data of Lide (1957-497) and of Takagi and Kojima (1971-167), Harmony *et al.* (1979-155) evaluated the bond distances and angles. The ground state rotational constants from far-infrared spectroscopy by Ohashi *et al.* (1987-94) were used to calculate $I_a I_b I_c$, see Table 23. Based on the molecular structure reported by Itoh (1956-575), we calculated $I_c = 1.852 \times 10^{-40}$ g cm².

Methanamine has point symmetry C_v with a symmetry number (σ) of 1. All fifteen normal vibrations are both Raman and infrared active. There are nine A' species $(\nu_{10}-\nu_{9})$ and the remaining six are A" species $(\nu_{10}-\nu_{15})$. There are numerous reports of infrared (1938-378, 1939-392, 1939-393, 1939-395, 1940-330, 1940-335, 1955-88) and Raman (1939-394, 1955-626, 1964-373, 1968-239, 1970-180) spectra. Gray and Lord (1957-496) used their carefully measured infrared spectra of methanamine and its deuterated derivatives to assign the fundamental vibrational frequencies. Later, Shimanouchi (1972-110) critically reviewed the reported vibrational assignments for this molecule. For evaluation of the vibrational contributions (except those for in-

TABLE 23. Molar mass, product of moments of inertia, internal rotation, and inversion constants.

							Internal	rotat	ion ^e				NH ₂	inversion ^f	
Molecule	\mathbf{M}^{a}	$I_{\mathbf{a}}I_{\mathbf{b}}I_{\mathbf{c}}{}^{b}$	$\sigma_{ m total}{}^c$	$\mathbf{E_0}$	bond	$I_{\mathbf{r}}$	ν(0←1)	m	V_m	n	V_n	$\overline{A_{\mathbf{w}}}$	$B_{\mathbf{w}}$	ν(0←1)	$V_{ m inv}$
methanamine	31.05744	12.1387	6		C ₁ -N	1.852	262.8	3	8.203	6	-0.0293	46.19	12.09	780.1	20.19
ethanamine (trans)	45.08432	272.736	3	0.0	C ₁ -C ₂ C ₁ -N	4.368 2.706	264.5 236.7	3	16.238 8.909	-	ginganina			793 ^g	
ethanamine (gauche)	45.08432	260.489	3	1.196	_	4.327 2.709	258.8 218.0	3 3	15.456 7.737	-	_			773 ^g	
1-propanamine	59.11120	1788.2	3		C ₂ -C ₃ C ₁ -C ₂	4.698 17.353	252.0 104.0	3 1	15.807 3.670	- 3	— 8.590			775 ^g	
					C_1 -N	2.813	210.0	3	7.456						
2-propanamine (trans)	59.11120	1917.7	9	0.0	C_1-C_2 C_2-C_3 C_2-N	5.126 5.126 2.946	258.0 236.0 267.0	3 3 3	17.877 15.089 11.801	- -				785 ^g	
2-propanamine(gauche)	59.11120	1866.6	9	1.749	C_1-C_2 C_2-C_3 C_2-N	5.123 5.123 2.947	263.0 201.0 221.0	3 3 3	18.519 11.155 8.422	-				785 ^g	
benzenamine	93.12828	22846.3	4		C ₁ -N	2.663	277.3	2	23.64	-	-	45.00	6.80	40.08	6.22
2-methylbenzenamine	107.15516	62963.0	6		$egin{array}{c} C_2-C_6 \ C_1-N \end{array}$	5.259 2.316	99.70 29 6.5	3 2	6.230 23.64	-	_	45.85	6.83	40.05	6.40
3-methylbenzenamine	107.15516	74531.0	6		${f C_3-C_6} \ {f C_1-N}$	5.253 2.314	5.329 296.6	- 2	23.64	-	_	45.38	6.80	40.40	6.28
4-methylbenzenamine	107.15516	63970.0	12		${ m C_4\text{-}C_6} \ { m C_1\text{-}N}$	5.175 2.300	5.410 297.4	- 2	 23.64	-		45.13	7.20	30.93	7.00

 $^{{}^{}a}M = \text{molar mass, g} \cdot \text{mol}^{-1}$.

 $^{{}^}bI_aI_bI_c=$ product of the three principal moments of inertia, $10^{-117}{
m g}^3\cdot{
m cm}^6.$

 $^{^{}c}\sigma_{\text{total}}$ =total symmetry number.

 $^{{}^{}d}E_{0} = \text{energy of lowest state relative to ground state, kJ·mol}^{-1}$;

^eBond is the axis of relative rotation and the subscripts denote carbon numbers; $I_r = \text{reduced moment of inertia, } 10^{-40} \text{ g} \cdot \text{cm}^2$;

 $[\]nu$ (0 \leftarrow 1) = torsional wavenumber, cm⁻¹; V_m and V_n in kJ·mol⁻¹ for the internal rotation potential function: $V_r = \frac{1}{2}[V_m(1-\cos m\theta) + V_n(1-\cos n\theta)]$ with $\theta =$ angle of internal rotation.

 $^{{}^}fA_{\mathbf{w}}$ and $B_{\mathbf{w}} = \text{coefficients in -NH}_2$ inversion potential function, Eq. 13; $V_{\text{inv}} = \text{inversion potential barrier height, kJ·mol}^{-1}$.

gTreated as a wagging vibration, see Table 24.

TABLE 24. Fundamental vibrational wavenumbers.

Compound	Fundamental vibrational wavenumber (cm ⁻¹)
Methanamine	3427, 3361, 2985, 2961, 2820, 1623, 1476, 1473, 1430, 1335, 1130, 1044, 945
Ethanamine (trans)	3754, 3656, 3400, 3307, 3270, 3243, 3240, 1600, 1524, 1510, 1459.1, 1433, 1408, 1349.8, 1177, 1118.7, 1090, 1055, 881.9, 793, 789.1, 387
Ethanamine (gauche)	3741, 3641, 3341, 3302, 3241, 3176, 3075, 1621.7, 1487.3, 1464.8, 1455.3, 1397.2, 1377.9, 1292.8, 1238.2, 1116.8, 1085.5, 1015.6, 892.5, 816.2, 773.1, 403
1-Propanamine	3347, 3244, 2972, 2954, 2954, 2943, 2902, 2892, 2885, 1626, 1475, 1466, 1460, 1437, 1400, 1354, 1316, 1302, 1275, 1220, 1142, 1087, 1077, 1023, 887, 878, 775, 722, 454, 323
2-Propanamine (trans)	3411, 3342, 2968, 2965, 2950, 2945, 2932, 2878, 2860, 1618, 1460, 1469, 1469, 1449, 1375, 1360, 1343, 1245, 1240, 1170, 1130, 1029, 976, 942, 919, 819, 785, 472, 404, 369
2-Propanamine (gauche)	3393, 3328, 2968, 2965, 2950, 2945, 2918, 2878, 2860, 1618, 1460, 1469, 1469, 1449, 1375, 1360, 1343, 1245, 1240, 1170, 1130, 1029, 976, 942, 919, 826, 781, 459, 407, 369
Benzenamine	3500, 3418, 3088, 3072, 3053, 3037, 3025, 1618, 1603, 1590, 1503, 1468, 1324, 1276, 1190, 1173, 1152, 1090, 1050, 1028, 990, 968, 957, 874, 825, 812, 745, 690, 619, 526, 500, 415, 390, 233
2-Methylbenzenamine	3470, 3430, 3080, 3060, 3060, 3025, 2940, 2940, 2920, 1622, 1622, 1585, 1470, 1445, 1445, 1445, 1382, 1301, 1280, 1260, 1218, 1200, 1155, 1062, 1033, 1033, 985, 985, 927, 845, 845, 750, 750, 713, 651.3, 535, 515, 435.5, 435.4, 398.5, 263.2, 251.6
3-Methylbenzenamine	3480, 3430, 3065, 3055, 3055, 3040, 2940, 2940, 2920, 1625, 1610, 1585, 1498, 1470, 1470, 1470, 1375, 1312, 1295, 1295, 1171, 1160, 1143, 1075, 1030, 1030, 999, 960, 930, 930, 875, 780, 690, 664.7, 545, 520, 475, 431.3, 395.7, 282.2, 275.1
4-Methylbenzenamine	3480, 3440, 3060, 3060, 3045, 3045, 2940, 2940, 2920, 1645, 1627, 1585, 1515, 1445, 1445, 1445, 1380, 1325, 1270, 1270, 1177, 1177, 1120, 1085, 1045, 1045, 980, 950, 925, 845, 845, 815, 740, 651.3, 651.3, 651.3, 499.4, 434, 410, 382.6, 273, 273

nal rotation and inversion), the frequencies (ν_1 – ν_8 , ν_{10} , d ν_{11}) recommended by Shimanouchi (1972-110) and use determined by Woltt *et al.* (ν_{12}) (1964-496) and Hada *et al.* (ν_{13} and ν_{14}) (1982-82) were used, see Table 24.

The interactions among the vibration, inversion, internal rotation, and molecular rotation in methylamine has been the subject of spectral investigations which include microwave (1954-679, 1954-681, 1955-612, 1956-575, 1957-

TABLE 25. Potential barriers to internal rotation in methanamine.

V_3	V_6		
kJ⋅ mol ⁻¹		Author(s)	Ref.
11.96	-	Aston et al.	1937-248
6.36		Aston et al. Aston and Doty	1940-325
8.85		Lassettre and Dean	1949-506
7.56		Lide	1954-678
8.14		Shimoda et al.	1954-681
7.95		Aston and Gittler	1955-602
8.27		Itoh	1956-575
8.19		Lîde	1957-497
8.27		Nishikawa	1957-503
8.25		Gray and Lord	1957-496
8.190	-0.038	Tsubor et al.	1966-408
8.27		Tsubor et al.	1967-261
8.173	-0.024	Tamagake et al.	1968-228
8.173	-0.024	Tsubor et al.	1968-229
8.203^{a}	-0.130^{a}	Takagi and Kojima	1971-167
8.180	-0.002	Belorgeot et al.	1982-85

^aAdopted in this work.

497, 1957-498, 1957-503, 1971-167, 1974-202, 1974-203), infrared (1957-496, 1964-409, 1967-261, 1968-228, 1969-192, 1974-199, 1982-82, 1982-85, 1984-175) and ultraviolet (1969-193, 1982-134) studies.

Mathematical models for the internal rotation and inversion in methanamine, using microwave spectral data,

have been developed by Itoh (1956-575), Kivelson and Lide (1957-497), and Nishikawa (1957-503). Table 25 summarizes the potential barriers to internal rotation in CH_3NH_2 reported in the literature. The reported torsional wavenumbers of the - CH_3 top in CH_3NH_2 are summarized in Table 26.

TABLE 26. Torsional wavenumber in methanamine.

Torsional Wavenumber/cm ⁻¹	Method of Determination	Ref.	
270	Infrared spectroscopy	1940-325	
269.5	Far infrared spectroscopy	1954-693	
264	Theoretical calculation	1957-496	
263.9	Infrared spectroscopy	1968-228	
270, 271	Theoretical calculation	1968-235	
268	Selected value	1972-110	
269.8, 270.2	Theoretical calculation	1978-98	
262.8	Calculated value	this work	

Inversion Wavenumber cm ⁻¹	Inversion potential barrier kJ· mol ⁻¹	Method of Determination	Ref.
780		Infrared spectroscopy	1957-496
780.1		Infrared spectroscopy	1964-409
780		Raman spectroscopy	1964-496
	20.19 ± 0.12	Theoretical calculation	1967-261
776.16, 783.83	21.82	Theoretical calculation	1978-98
	19.09	Theoretical calculation	1978-100
	24.89^a	Theoretical calculation	1987-94
780.1	20.19	Selected and calculated	this work

TABLE 27. Inversion wavenumber and potential barrier in methanamine

Takagi and Kojima (1971-167) used their microwave spectra of methanamine and its deuterated species to determine the molecular constants including the V_3 and V_6 terms for the -CH₃ internal rotation and potential function $V_1(\theta) = \frac{1}{2}[V_3(1-\cos 3\theta) + V_6(1-\cos 6\theta)]$. This potential function was adopted together with the calculated reduced moment of inertia (I_r) listed in Table 23. Draeger *et al.* (1983-12) employed the potential function $V_1 = \frac{1}{2}V_3(1-\sin 3\theta)$, where $V_3 = 8267$ kJ mol⁻¹, for calculating the restricted rotor contributions.

Shimoda et al. (1954-681) calculated the version splittings for CH_3NH_2 . Tsuboi et al. (1964-409, 1967-261) used the fine structure of their 780.1 cm⁻¹ infrared band to calculate the potential barrier height for methanamine inversion as (1688 \pm 10) cm⁻¹ [(20.19 \pm 0.12) kJ mol⁻¹]. Kreglewski (1978-98) developed a Hamiltonian for vibration, inversion, internal rotation, and rotation of CH_3NH_2 and used the data of Tsuboi et al. (1967-261) to calculate the potential constants and energy levels for inversion and internal rotation. Diallo et al. (1985-335) used a spectrometer with improved resolving power to obtain new details in the central region of the amino wagging band of CH_3NH_2 at 780 cm⁻¹. The reported inversion wavenumbers and potential barriers are listed in Table 27.

Draeger et al. (1983-12) employed a variation of Eq. (13) to calculate the inversion energy levels for evaluating the inversion contributions to the thermodynamic properties of CH₃NH₂. The potential function was derived from the observed transitions and barrier heights of the inversion mode. However, we could not reproduce the transition frequencies with his parameters. His parameters gave $v_{inv}(1, \leftarrow 0_v) = 825.7 \, \text{cm}^{-1}$ which is not consistent with the accepted value of 780 cm⁻¹. We redetermined the constants in Eq. (13) to reproduce the experimentally observed (1964-409) value $v_{inv} = 780.1 \, \text{cm}^{-1}$. Thirty-six generated energy levels (0 to 24100 cm⁻¹) were employed for calculating the inver-

sion contributions to the thermodynamic properties of CH_3NH_2 .

Tables 23 and 24 summarize the molecular constants used for calculation of the ideal gas thermodynamic properties of methanamine. The results are listed in Table 13.

The calculated values are compared with experimental values where possible. Felsing and Jessen (1933-392) used a constant-flow calorimeter to determine the vapor heat capacities (C_n) of methanamine at 273.15, 298.15, and 323.15 K as 49.02, 54.02, and 57.70 J K^{-1} mol⁻¹, respectively. Their measurement imprecision was about 2%. Aston and Doty (1940-325) subsequently used the Berthelot equation of state to convert these values to ideal gas heat capacities (C_p°) as 47.91, 53.18, and 57.03 J K⁻¹ mol⁻¹. Evidently, the \dot{C}_{p}° values quoted by Draeger et al. (1983-12) for CH₃NH₂ are for the real gas (1933-392) rather than for the ideal gas. We assumed the C_n measurements of Felsing and Jessen (1933-392) were at atmospheric pressure and used the second virial coefficients of this work to derive values of C_p° at 273.15, 298.15, and 323.15 K as 46.78, 52.43, and 56.53 $J K^{-1} mol^{-1}$, respectively. Our values from spectroscopic data for the same respective temperatures are 47.81, 50.05, and 52.43 J K⁻¹ mol⁻¹. It is very unlikely that the computed values can be in error by as much as the differences from the experimental values. Stull and Sinke (1969-147) speculated that the experimental values may be too high because corrections for hydrogen bonding could not be adequately made. Draeger et al. reproduced these experimental values much more closely in their statistical mechanical calculations; however, they used a single term, n = 3, in Eq. (11) for the methyl rotation. We could not reproduce the derivation of their Eq. (12) from their Eqs. (8) and (11) for internal rotation, and we had problems with their inversion potential as discussed above.

There are several reports of the ideal gas thermodynamic properties of methanamine calculated from statistical me-

^aQuoted value.

chanics. The values of C_p° and S° (p=1 atm) at 298.15 K were reported as (in J K⁻¹ mol⁻¹): 51.71, 241.63 (1954-117); 49.25, 242.84 (1961-264); 49.83, 242.38 (1965-395); 50.08, 242.59 (1969-147); and 53.01, 243.38 (1983-12), respectively. The values obtained in this work are 50.05 and 242.9 (1 atm) J K⁻¹ mol⁻¹, respectively. The entropy at 298.15 K derived in this work from the third law (241.77 \pm 1.26) J K⁻¹ mol⁻¹ agrees within the accuracy of the two values.

Aston and Gittler (1955-602) (1955-621) derived a value of (243.6 \pm 1.3) J K⁻¹ mol⁻¹ from chemical equilibrium studies of methanamine with hydrogen chloride at temperatures from 276.15 to 313.15 K. They determined the activity of the hydrogen chloride from emf measurements involving HCl with mercury and with silver.

Ethanamine. Rotation of the -NH₂ group about the C-N axis of ethanamine produces one trans and two gauche conformers where the relative conformations are for the unshared pair of p electrons on the nitrogen atom with respect to the terminal methyl group. Wolff and Ludwig (1964-496) noted the differences in the Raman spectra of the trans and gauche isomers. Molecular orbital calculations by Radom et al. (1972-30) predicted that the gauche conformer was more stable than the trans by (182 cm⁻¹ or 2218 J mol⁻¹). Manocha et al. (1974-186) analyzed the far-infrared spectra of gaseous CH₃CH₂ND₂ and CH₃CD₃ND₂ to predict that the gauche form is more stable than the trans by 104 cm⁻¹ (1243) J mol⁻¹). Contrary to the foregoing investigations, others have indicated that the trans isomer is more stable. From examination of the infrared absorption spectra of eight isotopic ethanamine molecules, Tsuboi et al. (1975-118) assigned the torsional oscillational frequencies of the methyl and amino groups for the trans and gauche isomers. They made the energy level calculations on the basis of a coupled two-top system and reported that the trans form was more stable by 230 cm $^{-1}$ (2753 J mol $^{-1}$). Durig and Li (1975-168) used their observed Raman spectra of gaseous CH₃CH₂NH₂ and CH₃CH₂ND₂ to determine that the trans conformer is more stable by 207 cm⁻¹ (2477 J mol⁻¹). Hamada et al. (1983-92) used the difference in intensity of the -NH₂ vibrations observed in matrix isolation spectroscopy with varied nozzle temperatures to determine that the trans conformer was more stable by (100 ± 10) cm⁻¹ $(1197 \pm 120 \text{ J mol}^{-1})$. Fischer and Botskor (1984-145) compared the relative intensities from the microwave spectra for several temperatures to determine that the trans conformer is more stable by (110 ± 50) cm⁻¹. We adopted the value of Hamada et al. (1983-92) in this work.

Both trans- and gauche-ethanamine were studied by Fischer and Botskor (1982-83, 1984-145) with microwave spectroscopy to determine the rotational constants. Their values were adopted to obtain the product of the three principal of inertia $(I_aI_bI_c)$ and the reduced moments of inertia (I_r) , listed in Table 23. Some of the reported molecular structural parameters of trans- and gauche-ethanamine (1971-156, 1974-186, 1975-188, 1975-168, 1982-83) were estimated.

Investigations of the vibrational spectra of ethanamine include: Raman spectra by Wolff and Ludwig (1964-496,

1972-198), Durig and Li (1975-168) and Manocha and Fateley (1976-119); and far-infrared spectra by Tsuboi et al. (1968-229) and Manocha et al. (1974-186). The infrared absorption spectra of the two rotamers and eight deuterated species were examined by Scott (1971-155) and Tsuboi et al. (1975-118). Recently, Hamada et al. (1983-92) studied the infrared and Raman spectra of CH₃CH₂NH₂ and five deuterated species. They assigned a complete set of normal vibrational wavenumbers for the gaseous trans and gauche conformers. Their vibrational assignments for each conformer were used (except for the torsional wavenumbers for the -CH₃ and -NH₂ rotations, see Table 24).

From the internal rotation constants (F) and torsional wavenumbers (1975-168, 1976-119) for -CH₃ and -NH₂ rotations, the respective barrier heights (V_3 and V_2) were calculated. Ninety-six energy levels (0 to 15300 cm⁻¹) for the -CH₃ rotation and seventy-eight energy levels (0 to 16000 cm⁻¹) for the -NH₂ rotor were used in calculating the contributions to thermodynamic properties.

The results for the two conformers were combined with their enthalpy of isomerization to calculate the thermodynamic properties of the equilibrium mixtures. The results are presented in Table 13.

Experimental values for ethanamine are not available for comparison with our calculations. Some statistical mechanically derived values of C_p° and S° at 298.15 K and 1 atm, are compared with our results as follows (in J K⁻¹ mol⁻¹): 72.63, 284.85 (1969-147); 72.63, 284.64 (1971-156); and 71.54, 283.77 (this work). A methylene increment method (1968-224) gave 71.25 and 271.29 for C_p° and S° at 298.15 K.

1-Propanamine. 1-Propanamine has five possible conformations: T-T, G-T, G-G', T-G, and G-G where the first letter (T or G) refers to the trans or gauche orientation of the C-C-C-N chain, and the second letter (T, T, or T) refers to the trans or one of the two nonequivalent gauche orientations of the C-C-N-: chain. The symbol: is for the unshared pair of T electrons on the nitrogen atom. The observed spectra of this compound are too complex to interpret as arising from a single conformation (1971-155). Theoretical calculations (1980-110, 1985-281) show that the T-G form is the most stable and that the T-T form (formed from the T-T form by rotation of 120° about the T-T bond) is 2.72 kJ higher in potential energy than the T-T conformer. These conformers define the path of minimum potential energy for rotation about the T-T0 bond.

Wolff and Ludwig (1964-496, 1972-198) determined the Raman spectrum of 1-propanamine(g) and gave a partial vibrational assignment. Based on the observed far-infrared spectrum (1968-227), Scott (1971-155) satisfactorily showed that the observed wavenumbers cannot be uniquely assigned to his calculated normal vibrational frequencies for the five possible conformations of this compound.

The molecular structure of 1-propanamine has not been experimentally determined. Estimated molecular structural parameters (1971-155) of the T-G conformer were used to calculate the values of I_a , I_b , and I_c and reduced moments of inertia (I_c) for the -CH₃ and -NH₂ rotations (see Table 23).

We adopted the normal vibrational wavenumbers of the

 ^-G conformer assigned by Scott. If observed wavenumbers vere not available, calculated values were used. The barriers o rotation, V_3 in Eq. (11), were calculated from torsional vavenumbers [252 cm $^{-1}$ for CH $_3$ and 210 cm $^{-1}$ for -NH $_2$ 1971-155)] and the corresponding F values. Rotation bout the C_1 - C_2 bond was treated as hindered with a toronal wavenumber of 104 cm $^{-1}$, and the potential function vas used in the semiclassical approximation of Pitzer and winn (1942-175). Inversion was treated as a harmonic oscillator.

The internal rotational contributions to thermodynam: properties were determined from 96 and 78 internal rotation energy levels for -CH₃ and -NH₂, respectively. We street approximate agreement between the calculated encopy at 298.15 K (325.44 J mol⁻¹ K⁻¹) with our evaluated nird-law value $S^{\circ} = (325.93 \pm 0.84)$ J mol⁻¹ K⁻¹ by adisting the skeletal torsion of T-G conformer to 106 cm⁻¹. The calculated thermodynamic properties are listed in Table 3.

The vapor heat capacity of this compound has not been leasured. Previous statistical-mechanically calculated vales of C_p° and S° at 298.15 K and 1 atm compare with our alues as follows: (in J K⁻¹ mol⁻¹) 91.21, 325.93 (1971-55); and 91.17, 325.44 (this work, at 1 atm). The following stimated values of C_p° and S° at 298.15 K calculated by roup additivity have been reported: 94.14, 301.08 (1968-24); 95.77, 324.18 (1969-147).

2-Propanamine. For 2-propanamine rotation of $-\mathrm{NH}_2$ bout the C-N bond produces three possible staggered constructions. The orientation with the unshared pair of electons on the N atom trans to the C-H bond is denoted as sans with C_s symmetry. The unshared pair of electrons and to one of the C-C bonds results in two equivalent auche conformations with C_1 symmetry. We treated 2-propanamine as an equilibrium mixture of s-trans and gauche onformers in methods similar to the calculations for 2-ethnamine, described above.

Krueger and Jan (1970-181) investigated the infrared pectrum of $(CH_3)_2CDNH_2$ in a dilute solution with CCl_4 and determined the energy difference between the two constraints as (0.50 ± 0.08) kJ mol⁻¹. A theoretically callated value of 2.80 kJ mol⁻¹ was reported by Lathan *et al.* 1973-187). The gauche conformers are more stable than it is s-trans.

From analysis of microwave spectrum of trans-2-proanamine(g), Mehrotra et al. (1977-105) determined the rotational constants and moments of inertia (I_a, I_b, I_c) which were used to obtain the values of $I_a I_b I_c$ listed in Table 23. Durig et al. (1979-100) studied the Raman spectra of gas, liquid, and solid, and the infrared spectra of gas and solid 2-propanamine- d_0 and $-d_2$. They assigned 33 vibrational wavenumbers for both s-trans and gauche conformers. Their vibrational assignments (except the two -CH₃ torsional wavenumbers for gauche conformer) were adopted. Their numerical values are listed in Table 24. Scott (1971-155) assigned similar vibrational wavenumbers for these two conformers from analysis of far-infrared spectra of 2propanamine in solution and vapor states (1968-227). He interpreted the observed spectra of 2-propanamine as arising from a single conformation; gauche with C₁ symmetry. His torsional assignments, as listed in Table 23, for the two -CH₂ rotations in the gauche conformer were selected for determining V_3 in Eq. (11).

For both the gauche and s-trans conformers, estimated molecular structural parameters were used to calculate the principal moments of inertia $(I_a, I_b, \text{and } I_c)$ and the reduced moments of inertia (I_r) for the -CH₃ and -NH₂ rotors. See Table 23 for their values.

The internal rotational contributions to thermodynamic properties for each conformer were determined from 102 and 78 internal rotation energy levels for -CH₃ and -NH₂, respectively.

The selected value H° (gauche,0 K) – H° (s-trans, 0 K) = 1.749 kJ mol⁻¹ (1979-100) was used with the properties calculated for the conformers to compute the thermodynamic properties of 2-propanamine which are listed in Table 13.

Vapor heat capacities of 2-propanamine are not available for comparison with our results. Calculated thermodynamic properties of 2-propanamine have been reported by Scott (1971-155) and Durig et al. (1979-100). Scott (1971-155) adopted his vibrational assignments for gauche conformer and the calculated principal moments of inertia based on an assumed molecular structure to evaluate the thermodynamic properties for 2-propanamine. He disregarded the presence of rotational conformers; his calculated thermodynamic property values are generally lower than either ours or those of Durig et al. (1979-100). Durig et al. (1979-100) employed a molecular model composed of strans and gauche conformers. For -NH₂ torsion, they used a potential function of the form

$$V_r = \frac{1}{2} \sum_{i} V_i (1 - \cos i\theta),$$
 (14)

where i = 1 to 6 and the internal rotational constant of the form

$$F = F_0 + \sum_i F_i \cos i\theta, \tag{15}$$

where i=1 to 4, and F is a function of the angle of internal rotation (θ) and F_0 is defined for the s-trans conformer. For -CH₃, a complicated internal rotational Hamiltonian was used to account for interaction of the methyl rotations. They selected a value of 1749 J mol⁻¹ for the energy difference between s-trans and gauche conformers to compute the compositions of the equilibrium mixture of 2-propanamine.

The reported statistical-mechanical values of C_p° and S° at 298.15 K and 1 atm are compared with ours as follows (in J K⁻¹ mol⁻¹): 95.8, 311.8 (1979-100); 94.56, 312.54 (1971-155); and 97.55, 312.24 (this work). The entropy derived from condensed phase heat capacity measurements in section 3.7, (311.6 \pm 0.8) J K⁻¹ mol⁻¹, adequately agrees with the value derived from spectroscopic data.

Benzenamine. Benzenamine has symmetry C_s ($\sigma = 1$). The nonplanar configuration of this molecule has been discussed by Evans (1960-296). From an investigation of the microwave spectra of C₆H₅NH₂ and C₆H₅NHD, Lister and Tyler (1966-402) established that C₆H₅NH₂(g) has a nonplanar structure in which the -NH2 plane (containing the nitrogen atom and its two attached hydrogens) makes an angle of 40° with the plane of the C₆H₅- group. The same result was obtained from uv studies by Brand et al. (1966-403). Lister et al. (1974-79) determined the molecular structure from microwave spectra of thirteen deuterated species of benzenamine and found that the C-H distance is (1.402 ± 0.002) Å and that the -NH₂ group adopts an outof-plane angle of $37^{\circ}29' \pm 2^{\circ}$ with the angle HNH 113°6′ \pm 2°. They also reported the values of I_a , I_b , and I_c . These values were adopted to calculate the $I_a I_b I_c$ (see Table 23). Similar moments of inertia values were reported by Hatta et al. (1973-164).

The infrared and Raman spectra of benzenamine have been the subject of several investigations. Williams et al. (1939-411) investigated the near infrared spectrum. Evans (1960-296) studied the Raman spectra (liquid phase) and infrared spectra (vapor, solution and liquid phases) of C₆H₅NH₂, C₆H₅NHD, and C₆H₅ND₂. Complete vibrational assignments for C₆ H₅ NH₂ were made. Tsuboi (1960-211) examined isotopic effects on the vibrational wavenumbers and made assignments for modes involving the -NH₂ group. Kuwae and Machida (1978-112) studied the CH out-of-plane deformation vibrations of monosubstituted benzenes. Their assignments of the vibrational wavenumbers for benzenamine agreed with those reported by Evans (1960-296). Vibrational assignments of Evans were adopted for calculating the thermodynamic properties of this compound by Draeger (1984-19) and Hussein et al. (1985-203). Recently, Niu et al. (1985-127) proposed a number of reassignments of the spectra of C₆H₅NH₂ and its deuterated analogs. The values reported by Niu et al. (1985-127), except those for -NH2 internal rotation and inversion modes, were employed here.

Larsen et al. (1976-13) used far infrared spectroscopy to investigate the inversion and torsion of the -NH₂. They used the molecular structure determined by microwave spectroscopy (1974-79) with $V_r(\theta) = (1/2) \Sigma_i V_i \times (1-\cos i\theta)$ (i=1 and 2) for the potential function to calculate the wavenumbers for the inversion mode. The potential barrier 524.4 cm⁻¹ used for their calculation is larger than the 454 cm⁻¹ barrier found by Quack and Stockburger (1972-193), and the potential minimum at 42.17° is in agreement with the value of 42° (1972-193) but larger than the value 37.5° reported by Lister et al. (1974-79).

Kydd and Krueger (1977-91) observed the vapor phase infrared spectra of C₆H₅NH₂, C₆H₅NHD and

 $C_6H_5ND_2$ from 12 to 650 cm⁻¹. They assigned several inversion transitions due to $C_6H_5NH_2$, which were in excellent agreement with those proposed by Larsen *et al.* (1976-13). Kydd and Krueger (1977-91) chose a simple double-minimum potential with a gaussian barrier to describe the inversion motion. The calculated inversion transitions were in perfect agreement with the observed energy levels. The barrier height, 525.9 cm⁻¹, compares favorably with the value 524.4 cm⁻¹, reported by Larsen *et al.* (1976-13).

Based on the inversion transitions 40.8, 423.8, and 700.1 cm⁻¹ observed by Kydd and Krueger (1977-91), Draeger (1984-19) derived a reduced potential function $V_w/\text{cm}^{-1} = 45.00 \left[(r/r_o)^4 - (r/r_o)^2 \right]$ for inversion in $C_6H_5NH_2$. This potential function was used to generate 30 inversion energy levels (0 to 19500 cm⁻¹) for evaluation of the inversion contributions to thermodynamic properties.

The torsional wavenumber of 277.3 cm $^{-1}$ for benzenamine was determined by Larsen *et al.* (1976-13) from farinfrared spectrum. We adopted this torsional wavenumber and calculated F = 10.512 cm $^{-1}$ to evaluate the internal rotation barrier height (V_2) in Eq. (11) as 23.637 kJ mol $^{-1}$ for the -NH $_2$ rotation. The adopted value of I_r was based on the molecular structure determined by Lister *et al.* (1974-74) from microwave spectroscopy. We generated 72 internal rotation energy levels (0 to 14500 cm $^{-1}$) for evaluation of internal rotational contributions to thermodynamics properties.

The computed thermodynamic properties of benzenamine are listed in Table 13. The value of S° (298.15 K) = 317.87 J K⁻¹ mol⁻¹ obtained at 1 bar pressure or 317.76 J K⁻¹ mol⁻¹ at 1 atm is in agreement with the third law value (318.67 \pm 0.84) J K⁻¹ mol⁻¹. Our calculated C_{ρ}° and S° at 298.15 K and 1 atm are compared with statistical mechanically derived values as follows (in J K⁻¹ mol⁻¹): 108.41, 319.16 (1962-3, 1969-147); 108.11, 318.40 (1983-12); 111.21, 319.78 (1985-203); and 107.94, 317.87 (this work).

2-Methylbenzenamine. An assumed molecular structure of 2-methylbenzenamine was used to calculate the values of $I_aI_bI_c$ and the reduced moments of inertia (I_r) for -CH₃ and -NH₂ rotors. The structural parameters of the ring were assumed to be the same as those of benzenamine (1974-79). The bond distances and angles in the -CH₃ group were the same as those in alkanes. The calculated results are given in Table 23.

Based on reported infrared spectra of 2-methylbenzenamine, Draeger (1984-19) obtained the vibrational wavenumbers of this compound which were adopted in this work (see Table 24). Partial vibrational assignments for the compound were reported by Sverdlov et al. (1974-117). The barrier for -CH₃ rotation, $V_3 = 6230 \text{ J mol}^{-1}$, was taken from Rudolph et al. (1973-66), assuming the barrier for the adjacent methyl groups in 1,2-dimethylbenzene molecule is the same as that for the adjacent -CH₃ group in 2-methylbenzenamine. From the far-infrared vapor phase spectra of the 2-, 3-, and 4-methylbenzenamines, Kydd and Krueger (1980-76) observed the first three -NH₂ inversion vibration energy levels for each isomer. Draeger (1984-19) derived a $V_w(r/r_o) = \{a(r/r_o)^4$ reduced potential function

 $-b(r/r_o)^2$ } where a=45.85 cm⁻¹ and b=6.83 cm⁻¹ for fitting the -NH₂ inversion energy levels reported by Kydd and Krueger (1980-76) for 2-methylbenzenamine. We adopted this reduced potential function to generate 24 inversion energy levels (0 to 14400 cm⁻¹) for calculation of inversion contributions to thermodynamic properties of this compound.

The contributions to thermodynamic properties due to internal rotations of -CH₃ and -NH₂ group were evaluated by using 102 and 66 internal rotation energy levels, respectively. The I_r and barrier height values employed for generating levels are presented in Table 23. The value of F was computed, and the value of V_2 for the -NH₂ group was taken from that of -NH₂ in benzenamine.

The calculated thermodynamic properties of 2-methylbenzenamine are given in Table 13. There are no experimental vapor heat capacity or third-law entropy measurements available for comparison. Our calculated values of C_n° and S° at 298.15 K and 1 atm are compared with other calculated values in the literature as follows (in $J K^{-1} mol^{-1}$): 133.9, 349.3 (1983-108); 134.94, 355.20 (1984-19); and 130.21, 351.05 (this work). The differences between our values and those of Draeger (1984-19) result from differing computational methods because the differences persisted when his choice of molecular constants and vibrational frequencies were used as input to our computational procedure; the differences appear to arise from internal-rotational contributions to the heat capacity. The differences from those of Kudchadkar et al. (1983-108) arise from differences in choices of input data.

3-Methylbenzenamine. Molecular structural parameters for 3-methylbenzenamine were estimated by procedures similar to those for 2-methylbenzenamine to calculate values of $I_aI_bI_c$ and reduced moments of inertia for the -CH₃ and the -NH₂ rotor. They are listed in Table 23.

The fundamental vibrational wavenumbers reported by Draeger (1984-19) were adopted (see Table 24). The -CH₃ group was assumed to rotate freely. Based on $V_2 = 23.64$ kJ mol⁻¹ and F = 12.095 cm⁻¹, 66 -NH₂ internal rotation energy levels were generated for calculating the internal rotational contributions. The reduced potential function derived by Draeger (1984-19) for 3-methylbenzenamine was adopted to generate 24 inversion energy levels. The calculated inversion energy levels (40.4, 422.0, and 706.4 cm⁻¹) are in good agreement with those (40.2, 423.2, and 705.2 cm⁻¹) observed by Kydd and Krueger (1980-76).

The evaluated thermodynamic properties for 3-methylbenzenamine are listed in Table 13. There are no experimental C_p° and S° values available for comparison with our calculated results. A comparison of C_p° and S° at 298.15 K and 1 atm between other calculated values and ours are given here (in J K⁻¹ mol⁻¹): 128.9, 354.3 (1983-108); 130.04, 355.69 (1984-19); and 125.47, 352.49 (this work). The differences have explanations similar to those for 3-methylbenzenamine.

4-Methylbenzenamine. The values of $I_aI_bI_c$ for 4-methylbenzenamine and of I_r and V_n for the -CH₃ and the -NH₂ groups were determined by estimation procedures similar to those for the other benzenamine methyl deriva-

tives described above. The vibrational assignments of Draeger (1984-19) for this substance were employed for statistical calculation of vibrational contributions to thermodynamic properties. The -CH₃ group was assumed to be a free rotor. Sixty-six energy levels were generated for the -NH₂ internal rotation. Kydd and Krueger (1980-76) observed the first three -NH₂ vibration wavenumbers for this compound. We employed the reduced potential function derived by Draeger (1984-19) from these observed inversion energy levels to generate 24 inversion energy levels calculating -NH₂ inversion contributions to thermodynamic properties. The evaluated thermodynamic properties are presented in Table 13.

No experimental C_p° and S° have been reported in the literature. Our calculated C_p° and S° at 298.15 K and 1 atm are compared with other calculated values reported in the literature as follows (in J K⁻¹ mol⁻¹): 128.5, 353.4 (1983-108); 130.79, 352.37 (1984-19); and 126.16, 347.02 (this work). The comments on the differences for 2-methylbenzenamine apply here.

4. Discussion

The eight primary amines selected in this study of their thermodynamic and thermophysical properties are the lowest members of the primary alkanamine and alkylbenzenamine homologous series of compounds. These results serve as a basis in empirical correlations for estimating properties of the higher members of these homologous series. However, the reliability of the estimated quantities depends on the accuracy and reliability of the basic values used for the estimation. It would be beneficial to obtain new data to improve the reliability of the thermodynamic properties of the amines selected for this work.

Predictive methods were used to derive recommended values of the critical properties of the methyl substituted benzenamines because measurements for these were absent or of poor quality; measurement of the critical properties for these is recommended. For 2-propanamine, the vapor pressure data above atmospheric pressure appears inconsistent. There are few reliable density values at high temperature for ethanamine, and the methylbenzenamines. Second virial coefficient data were measured for methanamine and ethanamine, but the values for ethanamine are of low quality. Second virial coefficient measurements would be informative for the higher alkanamines and benzenamines; however, these could be derived from enthalpy of vaporization values which are absent for these same substances. Reliable enthalpy of combustion measurements for the methylbenzenamines should receive high priority. There are no low temperature heat capacity measurements for ethanamine and the three methylbenzenamines. Liquid heat-capacity measurements on these compounds are either nonexistent or unreliable. For any of the properties considered here, measurements of properties for 2-methylbenzenamine would be more informative than they would be for the other two isomers.

We are not completely satisfied with the methods used for computing the ideal gas thermodynamic functions by

statistical mechanics. The greatest deficiencies lie in the computational methods for compounds with compound internal rotations such as those in ethanamine and the propanamines.

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6. Symbols and Notation

Subscripts a	ınd	indexes,	general
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c	for value of T , p , V , or ρ at the critical point
f	for formation of the substance from its elements, each in their standard states
g	for vapor in equilibrium with liquid
i, j, m, n	integer index
1	for liquid in equilibrium with vapor
r	for coefficient to reduced variable in Eq.
	(10); for reduced variable in Eq. (12);
	for moment of inertia; for rotational po-
	tential function
ref	at reference pressure (101.325 kPa) in
	Cox vapor pressure Eq. (3a) and (3b)
sat	for value of C_{sat} or p_{sat} determined with
	an infinite amount of vapor(here) in
	equilibrium with the condensed phase
	(l or c)
tr	for value of T or Δ of H at a transition
•	temperature
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Superscripts (see other variables and notations, and functional notation below)

Other variables and designations

$A_a,B_a,,F_a$	coefficients in extended Antoine Eq.
	(5)
A_d, A_d	coefficients in Eq. (13) for -NH ₂ inversion
A_i	least squares adjusted parameter in Eqs.
	(2), (3a), and (6)
A_r	coefficient to ρ_c in Eq. (10) for second
	virial coefficient
A_x	exponential function in Eqs. (3a) and
	(3b)
A',A'',C_1,C_s	molecular symmetry species
В	second virial coefficient in Eqs. (8)-
	(10)
C	carbon symbol
C_b	coefficient to exponential term in Eqs.
	(9)–(10)
$C(A_i,A_j)$	element in correlation matrix in Eq. (2)
C_{cnd}	heat capacity determined at constant cnd (sat or p)

D_r	coefficient to (T_c/T) in expontential
2,	term of Eq. (10)
\boldsymbol{F}	= $h/8\pi^2 cI_r$, function for internal rota-
_	tion
F_i	coefficient in $\Sigma_i F_i$ cos $i\theta$ for angle de-
\boldsymbol{G}	pendent function for internal rotation molar Gibbs energy
H	hydrogen symbol
H	molar enthalpy
I_a , I_b , and I_c	moments of inertia about the three prin-
7	cipal orthogonal axes
I_r	reduced moment of inertia for relative rotation about a bond
L	number of degrees of freedom involved
	in rotation about C-N and C-C bonds
N	nitrogen symbol
N	number of atoms in each molecule
S T	molar entropy
T_a°	temperature nearest integer value of temperature in
- u	degree Celsius at which the vapor pres-
	sure is 130 kPa in the extended Antoine
Tr.	Eq. (5)
T_b T_m	boiling temperature at 101.325 kPa freezing temperature at 101.325 kPa in
1 m	air
V	molar volume; potential function
V_n	coefficients in potential function for rel-
T/	ative rotation about a bond
V_r	potential function for relative rotation about a bond
V_w (z or r/r_o)	potential function for inversion of -NH ₂
w \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \	where z and r/r_o are the relative motion
	displacements
X_a	in the extended Antoine Eq. (5)
a,b	coefficients in potential function for -NH ₂ inversion
c	crystal
g	gas
1	liquid exponent to X_n in extended Antoine Eq.
n	exponent to X_a in extended Antoine Eq. (5)
p	pressure
p_{sat}	vapor pressure
$p_{\rm tp}$	triple point pressure
x	= $[1 - T/(T_c)]$ in Eq. (6) condensed phase
α_m	coefficient to $(1 - T/T_c)$ in Eq. (7)
Δ	see functional notation below
ϵ	= 0.35, exponent to x in Eq. (6)
θ	angle of rotation
ν_i	fundamental vibrational frequency bending frequency between lowest two
$ u_{ m inv}$	energy levels for inversion about a ni-
	trogen atom
$v_{\rm tor}(0\rightarrow 1)$	torsional frequency for transition be-
_	tween lowest two energy levels
$ ho \sigma$	density molecular symmetry number
U	molecular symmetry number

imprecision in the variable x with $\sigma_{\epsilon}(x)$ $\sigma(x)$ constant contribution and $\sigma_{\ell}(x)$ frac-

tional contribution

Constants and units

°C degree celsius, temperature J joule, energy K kelvin, temperature $pascal = newton/(meter)^2$, pressure Pa $= 8.3145 \, 10 \, \text{J K}^{-1} \, \text{mol}^{-1}$, gas con-R $= 2.99792458 \times 10^8 \text{ m s}^{-1}$, speed of c light cm^{-1} ≥29 979.2458 MHz, wavenumber = 2.71828,..., Napierian base e $= 6.6260755 \times 10^{-34}$ J Hz, Planck's h constant meter m $= 6.0221367 \times 10^{23}$ molecules, mole

S = 3.1415... π

second

Functional notation

chaftsl. 1887, 1, 237

mol

cosine of angle θ $cos(\theta)$ logarithm of Z for Napierian base, e ln(Z)logarithm of Z for base 10 $\log_{10}(Z)$ angle of Y degrees and Z minutes variable Y as a function of the param- $Y(A_1,A_2,...)$ eters, A_1, A_2, \dots Z° value of Z(C,H,S,G) at 100 kPa, standard state Z(ph,T)value of $Z(C_p, \Delta_f H^\circ, \text{etc.})$ for phase phat temperature \vec{T} change in variable Z(G,H,S) for pro- $\Delta_{\alpha}Z$ cess(f or tr) $\Delta_{\rm cl}^{\rm v2} Z$ change in variable Z(G,H,S) in passing between states s1 to s2

7. References

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